SORPTION OF OIL POLLUTION BY ORGANOCLAYS AND A COAL/MINERAL COMPLEX

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Abstract - Recently, increasing concern about pollution of groundwater by organic chemicals has led to research on the use of various adsorbents. This study addressed the sorption of phenol and organic compounds by two organoclays and a coal/mineral complex (ARO). The organoclays used were a bentonite from Brazil (SVC) and Wyoming bentonite (SWy) with quaternary ammonium salt (ABDMA). Swelling capacity of the sorbents in toluene, diesel, gas, Varsol and kerosene were measured. Absorption of organic compounds served as an ASTM D 281-95 base, which resulted in the following order for ABDMA-SVC: gas > toluene > kerosene > diesel > Varsol. ABDMA-SWy absorbed in the following order: gas > toluene > Varsol > diesel > kerosene. ARO absorbed: gas > toluene > diesel > Varsol > kerosene. Sorption of phenol followed the order of ABDMA-SVC > ABDMA-SWy > ARO. The adsorption data show that the materials prepared were effective in sorbing phenol, and that the Brazilian clay was the most efficient of the three materials.

Keywords: adsorption, sorption, absorption, organoclay, hydrocarbon, phenol.

INTRODUCTION

Soil and water contamination by hydrocarbons from leaking storage tanks and improper disposal of hazardous wastes are of concern worldwide. Petroleum hydrocarbons are responsible for 65% of all contaminated groundwater sites (EPA/540/R-95/508b). Treatment of petroleum contaminated sites is a subject of almost unlimited scope. Sites can be as simple as a corner service station with little contamination to a refinery contaminated with hundreds of compounds over every square inch of ground.

Underground petroleum storage tank systems (USTs) have been buried since the early decades of the twentieth century. Not until the mid-1970s did anyone seriously consider the fact that these buried USTs might be leaking gasoline into the environment. The fact that approximately 85% of all USTs were steel with little or no corrosion protection went unnoticed (Cole, 1994).

If proper remediation measures are not taken, the
organic pollutants released from gasoline spills can lead to surface and groundwater contamination, which can be potentially toxic to biota and humans.

Phenolic compounds, generated by petrochemical and petrochemical, coal conversion and phenol-producing industries, are common contaminants in wastewater. Thus, it is necessary to identify, characterize and develop effective cleanup or containment methods for these hazardous contaminants.

Organoclays have attracted considerable attention for their use in contaminant treatment (Xu et al., 1997). Due to the isomorphous substitutions in the aluminosilicate layers, natural clay minerals usually have a net negative charge, which is balanced by alkali metal and alkaline-earth-metal cations such as Na⁺ and Ca²⁺. The strong hydration of these inorganic cations creates a hydrophilic environment on the surface and in the interlayer region of natural smectites (Souza Santos, 1992). The substitution of Na⁺ or Ca²⁺ by quaternary ammonium cations of the form [(CH₃)₃NR]+ or [(CH₃)₂NRR']⁺ at the exchangeable sites of natural clays results in organoclay derivatives with organophilic properties that can act as sorbent contaminant hydrocarbons (Büchler, 1986a, 1986b; Jaynes and Boyd, 1990; Xu and Boyd, 1995). Organoclays are effective sorbents for a variety of aqueous organic compounds, including many common groundwater contaminants (Boyd, et al., 1988a, 1988b; Lee et al., 1989, 1990; Sharmasarkar et al., 2000).

The use of organoclays in conjunction with conventional bentonite clay provides a barrier with the combined ability to act as a sealant and to effectively adsorb and retain dissolved organic contaminants. This type of composite liner provides an additional barrier to the escape of chemicals from storage tanks and landfills and represents a fundamental improvement in liner technology (Jaynes and Boyd, 1990).

Organoclays formed with quaternary ammonium salts such as trimethylphenylammonium (TMPA) or hexadecyltrimethylammonium (HDTMA) from smectites were more effective sorbents for phenol and chlorophenols than unmodified smectite. Sorption of phenol was maximized when water and then clays were left to settle overnight. The clay supernatant was removed and mixed with an aqueous solution of ABDMA chloride salt in the amount of 100 meq ABDMA per 100 g of the clays and stirred for 20 minutes. The ABDMA-smectite complexes were vacuum filtered and stored at room temperature.

The ARO was prepared at Department of Metallurgical and Materials Engineering, Polytechnic School, University of São Paulo, São Paulo, Brazil, (PMT/EPUSP).

The diesel, gas and kerosene were obtained from Petróleo Brasileiro S. A. (Petrobrás).

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varsol is a commercial mixture of low-molecular-weight aliphatic hydrocarbons.
Basal spacings were determined by X-ray diffraction (XRD) analysis. X-ray diffraction patterns were recorded using CuKα radiation (λ = 1.5416 Å) and a Philips XPERT-MPD X-ray diffractometer in steps of 0.02°/step.

