

Development and evaluation of multiparticulate biphasic system for the treatment of circadian diseases

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Multiparticulate systems have biopharmaceutical advantages when compared to the monolithic systems, once they allow different patterns of drug release and can be used in different treatments. The aim of the present work was to develop a biphasic controlled release delivery system, using propranolol hydrochloride (PROP) that can be used for the treatment of circadian diseases. This system was obtained by the combination of cellulosic polymers hydroxypropyl methylcellulose (HPMC) and ethylcellulose (EC) in a 2² factorial experimental design, which allowed the optimization of the development stage. The pellets produced and used in biphasic formulations were evaluated for physical and chemical characteristics and presented acceptable results. The immediate fraction obtained showed the complete release in 30 min while the others kept the release of the drug for 24 h. This study showed that the combination of beads with different releasing characteristics allowed to obtain different release profiles, which can be modulated according to the pathological needs, especially with regard to circadian diseases that suffer alterations throughout the day.

Keywords: Chronotherapy. Biphasic Release. Pellets. Cellulosic Polymers. Experimental Design.

INTRODUCTION

Multiparticulate systems are, by definition, a functional unit that contains the drug subdivided into pellets, granules, mini-pills or a combination of these (Zerbini, Ferraz, 2011). Pellets are spherical units constituted by agglomeration of drugs and excipients, with diameters ranging from 100 to 2000 µm, and may act as an intermediate for the production of sachets, capsules or tablets. Multiparticulate systems have advantages when compared to classical unitary systems: better distribution on the gastrointestinal tract (GIT), lack of influence of gastric emptying, lower risk of systemic toxicity and local irritation, as well to enable the obtaining of customized release forms (Ghebre-Selassie, 1989; Bauer *et al.*, 1998; Pezzini, Silva, Ferraz, 2007; Aulton, Ortega, 2008; Kulkarni, 2010; Lachman, Lieberman, Kaning, 2013).

In an ideal therapeutic regimen, the drug must reach the site of action quickly and its release must be constant during the treatment. Some drugs have naturally a long time of action, requiring only one daily dosing to maintain the adequate plasma levels. However, many others must be administered repeatedly, which may result in a seric drug fluctuation in intervals prior to the next administration (Aulton, Ortega, 2008; Bruschi, 2015). As an alternative to such inconvenience, it has been increasingly sought the use of systems capable of modulating the release of the drug in a gradual manner, providing a reduction in the frequency of administration, less fluctuation in plasma concentrations of the drug, less side effects and greater adherence to treatment (Lopes, Lobo, Costa, 2005; Villanova, Oréfice, Cunha, 2010).

On the types of modified release existing in the pharmaceutical context, the biphasic delivery system stands out, which is intended to release the drug at different stages of release, a fraction of initial release (fast) and a modified release (slow) and the first fraction may be represented by the immediate release, while the second by extended release (Jha, Rahman, Rahman, 2011).

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Representing the pharmacotherapeutic agent candidates and attractive for this type of release, one has the antihypertensive drugs, antihistamines, analgesics, antipyretics and anti-allergic. These drugs are used for the treatment of diseases known as circadian that have oscillations according to the period of the day, since the human organism is complex and is constantly subject to physiological and biochemical changes, such as the case of hypertension, where the occurrence of manifestations related to cardiovascular complications occur predominantly in the early morning hours, period on which the blood pressure is higher (Londhe, Gattani, Surana, 2010; Ohdo, 2010; Jha, Rahman, Rahman, 2011; Lin, Kawashima, 2012; Verdecchia *et al.*, 2012; Dallmann, Brown, Gachon, 2014).

To obtain a specific release system, it is often necessary the use of polymer-based coatings, being common in these cases the mixture of polymers with different characteristics and solubility properties, for example the association of cellulose derivatives hydroxypropyl methylcellulose (HPMC), with high water solubility, and ethyl cellulose (EC), with water-insoluble characteristics, widely used in pharmaceuticals in order to obtain modified drug release systems (Lopes, Lobo, Costa, 2005; Oliveira, 2007; Guerra-Ponce *et al.*, 2016).

In cases in which are used the combination of polymers to obtain the desired release profile, it is extremely important the knowledge of its characteristics and influence in the formulation, in order to reduce the development time and the number of trials. Thus, several tools have been used to optimize the development phase, as the case of the use of the experimental design tool that provides more accurate information with a lower number of experiments. In the present scenario, the pharmaceutical industry seeks to increasingly reduce the development time and getting more robust processes that increase competitiveness in the market (Pisano, 1997; Singh, Kumar, Ahuja, 2005; Rubin *et al.*, 2006; Lachman, Lieberman, Kaning, 2013).

