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# Use of agricultural and agroindustrial residues as alternative adsorbents of manganese and iron in aqueous solution

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# **ABSTRACT**

The increase in the volume of agricultural and agroindustrial waste, associated with improper disposal, is a growing worldwide problem. The recovery of those residues is of crucial importance, since it reduces environmental impacts, protects public health, and allows the addition of value to the materials. One of the ways of exploiting adsorbents is related to the capacity of some wastes to be used as alternative adsorbents in the efficient removal of microcontaminants in aqueous systems. This work assessed the use of agricultural and agroindustrial residues: maize straw, wheat straw, soybean straw and soybean hulls for the production of alternative adsorbents to remove iron (Fe) and manganese (Mn) in water. For each residue investigated, two different polymers were obtained for use as adsorbents, a natural polymer (cellulose/lignin) and an EDTA-modified polymer (ethylenediaminetetraacetic acid). The adsorbents were characterized through FTIR (Fourier transform infrared spectroscopy) and nitrogen content. To evaluate the efficiency of the adsorbents, kinetic tests in batch mode and determination of Lagergren pseudo-first and pseudo-second order kinetic constants were performed. The results found that the modified polymer obtained from soybean hulls (SHE) showed increased Fe (96%) and Mn (88%) removal rate, in which the pseudo-second order kinetic model presented closer results between the experimental adsorption rates and the calculated ones for the two microcontaminants under study. In general, the modified soybean hulls proved to be a promising alternative adsorbent for the removal of iron and manganese in water treatment.

**Keywords:** adsorption, agribusiness, microcontaminants, waste recovery.



# Uso de Resíduos Agrícolas e Agroindustriais como Adsorventes Alternativos de manganês e ferro em Sistema Aquoso

#### **RESUMO**

O aumento do volume de resíduos agrícolas e agroindustriais gerados, acompanhados do descarte inadequado dos mesmos é um problema mundial crescente. O aproveitamento desses resíduos é de extrema importância, já que resulta na redução de impactos ambientais, preservação da saúde da população, e permite agregar valor à esses materiais. Uma das formas de aproveitamento está relacionada à capacidade de alguns resíduos serem utilizados como adsorventes alternativos na remoção eficiente de micro-contaminantes em sistemas aquosos. Este trabalho teve como objetivo investigar o uso dos resíduos agrícolas e agroindustriais: palha de milho, palha de trigo, palha de soja e casca de soja para produção de adsorventes alternativos para remoção de ferro (Fe) e manganês (Mn) em água. Para cada resíduo investigado, dois diferentes polímeros foram obtidos para uso como adsorventes, um polímero natural (celulose/lignina) e um polímero modificado com EDTA (ácido etilenodiaminotetraacético). Os adsorventes foram caracterizados por FTIR (espectroscopia de infravermelho por transformada de Fourier) e teor de nitrogênio. Para a avaliação da eficiência dos adsorventes foram realizados testes cinéticos, em regime batelada, e determinação das constantes cinéticas de pseudo-primeira e pseudo-segunda ordem de Lagergren. Os resultados obtidos indicaram que o polímero modificado obtido da casca de soja apresentou maior remoção de Fe (96%) e Mn (88%), em que o modelo cinético de pseudo-segunda ordem apresentou resultados mais aproximados entre os valores de quantidade adsorvida experimentais e os calculados para os dois micro-contaminantes em estudo. De modo geral, a casca de soja modificada mostrou ser um adsorvente alternativo promissor para a remoção de ferro e manganês no tratamento de

Palavras-chave: adsorção, agroindústria, aproveitamento de resíduos, micro-contaminantes.

# 1. INTRODUCTION

Water is a basic necessity worldwide and is of immeasurable environmental importance since it is the primitive requirement for human life (Bushra et al., 2017, Carolin et al., 2017). Inorganic and organic chemicals are major life-threatening factors of water pollution (Sharma et al., 2017). Metal ion pollution is a most concerning topic of investigation in the present era due to its alarming rate of increase (Naushad et al., 2016). Domestic and industrial wastewaters containing metal ions are increasingly discharged into the environment and these metal ions are of significant importance as they are not biodegradable and cannot be metabolized by the environment but tend to accumulate in living organisms, causing various diseases and disorders (Hasanzadeh et al., 2017). Most of the metals are carcinogenic and/or pose severe health problems, such as organ damage, reduced growth and development, oxidative stress, and nervous system impairments (Naushad et al., 2015).