Adsorption isotherms were determined using the batch equilibration technique. The initial concentrations of phenol were prepared in the range of 200 to 800 mg/L. Glass tubes (35 mL) containing 500 mg of organoclays and 25 mL of phenol aqueous solutions were closed and mixed. Every batch stood for 24 hours at 33 °C. Preliminary kinetic work indicated that sorption equilibrium was reached in less than 20 hr. After reaching equilibrium, the aqueous phase was separated by centrifugation at 3000 rpm for 60 min at room temperature using a BE-4004 type BIO-ENG. A 10 mL portion of the supernatant was analyzed by the total organic carbon method (TOC) with a TOC-5000 A type Shimadzu in order to measure concentration of phenol equilibrium. The amounts of phenol adsorbed were calculated by the differences between the initial and equilibrium concentrations. Isotherms were obtained by plotting the amounts adsorbed against the equilibrium concentration in solution. All experiments were carried out in duplicate and each point on the isotherm is the average of two experiments.

The absorption of organic compounds served as an ASTM D 281-95 base. All experiments were carried out in duplicate.

The swelling capacity of organophilic clays in toluene, diesel, kerosene, gas and Varsol, was measured, as described previously by Valenzuela Díaz (2001).

RESULTS AND DISCUSSION

Swelling

Table 1 shows the swelling of the organoclays. Intermediate values (between 6 to 8 mL/g) were observed for the swelling in toluene and gas, attesting the organophilicity of the clays.

The organoclays had low (below 5 mL/g) or intermediate values for swelling in organic compounds. The ABDMA-SVC had low values for swelling in diesel (without mixing) and intermediate values for swelling in diesel with mixing, in gas with and without mixing and in toluene without mixing. The ABDMA-SVC had high values for swelling in toluene with mixing. The ABDMA-SWy had low swelling in diesel and in gas both with and without mixing and middle swelling in toluene with and without mixing. All the organoclays had swelling below 3 mL/g in Varsol and kerosene.

Table 1: Swelling of organoclays (mL/g).

<table>
<thead>
<tr>
<th>Organoclays</th>
<th>( n_f )</th>
<th>( K_f (L/mg) )</th>
<th>( R^2_f )</th>
</tr>
</thead>
<tbody>
<tr>
<td>ABDMA-SWy</td>
<td>1.5260</td>
<td>1.2893</td>
<td>0.9472</td>
</tr>
<tr>
<td>ABDMA-SVC</td>
<td>1.6152</td>
<td>1.0002</td>
<td>0.9924</td>
</tr>
<tr>
<td>ARO</td>
<td>2.5529</td>
<td>0.5121</td>
<td>0.9457</td>
</tr>
</tbody>
</table>

Infrared Curves

Figure 1 shows the infrared curves for ABDMA-SVC and ABDMA-SWy. The infrared curves showed the groups NH, CH₃ and CH₂, indicating that the cationic quaternary ammonium molecules were intercalated between the clay mineral layers.

X-Ray Diffraction Analysis

Figure 2 shows the interlayer spacings of the ABDMA-SVC and ABDMA-SWy. All the organoclays were pretreated at 60°C, 110°C and 350°C. The X-ray diffraction basal spacings (d₀₀₁) of the ABDMA-SVC and ABDMA-SWy were between 12.60 and 22.15 Å. The basal spacings of the ABDMA-SVC were slightly larger than those of the ABDMA-SWy. The basal spacings of the natural clays were approximately 12 Å. The X-ray diffraction analysis of the organoclays showed that the interlayer basal spacing of the natural clays was low in comparison to that of the organoclays. The structure of the organoclays did not collapse at 350°C.
Absorption

The absorption of organic compounds served as an ASTM D 281-95 base. Table 2 shows the results for ABDMA-SVC, ABDMA-SWy and ARO. The order of ABDMA-SWy absorption was gas > toluene > Varsol > diesel > kerosene. The order of ABDMA-SVC absorption was gas > toluene > kerosene > diesel > Varsol. The order of ARO absorption was gas > toluene > diesel > Varsol > kerosene.

The data showed that the ABDMA-SVC absorbed more gas (32.71%) and kerosene (22.54%) than did the ABDMA-SWy. The ARO absorbed more diesel (5.95%) than the ABDMA-SVC and more toluene (8.47%) than the ABDMA-SWy.

Sorption of Phenol

Sorption of phenol (Figure 3) occurred in the following order: ABDMA-SVC > ABDMA-SWy > ARO.

The Langmuir and Freundlich models are the most frequently employed models. Banat (2000) used both models to describe the relationship between the amount of phenol adsorbed and its equilibrium concentration. A comparison of correlation of the data ($R^2$) values indicated that the data would better fit with the Freundlich model than the Langmuir equation (Banat, 2000).

In this work the data were fitted to the Freundlich model, resulting in greater correlation of the data ($R^2$). The Freundlich equation can be expressed as follows:

$$y = K_f C_e^{n_f}$$

Freundlich equation

where $K_f$ (L / mg) and $n_f$ (dimensionless) are constants related to sorbate-binding capacity and a conditional index that describes the shape of the isotherm, respectively. The results of fitting models to phenol sorption on organoclays are listed in Table 2. The $n_f$ values were high than 1 for the three organoclays. Freundlich fitting with $n_f > 1$ would indicate conformity of the data to multilayer formation at the adsorbent surfaces. This observation could also be attributed to the molecular interactions between the sorbate species and subsequent aggregation in the pattern of the surface monolayer. These mechanistic paths could be possible attributes of the conformity of our data with the Freundlich fitting. The $n_f$ values that are high than 1 represent sorption results having convex curvatures (Sharmasarkar et al., 2000). Isotherms for ABDMA-SVC, ABDMA-SWy and ARO followed a convex up pattern. Banat et al. (2000) used natural bentonite to absorb phenol. He concluded that its adsorptive capacity was limited (on an order of magnitude of 1 mg/g).