The aim of the present study was to develop a biphasic controlled release delivery system with length of 24 hours, for the treatment of circadian diseases, using propranolol hydrochloride (PROP), a β -blocker drug widely used in heart diseases. Due to the peak concentration of 1-1.5 hour and the half-life of 4-6 hour, the active may be considered a strong candidate for developing a modified-release formulation (Brasil, 2010b). For that, it was used a combination of cellulosic polymers for coating with HPMC-EC polymers associated with a 2^2 factorial experimental design to the optimization of the development stage.

MATERIAL AND METHODS

Material

Propranolol hydrochloride, (PROP) (Iffect Chempar Co. Ltda, India), polyvinylpyrrolidone K30 –Plasdone® K30, (PVP K30) (Ashland, USA); sucrose inert beads 25-30 mesh, (EIS) (JRS Pharma, Germany); ethylcellulose N45 –Ethocel® N45 (EC) and hydroxypropyl methylcellulose 5cps –Methocel® E5 LV, (HPMC) (Colorcon, USA); talc (Magnesita, Brasil) and Triethyl citrate (TEC) (Vertelus, USA). The raw materials and excipients used were kindly provided by Prati Donaduzzi Ltda Pharmaceutical Industry, Brazil.

Compatibility study

The interaction between the drug and the excipients were evaluated through analysis of Differential Scanning Calorimetry (DSC) and Fourier Transform Infrared Spectroscopy (FTIR). Analyses were performed on samples containing pure PROP, binary mixtures of PROP with excipients in the proportion 1:1, mixture of the placebo used in the final formulation and PROP in equal proportion (1:1) and also the pellets of the best formulation obtained at the end of the development stage.

DSC analyses were performed using a DSC-1 (Mettler Toledo) and the results were processed in Star® software, licensed by Mettler-Toledo®. The analyses of FTIR were performed by using a Infrared Fourier Transform Spectrophotometer (Spectrum 400®, Perkin –Elmer®) with accessory of attenuated total reflectance probe (ATR) to mid-infrared.

Development of the immediate release fraction

For choosing the bonding agent employed in the attainment of pellets 4 formulations (A - D) were prepared using the solution PVP K30 or HPMC polymers in different proportions. An initial loading of 1500 g of EIS was used in the preparation of the formulations. The composition of formulations are shown in Table I.

For formulation A, the EIS was coated with an alcohol solution, a mixture of PROP, PVP K30 and talc. For the formulations B, C and D, EIS were coated with a hydroalcoholic solution (1:1, w/w) containing the mixture of PROP, HPMC and talc. The coating process of all formulations were performed in fluidized bed (Bosch Hüttlin® Unilab®), following the parameters: Inlet air flow rate = $250 \, \text{m}^3$ /h, inlet air temperature = $40 - 45 \, ^{\circ}\text{C}$ and product temperature = $37 - 39 \, ^{\circ}\text{C}$. After completion of the

TABLE I - Composition of formulations for choosing bonding agent

| Composition | A (%) | B (%) | C (%) | D (%) |
|-------------------------|--------|--------|--------|--------|
| PROP | 11.32 | 11.32 | 11.32 | 11.32 |
| PVP K30 | 1.89 | - | - | - |
| HPMC | - | 0.94 | 2.83 | 3.77 |
| Talc | 2.83 | 2.83 | 2.83 | 2.83 |
| EIS | 29.25 | 30.19 | 28.30 | 27.36 |
| Isopropyl Alcohol (AIS) | 54.72 | 27.36 | 27.36 | 27.36 |
| Purified Water | - | 27.36 | 27.36 | 27.36 |
| Total | 100.00 | 100.00 | 100.00 | 100.00 |

coating process, the pellets were dried at 40 $^{\circ}$ C for 30 min. The yield (R%) of the formulations was calculated as:

$$R(\%) = \frac{\text{weight obtained from coated pellets}}{\text{initial weight (excipients + PROP)}} \times 100$$
 (1)

From the initial formulations, the one with the highest yield and performance was used for developing the pellets. The formulation chosen, initial weight of 1500 g of pellets coated with PROP, was subjected to seal coating, prepared from an aqueous colloidal dispersion of HPMC (8.20%, w/w). The following parameters were followed: Inlet air flow rate = 250 m³/h, inlet air temperature = 45–50 °C, product temperature = 39–41 °C, atomization pressure = 1.20 bar, microclimate pressure = 0.25 bar, atomization nozzle diameter = 1.0 mm, air cap diameter = 12 mm, and atomization rate of the coating suspension = 10-14 g/min. After the coating process, the pellets were dried for 30 min at 40 °C.