The presence of micro contaminant compounds in groundwater, and eventually in drinking water, is a serious environmental problem which poses a substantial risk to local resource users and to the natural environment (Adekola et al., 2016). For example, iron overload in animal models and humans increases oxidative stress and induces cardiomyopathy that may contribute to increased cardiovascular risk (Marques et al., 2015). Manganese (Mn) might be toxic at excess exposure. Elevated concentrations of Mn in drinking water were associated with impaired child development and indicated an adverse effect on birth length in pregnant women (Rahman et al., 2015). In order to get safe drinking water, excessive iron and manganese must be removed (Rangreez et al., 2017).



The removal of toxic metals from water and wastewater has been achieved by several processes such as coagulation, electrochemical treatment, ion exchange, membrane separation, chemical precipitation and adsorption (Alqadami et al., 2016, Naushad et al., 2017, Reiad et al., 2012). In the last decade, the adsorption technique has been widely used for the removal of toxic metal from aqueous mediums (Ahamad et al., 2017) and has become one of the most preferred methods due to its high efficiency and low operational cost, making it a cost-effective method (Al-Othman et al., 2012). Furthermore, based on the regeneration, since adsorbents can be recreated by the desorption process, adsorption is also considered an environmentally acceptable method.

The selection of suitable precursors for the adsorption of metal ions from aqueous solutions is very important (Alqadami et al., 2017). The biosorption process using agricultural waste/plant material is an eco-friendly and easy method. Rapid industrialization associated with the population growth and intensive agricultural activities has prompted an increase in the amount and variety of agricultural and agroindustrial wastes produced (Asim et al., 2015). Most agricultural waste consists of three main structural components: lignin, cellulose and hemicellulose. These compounds possess adsorptive sites, such as ether, carbonyl, carboxyl, amine and hydroxyl groups, capable of absorbing metal species through ion exchange or complexation processes (Salleh et al., 2011).

Many agricultural wastes have directly or indirectly been used as sorbents for metal adsorption from water and wastewater which included rice husk, sunflower, potato, canola and walnut shell residues (Feizi and Jalili, 2015), peanut shell and orange peel (Surovka and Pertile, 2017).

In the light of the above, the present study investigated the use of agricultural and agroindustrial maize, soybean and wheat residues for producing alternative adsorbents, and their application in the removal of iron and manganese from aqueous solution.

# 2. MATERIALS AND METHODS

#### 2.1. Agricultural and Agroindustrial Waste

Maize straw (MS), wheat straw (WT) and soybean straw (SS) soil residues were collected directly in the field after the harvest of the crops, respectively, in rural properties located in Campo Mourão, State of Paraná, Brazil and Peabiru, State of Paraná, Brazil, which use the notillage technique. Agroindustrial soybean hulls (SH) residues were provided by the COAMO – Agroindustrial Cooperativa warehouse located in the city of Araruna, PR, Brazil.

#### 2.2. Preparation of Adsorbents

From each agricultural and agroindustrial residue, hemicelluloses were extracted to obtain a polymer composed of cellulose and lignin, known as a natural adsorbent of maize straw (MS), wheat straw (WT), soybean straw (SS) and soybean hull (SH). The stages of preparation and getting of e natural adsorbents followed the methodology described by Schafhauser et al. (2015).

For each residue, preparation of the adsorbent consisted of drying at 60°C in an oven for 24 h, grinding with a cutting mill and screening (10 mesh).

Subsequently, for hemicellulose removal, 30 g of the sample were weighed on an analytical balance and the extraction was carried out following an eluotropic series of solvents (n-hexane/alcohol/water) in Soxhlet-type extractors with a hot plate. After extraction using each solvent of the series, the residues were dried in an oven at 60°C for 24 h, weighed and returned to the Soxhlet system for further extraction with the other solvents. After extraction with water,



the material was dried and weighed and the hemicellulose-free natural polymer composed of cellulose and lignin, i.e., the natural adsorbent, was obtained.