Validation of the models for adsorption of phenol by organoclays was confirmed by testing the $R^2$ (correlation coefficient).

**Figure 1:** Infrared curves.
**ABDMA-SVC (350°C)**  
\(d_{001}=12.60\ \text{Å} \)

**ABDMA-SVC (110°C)**  
\(d_{001}=18.58\ \text{Å} \)

**ABDMA-SVC (60°C)**  
\(d_{001}=22.15\ \text{Å} \)

**SVC Natural (60°C)**  
\(d_{001}=15.20\ \text{Å} \)

**ABDMA-SWy (350°C)**  
\(d_{001}=12.78\ \text{Å} \)

**ABDMA-SWy (60°C)**  
\(d_{001}=17.65\ \text{Å} \)

**ABDMA-SWy (110°C)**  
\(d_{001}=17.37\ \text{Å} \)

**SWy Natural (60°C)**  
\(d_{001}=13.2\ \text{Å} \)

ABDMA-SVC = alkyl benzyl dimethyl ammonium.  
SWy = Wyoming bentonite.  
SVC = bentonite from the Brazilian state of Paraiba.  
\(d_{001}\) = basal spacing.

**Figure 2:** X-ray diffraction curves.

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**Equilibrium concentration (mg/L) vs. Amount adsorbed (mg/g)**

**ABDMA-SVC**  
\(y = 1.2893x^{0.6553}\)  
\(R^2 = 0.9472\)

**ABDMA-SWy**  
\(y = 1.0002x^{0.6191}\)  
\(R^2 = 0.9924\)

**ARO**  
\(y = 0.5121x^{0.0017}\)  
\(R^2 = 0.9457\)

ABDMA = alkyl benzyl dimethyl ammonium.  
SWy = Wyoming bentonite.  
SVC = bentonite from the Brazilian state of Paraiba.  
ARO = coal/mineral complex.

**Figure 3:** Adsorption isotherms and Freundlich equation.
Table 2: Absorption (g organic compound/g material).

<table>
<thead>
<tr>
<th>Organoclays</th>
<th>Swelling without mixing (mL/g)</th>
<th>Swelling with mixing (mL/g)</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>diesel</td>
<td>gas</td>
</tr>
<tr>
<td>ABDMA-SWy</td>
<td>3</td>
<td>3</td>
</tr>
<tr>
<td>ABDMA-SVC</td>
<td>4</td>
<td>6</td>
</tr>
</tbody>
</table>

Table 3: Model parameters for phenol adsorption by organoclays.

<table>
<thead>
<tr>
<th>Organoclays</th>
<th>diesel</th>
<th>gas</th>
<th>kerosene</th>
<th>Varsol</th>
<th>toluene</th>
</tr>
</thead>
<tbody>
<tr>
<td>ABDMA-SWy</td>
<td>0.85</td>
<td>1.44</td>
<td>0.79</td>
<td>0.93</td>
<td>1.08</td>
</tr>
<tr>
<td>ABDMA-SVC</td>
<td>0.79</td>
<td>2.14</td>
<td>1.02</td>
<td>0.72</td>
<td>1.47</td>
</tr>
<tr>
<td>ARO</td>
<td>0.84</td>
<td>1.38</td>
<td>0.76</td>
<td>0.78</td>
<td>1.18</td>
</tr>
</tbody>
</table>

ABDMA = alkyl benzyl dimethyl ammonium.
SWy = Wyoming bentonite.
SVC = bentonite from the Brazilian state of Paraíba.
ARO = coal/mineral complex.

CONCLUSIONS

The infrared curves (Figure 1) showed groups NH, CH₂ and CH₃. The X-ray diffraction basal spacings (d₀₀₁) of the ABDMA-SVC was 22.15 Å and ABDMA-SWy was 17.65 Å at 60°C. The basal spacings of the natural clays are approximately 12 Å at 60°C. These facts indicate that the cationic quaternary ammonium molecules became intercalated between the clay mineral layers.

The ABDMA-SVC and ABDMA-SWy adsorption curves for phenol indicate that these organoclays were effective in adsorbing the phenol and can be used as liners and waste disposal reservoirs. The Freundlich isotherms were found to be applicable for the adsorption equilibrium data.

The ABDMA-SVC and ABDMA-SWy data for diesel, gas, kerosene, toluene and Varsol suggests that these organoclays can be utilized more effectively as liners around gasoline storage tanks and waste disposal reservoirs for the purpose of hydrocarbon-containment and controlling pollution from petroleum-contaminated waters.

The data showed that the Brazilian clay is the most efficient of the three materials studied.

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REFERENCES