Development of the modified release fraction

To optimize the development of PROP pellets for modified release, experiments were performed based on a full factorial design with two factors in two levels (2²) and triplicate on the center point, resulting in 7 modified release formulations. The variables studied were the concentrations of HPMC and EC coating polymers in the third coating layer of the pellets as well as HPMC x EC interaction in response of the PROP release time. For each factor (HPMC and EC), two levels were used: -1 (low) and +1 (high), according to Table II.

The experiments were performed randomly and with triplicate at the center point. The factorial matrix used for the design of experiments is shown in Table III. The

TABLE II - HPMC and EC variables and levels (-1, 0 and 1) used in the factorial experimental design 2^2

| Variables | | Levels | |
|-----------|-------|--------|-------|
| Variables | -1 | 0 | 1 |
| HPMC (mg) | 2.00 | 4.00 | 6.00 |
| EC (mg) | 10.00 | 20.00 | 30.00 |

experimental data obtained from this 2² factorial design were processed using the Design Expert® 7.1.3 software. The significance of the factors and model validation were confirmed by the analysis of variance (ANOVA) and linear regression.

TABLE III - Factorial 2² planning for the codified variables: HPMC (mg) and EC (mg). Experiments performed randomly and with triplicate at the center point

| Formulation | Sequence | Variables codified | | |
|-------------|----------|--------------------|---------|--|
| | | HPMC (mg) | EC (mg) | |
| F1 | 4 | -1 | -1 | |
| F2 | 3 | 1 | -1 | |
| F3 | 5 | -1 | 1 | |
| F4 | 2 | 1 | 1 | |
| F5 | 6 | 0 | 0 | |
| F6 | 1 | 0 | 0 | |
| F7 | 7 | 0 | 0 | |

In order to obtain modified release pellets, it was used as starting point PROP pellets with seal coating, an initial amount of 1500 g for batches. The coating of the F1 to F7 formulations was carried out from a hydroalcoholic solution (ethanol: water 9:1 w/w) of the EC, HPMC and TEC mixture, as the amounts described in Table IV. The following parameters were followed: inlet air flow rate = 250 m³/h, inlet air temperature = 40–45 °C and product temperature = 35–37 °C. After completion of the coating process, the pellets were dried at 40 °C for 30 min.

Obtaining the multiparticulate biphasic system of PROP

Different proportions of the immediate and modified release pellets obtained were placed in hard gelatin capsules #1 for evaluation and comparison of the dissolution profiles, resulting in the F8 and F9 formulations. The final concentration of 80 mg PROP was maintained in each of the formulations.

| Composition | F1 (mg) | F2 (mg) | F3 (mg) | F4 (mg) | F5 (mg) | F6 (mg) | F7 (mg) |
|-----------------|---------|---------|---------|---------|---------|---------|---------|
| Pellets Sealed | 337.60 | 337.60 | 337.60 | 337.60 | 337.60 | 337.60 | 337.60 |
| EC | 10.00 | 10.00 | 30.00 | 30.00 | 20.00 | 20.00 | 20.00 |
| HPMC | 2.00 | 6.00 | 2.00 | 6.00 | 4.00 | 4.00 | 4.00 |
| TEC | 1.20 | 1.60 | 3.20 | 3.60 | 2.40 | 2.40 | 2.40 |
| Alcohol 96 °GL* | 682 | 682 | 682 | 682 | 682 | 682 | 682 |
| Purified Water* | 68.20 | 68.20 | 68.20 | 68.20 | 68.20 | 68.20 | 68.20 |
| Total | 350.80 | 355.20 | 372.80 | 377.20 | 364.00 | 364.00 | 364.00 |

TABLE IV - Formulation for obtaining modified release pellets

Determination of drug content

PROP content in the pellets was determined using a UV/Vis spectrophotometer (Varian Cary® 50). A pellet mass equivalent to 25 mg PROP was weighed and transferred to a 25 mL volumetric flask, added with 2 mL methanol and the flask was taken to ultrasonic bath (Unique, model C3300) for 40 min. Subsequently, more 12.5 mL methanol was added and the flask was taken to ultrasonic bath for another 20 min. The volumetric flask volume was filled with the same solvent. From this solution, an aliquot of 2.0 mL was transferred to a 25 mL volumetric flask and the volume was completed with HCl 0.01 N. All solutions were filtered through a quantitative cellulose filter and the final concentration was 0.08 mg/ mL PROP. The samples were analyzed by UV/VIS spectrophotometer at 289 nm and trials were performed in triplicate.