Part of this product (natural adsorbent) was put aside and the other part was modified with EDTA (ethylenediaminetetraacetic acid) to obtain a modified polymer called modified maize straw (MSE), wheat straw (WTE), soybean straw (SSE) and soybean hulls (SHE) adsorbent, obtained from the natural adsorbent.

The introduction of EDTA into the cellulose fibers of the adsorbents was carried out in a 50 mL round-bottomed flask fitted with a ball condenser. Each flask contained 5 g of natural adsorbent, 15 g of disodium salt EDTA and 210 mL of DMF (dimethylformamide). The mixture was stirred and heated on a magnetic stirrer with a heating plate at 75°C for 24 h and then vacuum-filtered on a sintered plate funnel with porosity of 40-60 µm. The material trapped on the filter was subjected to sequential washing with solvents and then dried at 75°C for 24 h on a drying oven until constant mass, in order to obtain EDTA-modified natural polymer (Pereira et al., 2010).

#### 2.3. Characterization of Adsorbents

In order to characterize the adsorbents, they were weighed in an analytical balance, followed by a FTIR analysis (Fourier transform infrared spectroscopy) and total nitrogen determination.

For the FTIR analysis performed on a FTIR (IRAffinity-1S, Shimadzu) spectrometer, the pellets were prepared using 1 mg of adsorbent and 100mg of spectroscopic grade KBr. The spectra were collected over the 4000 to 400 cm<sup>-1</sup> wavenumber range at a resolution of 4 cm<sup>-1</sup> and 32 scans.

The determination of total nitrogen was carried out using the Kjeldahl method.

The analyses of the elements C, H, N and O for SHE and SS were carried using an elemental analyzer Eurovector EA 3000-S.

# 2.4. Kinetic Study

Kinetic tests of Fe or Mn adsorption in aqueous solution, in batch mode, were performed for each of adsorbent obtained. For each test, 20 mL of metal (Fe or Mn) standard solution (1g.L<sup>-1</sup>), 1980 mL of distilled water and 3 drops of nitric acid were added to 4 g of adsorbent, resulting in a solution of 10 mg.L<sup>-1</sup> for metal species and a concentration of 2 mg.mL<sup>-1</sup> of adsorbent material in solution. The solution was continuously stirred at 160 rpm, and kept at 25°C and pH of 6.8. The adsorption time ranged from 0 to 180 min, in which 20 mL-aliquots were collected at predetermined intervals, followed by sample filtration in a sintered glass filter and the analysis of the Fe or Mn concentration through atomic absorption spectrophotometry, using an Analytik Jena NOVAA300 spectrophotometer.

The amount of Fe and Mn adsorbed (q), in mg.g<sup>-1</sup>, was calculated by Equation 1:

$$\mathbf{q} = \frac{(\mathsf{C}_0 - \mathsf{C}_\mathsf{e})\mathsf{V}}{\mathsf{m}} \tag{1}$$

in which  $C_0$  and  $C_0$  and  $C_0$  correspond to the initial concentration of the micro-contaminant and the equilibrium concentration (mg.L<sup>-1</sup>), respectively; V is the volume of solution (L) and m is the amount of adsorbent used (g).

The adsorption efficiency of Fe and Mn from the aqueous solution was calculated by Equation 2:

$$\% Adsorbed = \frac{c_0 - c_e}{c_0} \times 100 \tag{2}$$



The results of the kinetic tests were fitted to Lagergren pseudo-first and pseudo-second order kinetic models (Equation 3 and 4):

$$\log(\mathbf{q}_{e} - \mathbf{q}_{t}) = \log \mathbf{q}_{e} - \frac{\mathbf{k}_{1}}{2,303} \mathbf{t}$$
 (3)

$$\frac{\mathbf{t}}{\mathbf{q_t}} = \frac{1}{\mathbf{k_2} \mathbf{q_e^2}} + \frac{\mathbf{t}}{\mathbf{q_e}} \tag{4}$$

in which  $q_e$  and  $q_t$  are the adsorbed quantities  $(mg.g^{-1})$  at equilibrium and time t, respectively;  $k_1$  is the pseudo-first order adsorption constant  $(min^{-1})$  and  $k_2$  is the pseudo-second order adsorption constant  $(g.mg^{-1}.min^{-1})$ .