Dissolution profile

Dissolution of PROP pellets was performed by a methodology validated in our laboratory according to Resolution n. 899 of ANVISA (Brasil, 2003), in USP dissolutor apparatus 1 (basket) Sotax[®] Semiautomatic, coupled to the automatic samples collector, using hydrochloric acid solution (HCl 0.01 N, 1000 mL) as dissolution medium at 37.0 ± 0.5 °C. The collections and respective readings occurred on-line at time intervals of 5, 10, 15, 20, 30, 60 and 90 min for the pellets with active coating and sealing coating and at intervals of 30, 60, 90 , 120, 180, 240, 360, 480, 600, 720, 960, 1200 and 1440 min for the modified pellets of biphasic release. For F3 the analysis time has been extended to 2400 min. Samples were analyzed by spectrophotometry in the ultraviolet region at 289 nm using UV/Vis spectrophotometer to determine the concentration of drug present.

The dissolution efficiency (DE) was calculated by

the method described by Khan (1975) and the similarity factor (f2) was evaluated in order to compare the similarity between the percentage of drug dissolved among the formulations, according to Costa, Lobo (2001); Maggio, Castellano, Kaufman (2008), where the dissolution of a number of samples (n) of reference (Rt) and test (Tt) products are compared in a certain period of time:

$$f2 = 50 * \log \{ [1 + (1/n) \sum_{t=1}^{n} (Rt - Tt)^{2}] 0^{-0.5} * 100 \}$$
 (2)

For the dissolution curves to be considered similar, the f2 value should be between 50 and 100 (Brasil, 2010a).

Characterization of the pellets obtained

Pellets that presented the desired release properties to obtain the biphasic formulations of PROP were analyzed for granulometric evaluation, apparent (AD) and compacted (CD) density, friability, loss by drying, sphericity and evaluation of the external morphology.

For the granulometric evaluation, 100.0 g samples were subjected to the vibrational agitation of 15 Hz for 10 min in a sieve Impact Test Sieve Shaker SV001, using 18, 20, 25, 30 and 35 mesh. The results were expressed in percentage of pellet mass retained in each mesh.

The evaluation of the pellet density was obtained after evaluation of a sample of 50 g in 250 mL graduated measuring cylinder, subjected to 200 beats, with the aid of a compaction densimeter Pharma Test PT-TD200 (Mehta *et al.*, 2012). The friability (%F) was determined according to European Pharmacopoeia (2011), by weighing the mass loss after 960 horizontal oscillations (240 oscilations per minute for 4 min) and determined according to equation (3) (Mehta *et al.*, 2012):

$$F(\%) = \frac{\text{initial weight } (w_1) - \text{final weight } (w_2)}{\text{initial weight } (w_1)} \times 100 (3)$$

^{*} Solvent evaporates during the process.

The moisture content (n=3) was determined in an infrared moisture balance (Mettler-Toledo® HB43-S Halogen), weighing samples of 2.0 g at the maximum temperature of 105 °C till constant mass. The percentage referring to the weight loss was considered as the moisture content of the sample.

Sphericity (S) of the pellets was calculated according to Lovgren and Lundberg (1989), through measurement of the length and width of the bidimensional image of the pellets using 20 units. The format was expressed as a sphericity percentage, where 100% corresponds to a perfect circle.

The evaluation of the external morphology of the pellets was performed through images obtained by scanning electron microscopy (SEM) (Shimadzu®, SS 550 model), at accelerating voltage of 15.0 kV and probe current of 4.0 pA. Samples were placed in a metallic sample holder, fixed with carbon tape, and subsequently coated with a thin layer of gold, using a current of 4 mA for 3 min.

RESULTS AND DISCUSSION

The study of compatibility between the active and the excipients is of fundamental importance, since it can reduce or predict possible complications during the development of the drug (Aulton, Ortega, 2008).

The DSC curves obtained for the PROP and the binary mixtures are showed in Figure 1. The thermogram obtained for the PROP showed a pronounced endothermic peak at 163.73 °C characteristic of its melting point (Sahoo *et al.*, 2008; Farmacopeia Brasileira, 2010). The thermograms obtained from the binary mixtures between excipients and PROP showed no significant alterations of the endothermic peak, indicating a good compatibility between the PROP and the chosen excipients. Samples of the placebo and PROP mixture and the final formulation of PROP also showed no alterations of these peaks, indicating that even after the use of excipients and the preparation process, the characteristics of the drug remained unaltered.

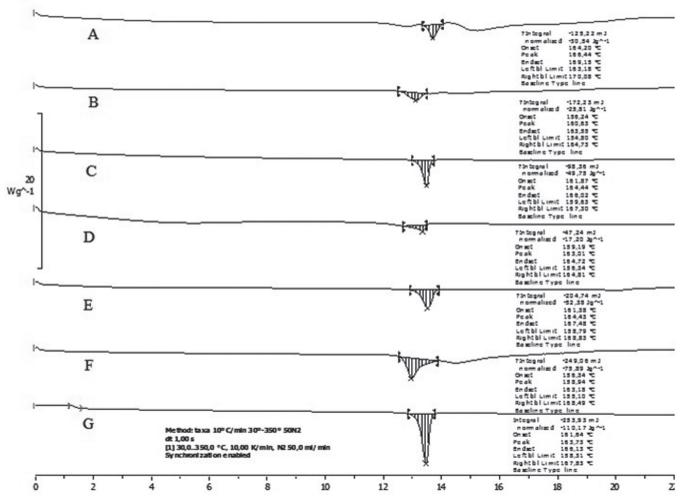


FIGURE 1 - Thermal analysis of DSC A) Final formulation of PROP; B) PROP + Placebo of the pellets; C) PROP + talc; D) PROP + PVP K30; E) PROP + HPMC; F) PROP + EIS; G) PROP.

Although the DSC analysis is the most used in compatibility studies, the interpretation of data provided are not always easy and can lead to misinterpretation of results. Moreover, the results obtained at high temperatures may not be relevant when it comes to room and/or storage temperature being often advisable to use confirmatory techniques, such as FTIR (Liltorp et al., 2011; Tiţa et al., 2011). The results obtained in FTIR analysis are shown in Figure 2. Pure propranolol showed characteristic peaks between 3650-3200 cm⁻¹ (-OH stretch), 3500-3100 cm⁻¹ (N-H stretch), 3100-3000 cm⁻¹ (styrene -CH of aromatics), 1600-1475 cm⁻¹ (aryl C=C stretch), 1240 and 1030 cm⁻¹ asymmetric and symmetrical O-CH₂ stretches, respectively, and at 798 cm⁻¹ due to alpha-substituted naphthalene. Peaks corresponding to pure propranolol in final formulation confirm the absence of interaction among

samples analyzed, since no significant alterations are observed (Srikanth *et al.*, 2012; Saeedi, Morteza-Semnani, Sagheb-Doust, 2013).

Tests from A to D, as described in Table 4, were performed in order to define the most suitable bonding agent in the attainment of immediate release pellets. After obtaining formulation A, it was observed a yield of 85.7% and 86.0% PROP content of the pellets, with the presence of many pellets agglomerated and fine powder inside the equipment during the process, suggesting that the increase in bonding agent, PVPK 30, in the attempt to correct the loss of powder, would worsen the agglomeration of the pellets while its decrease would cause the increase of powder loss. For the formulation B, it was obtained 94.20% yield and PROP content of 84.40%, in this case, it was possible to observe a considerable loss of the active

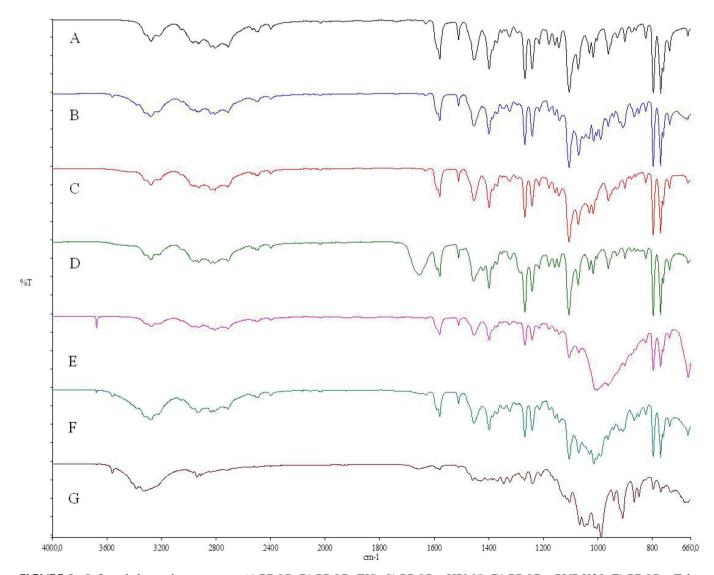


FIGURE 2 - Infrared absorption spectrum A) PROP; B) PROP+EIS; C) PROP + HPMC; D) PROP + PVP K30; E) PROP + Talc; F) PROP + Placebo; G) Final formulation of PROP.

compound, which was confirmed with the presence of large amounts of fine powder inside the fluidized bed. Even obtaining a yield above 90.00% in the test, the PROP content was lower than expected.