# 3. RESULTS AND DISCUSSION

#### 3.1. Collection of Adsorbents

Table 1 shows the quantity and the respective percentage of extracts (hemicelluloses) removed in each extraction step using the eluotropic series of different solvents for each waste assessed.

**Table 1.** Waste weight before and after extractions using the eluotropic and total percentage rate of extractives removed.

| Waste | Initial weight (g) | Weight   | after extract | ion (g) | Final weight (g) | Percentage of<br>Removed<br>Extracts (%) |
|-------|--------------------|----------|---------------|---------|------------------|--|
|       |                    | Ext      | raction solve | nt      |                  |  |
|       |                    | N-Hexane | Ethanol       | Water   |                  |  |
| MS    | 30.00              | 28.35    | 25.75         | 20.95   | 9.05             | 30.17                                    |
| WT    | 30.00              | 28.00    | 26.15         | 21.00   | 9.00             | 30.00                                    |
| SS    | 30.00              | 28.13    | 25.74         | 20.35   | 9.65             | 32.17                                    |
| SH    | 30.00              | 26.00    | 24.10         | 19.25   | 10.75            | 35.83                                    |

The process of removing extractives from the adsorbent material is an extremely important step when one aims at performing adsorption in aqueous solution, since hemicellulose, which is the most soluble constituent among lignocellulosic biomass materials, must be completely removed from the medium in order to prevent its solubilization and, consequently, the complexation of microcontaminants and the impairment of the final adsorption result. This process also avoids fungal and bacterial attack, increasing the useful life of adsorbent materials.

At the end of the process, all agricultural byproducts showed a reduction in total weight, demonstrating their efficiency in the extraction process. The biggest extraction occurred with SS (35.83%).

Similar results were reported by Schafhauser et al. (2015) in extractions using the same solvents, in the same order, in maize straw. The authors observed that, at the end of the process, the total percentage of extractives removed was 30.15%.

In order to obtain modified adsorbents, part of the natural adsorbents (MS, WT, SS, SH) were subjected to chemical modification with EDTA, followed by filtration, washing and drying. After those steps, the weight gain of modified adsorbents (MSE, WTE, SSE, SHE) was assessed to verify the EDTA's inclusion in the adsorbent materials: 10.75% for MSE, 11.00% for WTE, 8.80% for SSE and 33.00% for SHE.

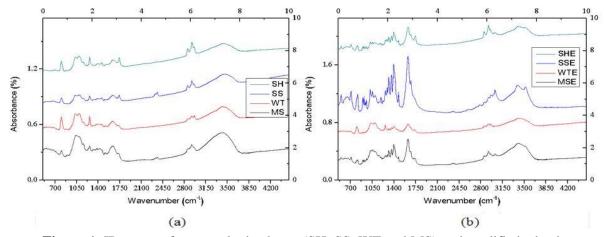
Weight gain was observed in the four types of adsorbent materials after modifications with EDTA, confirming the introduction of this chelating agent into the structures of the lignocellulosic fibers forming straws and hulls.



EDTA is a biodegradable and active agent containing two anhydride groups per molecule that can be used to introduce chelating abilities to the lignocellulosic materials through esterification reaction. This reaction allows introducing carboxylic and amine functional groups that present high ability to form stable complexes with heavy metal ions (Pereira et al., 2010). Therefore, the weight gain observed in modified adsorbent materials confirms that the carboxylate functions have been released and the amine functions have been conveyed into them.

# 3.2. Fourier Transform Infrared Spectroscopy

IR spectra for natural and modified adsorbents obtained are shown in Figures 1 (a) and (b), respectively. A comparison between the spectra revealed an increase and the appearance of strong bands in EDTA-modified straws and hulls at 1743-1747 cm<sup>-1</sup>, which can be attributed to the axial deformation C = O of ester, at 1633 cm<sup>-1</sup> due to the asymmetric axial deformation of the carboxylate, and at 1402-1408 cm<sup>-1</sup> due to the symmetrical axial deformation of the carboxylate. This finding evidences the incorporation of two types of carbonyls, ester and carboxylate, and also confirms the introduction of EDTA into the modified adsorbents.