In the attempt to solve the problem of powder loss during the coating process of B, C and D, tests were made with increasing amount of the HPMC bonding agent to 2.83 and 3.77% respectively. In test C, it was obtained 98.70% yield and 99.20% content of PROP, while in D, 92.10% yield, and 98.90% content of PROP. Even with the high content presented in the two formulations, formulation D presented lower yield when compared to C. This is possibly because the high concentration of polymer applied may have favored the agglomeration of the pellets during the coating step. Thus, formulation C was selected for following the experiments, due to the best results in the requisites of yield and PROP content values within the expected. The results of yield and content of PROP are listed in Table V.

TABLE V - Results of yield and content of PROP found for the formulations from A to D

| Formulation | Yield (%) | PROP content (%) |
|-------------|-----------|------------------|
| A | 85.70 | 86.00 |
| В | 94.20 | 84.40 |
| C | 98.70 | 99.20 |
| D | 92.10 | 98.90 |

To prevent contact of the drug present in the active coating with the functional coating, a sealing coating layer

was applied onto the active coating pellets (C), originating C1 in order to form a barrier between these two coatings and thus preventing the migration of the active compound to the functional coating and possible problems in the release and stability of the drug (McGinity, Felton, 2008). Besides protection against degradation, this coating allows the correction of defects and/or roughnesses that may exist on the surface of the pellets, allowing the functional coating to be distributed uniformly over the entire surface of the pellets (Prasad *et al.*, 2013).

The modified release pellets were obtained through application of the functional coating, composed of EC and HPMC over the pellets containing seal coating (C1), in order to obtain a 24-hour release profile (1440 min). EC is a polymer derived from cellulose, which has a good capacity to form transparent films, flexible and resistant, however water-insoluble, while HPMC has high solubility in water therefore being much used as pore former in modified release coatings (Rowe, Sheskey, Quinn, 2009).

TEC was used as a plasticizing agent in a concentration of 10.00% in relation to the dry weight of the polymers, aiming to improve the flexibility characteristics of the film, to facilitate its distribution on the surface of the pellets and ensure homogeneity of the applied coating (Bauer *et al.*, 1998).

For the evaluation of dissolution profile of the obtained pellets (Figure 3), it can be observed that C and C1 formulations showed an immediate release profile, since both formulations present average dissolution greater than 75.00% of the active substance within 30 min (Farmacopeia Brasileira, 2010), and the dissolution of C and C1, in 15 min, of $98.16\% \pm 1.13$ and $94.90\% \pm 2.36$,

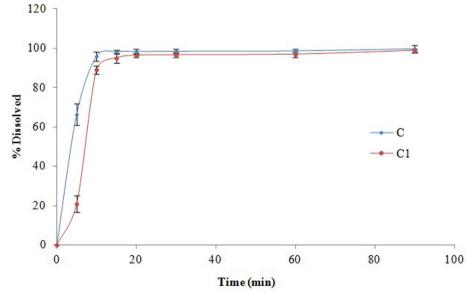


FIGURE 3 - Dissolution profiles of the pellets obtained in C and C1.

respectively. However, even presenting an immediate release, the release profile of these formulations do not present similarity, since f2 = 37.9.

The dissolution profiles obtained from the experimental design (Figure 4) show that F1 and F4 formulations achieve respectively 100.10% and 101.93% of the active compound released within 960 min, showing a 16-hour releasing profile. F2 formulation reaches more than 95.00% of drug release within 30 min, releasing all the active compound loaded in up to 90 min, classifying C as well as C1 in the category of the immediate release. F3 formulation releases only 84.20% of the amount of PROP present in the formulation in 1440 min, indicating that it would take more than 24 hours to release all PROP loaded in the pellets, representing a very slow release profile.

On the other hand, the profiles obtained by the formulations F5, F6 and F7 indicate a 24-hour release profile, reaching the PROP releasing aim during this period. Thus, formulation F5 was randomly chosen to represent the fraction of modified release of the biphasic formulation.

For the formulations F8 (20 mg C1 + 60 mg F5) and F9 (40 mg C1 + 40 mg F5), it was possible to obtain a biphasic release profile (Figure 5), so that F9 presented a faster release profile, when compared to F8 of up to about 600 min, extending the release in both formulations for a period of 24 hours. The dissolution efficiency (DE) values for F8 and F9 formulations were $75.94\% \pm 0.23$ and

 $83.04\% \pm 0.50$, respectively, with f2 = 40. These results show that even with the two formulations presenting release profiles of 24 hours, there was no similarity between them and is still possible to obtain exclusive release profiles according to the pathological need by means of association of pharmaceutical units containing different kinetics of release.