**Figure 1.** IR spectra for natural adsorbents (SH, SS, WT and MS) and modified adsorbents (SHE, SSE, WTE and MSE).

The results obtained in the present study are consistent with those reported by Pereira et al. (2010), who characterized through FTIR wood sawdust, EDTA-modified wood sawdust (SE), sugarcane bagasse (B) and EDTA-modified sugarcane bagasse (BE). When comparing the spectra of the modified materials with those of the starting materials, they observed the appearance of strong bands at 1742 cm<sup>-1</sup> for SE and at 1741 cm<sup>-1</sup> for BE, which correspond to stretching ester vibration. They also observed the presence of strong bands at 1634 cm<sup>-1</sup>, 1596 cm<sup>-1</sup> and 1403 cm<sup>-1</sup> for SE and at 1633 cm<sup>-1</sup>, 1602 cm<sup>-1</sup> and 1406 cm<sup>-1</sup> for BE, related to asymmetric and symmetrical stretch of the carboxylate ion, respectively. These bands indicate that EDTA was introduced via ester linkages accompanied by a release of carboxylic functional groups.

Gusmão et al. (2013) studied the adsorption of methylene blue (MB) and gentian violet (GV) in aqueous solution with unmodified sugarcane bagasse (B) and sugarcane bagasse modified with EDTA dianhydride (EB). When comparing the infrared spectra of EB with the unmodified bagasse spectrum, they observed the appearance of strong bands at 1741 cm<sup>-1</sup>, which can be attributed to the axial deformation of the ester bond (-O-C=O), and bands at 1633 and 1406 cm<sup>-1</sup>, which are probably due to axially asymmetric and symmetrical deformations of carboxylate (-COO<sup>-</sup>). These bands confirmed the introduction of EDTA

dianhydride through the formation of ester bonds with the subsequent release of carboxylate functions.

#### 3.3. Determination of Total Nitrogen

Data related to nitrogen analysis are presented in Table 2. A considerable increase in the nitrogen content after chemical modification with EDTA is observed. This finding also helps to confirm the introduction of EDTA in the materials through the incorporation of nitrogen in the modified adsorbents (WTE, MSE, SSE and SHE).

**Table 2.** Nitrogen content (%) of natural and modified adsorbents.

| Adsorbents | Nitrogen (%) |  |  |  |
|------------|--------------|--|--|--|
| WT         | 0.16         |  |  |  |
| WTE        | 0.87         |  |  |  |
| SS         | 0.16         |  |  |  |
| SSE        | 2.46         |  |  |  |
| MS         | 0.07         |  |  |  |
| MSE        | 0.78         |  |  |  |
| SH         | 1.36         |  |  |  |
| SHE        | 3.75         |  |  |  |

Similar results were reported by Pereira et al. (2010) and Gusmão et al. (2013) with dianhydride of EDTA (EDTAD) modifications in sugarcane bagasse in the adsorption processes in aqueous solution. Both researchers verified that the nitrogen rate of sugarcane bagasse before EDTAD modification was 0.13% and after modification was 2.32%. They explain that this fact occurred due to the incorporation of amine functions in the bagasse after esterification of hydroxyl, proving the introduction of EDTAD into it.

# 3.4. Kinetics of Fe and Mn Adsorption

The kinetic curve of manganese (Figure 2a and 2b) showed that the optimum adsorption time was approximately 15 min for SHE and 60 min for WT, SS, SH, MSE, WTE and SSE. In relation to the natural adsorbent of maize straw (MS), equilibrium was not reached up to 180 min.

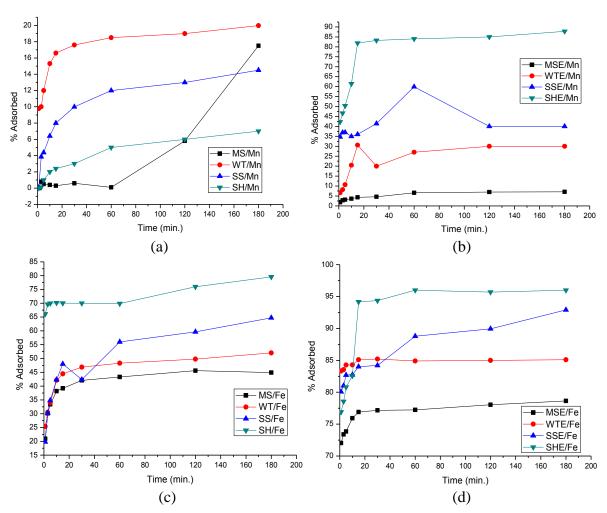
Overall, natural adsorbents showed reduced efficiency in the removal of manganese (Figure 2a). The maximum adsorbed amount was 16% for MS, 19% for WT, 13% for SS and 6% for SH.