Through the 2² factorial experimental design, it was possible to evaluate qualitatively and quantitatively the statistically significant factors that influence the total time of release of the drug (100%) in the dissolution profiles of the modified release PROP pellets. In the study, we evaluated the independent variables (HPMC and EC) and the interaction between these variables. The results obtained for the experimental design are listed in Table VI.

The highest value for the time of 100 % drug release was obtained with F3 with smaller amount of soluble polymer HPMC (2.00 mg) and greater amount of EC (30.00 mg), about 2400 min. This may be an indication that under these conditions few pores were formed by the soluble polymer HPMC against a great amount of insoluble polymer EC, delaying the release. The lowest value for the time of 100 % active compound release was obtained with formulation F2, with reverse condition, that is, a larger amount of HPMC (6.00 mg) and smaller amounts of EC (30.00 mg). In this condition, the insoluble polymer EC, by being in smaller concentrations, had no significant effect on the PROP release. For the intermediate

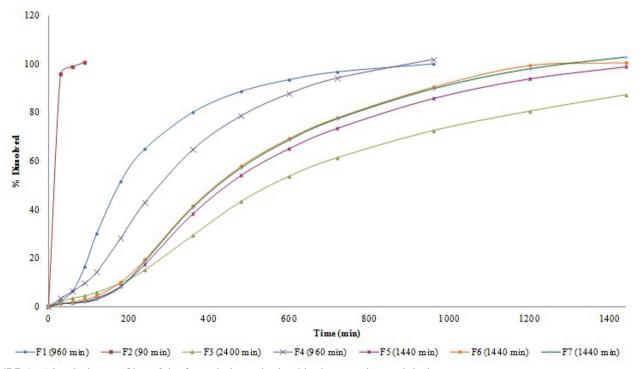


FIGURE 4 - Dissolution profiles of the formulations obtained in the experimental design.

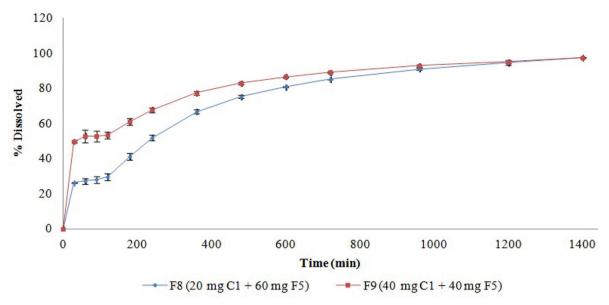


FIGURE 5 - F8 and F9 biphasic release profiles.

TABLE VI - Factorial experimental design 2² for the variables HPMC (mg) and EC (mg) with triplicate at the center point and release response time 100% (min) for the release profile of the pellets of modified release PROP

| | | Real Va | Release | |
|-------------|----------|-----------|---------|-----------------------|
| Formulation | Sequence | HPMC (mg) | EC (mg) | Time 100% (min) |
| F1 | 4 | 2.00 | 10.00 | 960 |
| F2 | 3 | 6.00 | 10.00 | 90 |
| F3 | 5 | 2.00 | 30.00 | 2400 |
| F4 | 2 | 6.00 | 30.00 | 960 |
| F 5 | 6 | 4.00 | 20.00 | 1440 |
| F6 | 1 | 4.00 | 20.00 | 1440 |
| F7 | 7 | 4.00 | 20.00 | 1440 |

conditions, the release was between 960 min (F4) and 1440 min (F5, F6 and F7), this last being considered the optimum point of the study reaching 24 hours of release.

The significance of the factors and model validation were evaluated through analysis of variance (ANOVA). It was possible to observe that both factors, HPMC and EC were significant for a linear model (p < 0.05). The interaction between the variables and the curvature of the model were not significant (p > 0.05). The results of P-value <0.05 indicated that the model is valid at the significance level of 95%.

The value of R²=0.9705 is in accordance with the R²adj=0.9508, confirming this result. The linear model was

constructed through the regression analysis, and describes the relationship between the significant independent variables and the response variable, as described below (equation 4), in which HPMC and EC are expressed in mg and the releasing time in minutes.

Realeasing time
$$100\% = 1102.50 - [(288.75 \text{ x HPMC}) + (57.75 \text{ x EC})]$$
 (4)

The positive coefficient for the amount of EC and negative for HPMC means that a greater amount of EC increases the dissolution time to reach a release of 100%. On the other hand, a higher content of HPMC decreases this time. This is due to the solubility features of each polymer.

The outline map and the response surface for the 100% releasing time is shown in Figures 6a and 6b, respectively. There is no significant curvature, demonstrating that the linear model is valid.

The results obtained after the characterization analyses demonstrate that for the pellets used to obtain the biphasic formulations F8 and F9, both the AD and CD values are similar and that a percentage greater than 90.00% of these same pellets were retained between the 25-20 meshes (Table VII), evidencing good homogeneity of these parameters. All the samples presented moisture values lower than 5.00%, specification recommended by Mehta *et al.* (2012) and friability < 0.40%, indicating acceptable values according to the data present in the literature (Déo, Andreazza, Possamai, 2011). After the evaluation of the external morphology of the pellets (Figure 7), it was observed the smoothing of the C1 surface

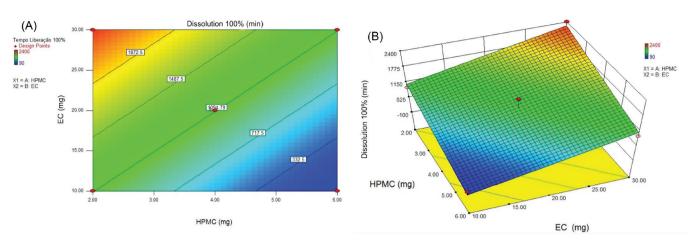


FIGURE 6 - Outline map A) and response surface B) for the experimental results of factorial experimental design 2². Response release time 100% (min) according to the amount of HPMC (mg) and EC (mg).

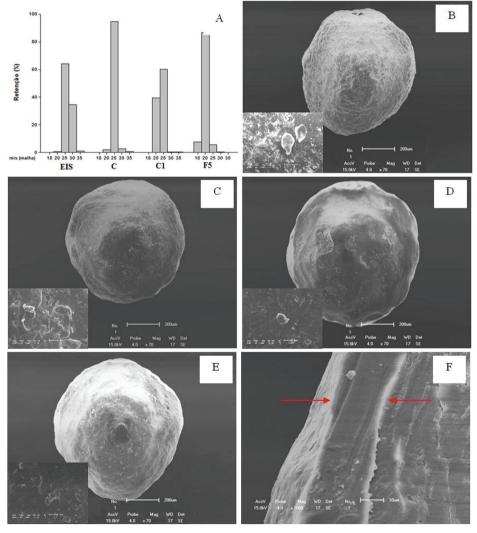


FIGURE 7 - Granulometric and external morphology analysis of pellets A) Granulometric analysis of the EIS and the pellets coated C, C1 and F5; B) Evaluation of the external morphology of the EIS in increase of 70x and 1000x; C) Evaluation of external morphology of C in increase of 70x and 1000x; D) External morphology evaluation of C1 in increase of 70x and 1000x; E) External morphology evaluation of F5 in increase of 70x and 1000x; F) Transversal image of F5 in increase of 1000x with emphasis in the coating layer of the pellet.

TABLE VII - Characterization analyses of pellets obtained

| D | Samples | | | | |
|-------------------------|-------------------|-------------------|-------------------|-------------------|--|
| Parameter — | EIS | С | C1 | F5 | |
| AD (g/mL) | 0.82 | 0.82 | 0.79 | 0.77 | |
| CD (g/mL) | 0.85 | 0.87 | 0.85 | 0.82 | |
| Sphericity \pm DP | 98.07 ± 0.012 | 98.22 ± 0.013 | 98.93 ± 0.006 | 99.02 ± 0.009 | |
| Loss by drying (%) ± DP | 3.09 ± 0.12 | 1.25 ± 0.07 | 1.17 ± 0.10 | 1.66 ± 0.11 | |

after sealing coating when compared to the surfaces EIS and C and homogeneity of the polymeric coating performed in F5.

Additionally, the thickness of the polymeric coating seems to be distributed uniformly throughout the surface of the pellet, which can be attributed to the good sphericity presented by the pellets (Table VII).

CONCLUSION

Thus, from our findings, it was possible to obtain a multiparticulate biphasic release system with the polymeric coating consisting of HPMC and EC, with quality within expected standards. The used 2² factorial experimental design allowed the optimization of the development stage, once it resulted in the 24-hour desired releasing profile with a small number of experiments. Furthermore, it was observed that the biphasic formulations F8 and F9, which are a combination of different releasing forms, ensure different releasing profiles, allowing the therapeutic adjustment according to the pathological needs.

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