Among modified adsorbents, the amounts of manganese removed were higher than that observed with natural adsorbents, except for the MSE, which showed a removal rate below 5%. The maximum removal was achieved using the modified soybean hulls adsorbent (SHE), with 88%

Tavlieva et al. (2015) used rice husk ash to remove Mn ions in aqueous solutions. The results showed that the Mn removal rate was 26.62%, much lower than that obtained in the present study with modified soybean hulls (SHH).

Regarding the kinetic tests for iron removal with the natural adsorbents, the kinetic curve (Figure 2c) shows that the optimum adsorption time was approximately 30 min for MS and WT, 60 min for SS and 180 min for SH. The maximum iron removal level achieved with natural adsorbents was 78%, using soybean hulls (SH).





**Figure 2.** Adsorption kinetics of manganese and iron by the following materials (a) MS, WT, SS and SH and (b) MSE, WTE, SSE and SHE.

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The adsorption of Fe with modified adsorbents (Figure 2d) revealed that the time required for the system to balance is approximately 15 min for MSE, WTE and SHE. There was no equilibrium for SSE up to 180 min.

It was also observed that the modified adsorption systems were more efficient in the removal of iron in comparison with the natural ones, reaching values 77% for MSE, 93% for SSE, 85% for WTE and 96% for SHE.

Considering only the modified soybean adsorbent (SHE), which showed the best results in Fe and Mn adsorption, the pseudo-second order kinetic model evidenced results that more closely match the experimental and calculated  $q_e$  values (Table 3), with higher coefficients of determination ( $R^2$ ) in comparison with the pseudo-first order kinetic model, describing better the adsorption process.



According to Feng et al. (2011), the pseudo-second order model assumes that the velocity-limiting factor may be the chemical adsorption involving valence forces, through the sharing or exchange of electrons between heavy metal ions and the adsorbent. It is a model that describes well the processes of chemical adsorption that involve donation or exchange of electrons between the adsorbate and the adsorbent, as covalent forces and ionic exchanges (Ho and Mckay, 2000).

**Table 3.** Parameters of the pseudo-first order and pseudo-second order kinetic models for Mn and Fe adsorption in SHE.

| Metal    | qe (exp)<br>(mg. g <sup>-1</sup> ) | Pseudo-first order                  |  |                | Pseudo-second order                |  |                |
|----------|------------------------------------|-------------------------------------|--|----------------|------------------------------------|--|----------------|
|          |                                    | qe (calc)<br>(mg. g <sup>-1</sup> ) | k <sub>1</sub><br>(min <sup>-1</sup> ) | $\mathbb{R}^2$ | qe (calc)<br>(mg.g <sup>-1</sup> ) | k <sub>2</sub><br>(g.mg <sup>-1</sup> .min <sup>-1</sup> ) | $\mathbb{R}^2$ |
| Mn<br>Fe | 1.00<br>2.60                       | 0.41<br>0.95                        | 0.021<br>0.021                         | 0.735<br>0.701 | 1.00<br>2.59                       | 0.359<br>0.168   | 0.999<br>0.999 |

In the present study, the pseudo-second order adsorption rate  $(k_2)$  for Mn and Fe in SHE was 0.359 and 0.168 g.mg<sup>-1</sup>.min<sup>-1</sup>, respectively.

# 4. CONCLUSION

Agricultural and agroindustrial wastes are high-abundance and low-cost materials that can be used as alternative adsorbents for the removal of microcontaminants in water treatment systems.

All the adsorbents produced from maize, wheat and soybean residues were able to adsorb iron and manganese in aqueous solution. However, the soybean hulls modified adsorbent (SHE) showed the best results in the removal process, displaying an adsorption rate of 96% for iron and 88% for manganese. The pseudo-second order kinetic model presented a better description of the adsorption process of Fe and Mn in SHE adsorbent.

It is concluded that this material has proved promising for use in the adsorption of metal microcontaminants in aqueous solution, creating added value to waste and economic and environmental advantages.

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