Evaluation of Organic Load Measurement Techniques in a Sewage and Waste Stabilisation Pond

Pedro Sérgio Fadini^a, Wilson F. Jardim^b and José Roberto Guimarães^{*,c}

^aFaculdade de Química, PUC-Campinas, CP 317, 13012-970 Campinas - SP, Brazil

^bInstituto de Química, Universidade Estadual de Campinas, CP 6154, 13083-971 Campinas - SP, Brazil

^cFaculdade de Engenharia Civil, Universidade Estadual de Campinas, CP 6021, 13083-970 Campinas - SP, Brazil

A Demanda Bioquímica de Oxigênio (DBO) e a Demanda Química de Oxigênio (DQO) são os principais indicadores rotineiramente utilizados para avaliação de carga orgânica em matrizes de interesse ambiental. Nesse contexto, avaliações da possibilidade de substituição das testes de DBO e DQO por medidas de Carbono Orgânico Dissolvido (COD) são apresentadas para diferentes águas residuárias. Para efluente de lagoa anaeróbia, as seguintes correlações foram obtidas: DQO = 1,08 COD + 79 e DBO = 0,82 COD + 12. Para efluente de lagoa facultativa, DQO = -0,29COD + 109 e DBO = 0,14COD + 26. Para esgoto bruto, DQO = 4,18COD - 2 e DBO = 0,46DQO + 5. Para efluente de lagoa aerada, DQO = 3,57COD + 6 e DBO = 0,27DQO + 3. Para efluente de lagoa de decantação, DQO = -1,34COD + 138 e DBO = 0,73COD + 16,5. A determinação de COD não mostrou-se adequada para uma substituição das alternativas clássicas, para as amostras testadas, a despeito das limitações que estas últimas apresentam.

Biochemical Oxygen Demand (BOD) and Chemical Oxygen Demand (COD) are the major parameters used as routine surrogate tests for measuring the load of organic carbon into the environment. In this context, an evaluation of possible replacement of BOD and COD for Dissolved Organic Carbon (DOC) measurements are presented for different wastewaters. For anaerobic pond effluent, the following correlations were obtained: COD = 1.08 DOC + 79 and BOD = 0.82 DOC + 12. For facultative pond effluent, COD = -0.29DOC + 109 and BOD = 0.14DOC + 26. For raw sewage COD = 4.18DOC - 2 and BOD = 0.46COD + 5. For aerated pond effluent COD = 3.57DOC + 6 and BOD = 0.27COD + 3. For sedimentation pond effluent, COD = -1.34DOC + 138 and BOD = 0.73DOC + 16.5. Determination of COD was not appropriate for substituting classical alternatives in tested samples in despite of the limitations of the samples.

Keywords: BOD, COD, DOC, organic carbon, pollution

Introduction

Measuring organic and inorganic carbon in surface and ground waters is of great interest to assess quality of life in many ecosystems. In pollution abatement works, organic carbon measurement provides a quick and simple method for monitoring pollution levels as well as the accumulation of non biodegradable or refractory organic materials. Under the ecological point of view, organic and inorganic carbon measurements give quantitative information about the carbon cycle and productivity of natural bodies of water. In environmental engineering, measurement of organic carbon provides a non-specific measure for monitoring potentially toxic organic materials in natural waters.¹ Efficiency of waste water treatment plants and kinetics characteristics of biological process are usually studied through BOD and COD, although difficulties are encountered in their measurement.²

As pointed out by Dart,³ and Logan and Wangenseller,⁴ some problems inherent to the use of BOD are, high variability of results; inconsistent results when in the presence of toxic species; possible need for foreign microorganisms as seed; labour-intensive and time-consuming test; laboratory conditions set in a way that may not reflect real environment; five days period necessary to produce a result may be non-representative due to operational problems that occurred during this period.

Although much simpler than BOD from an analytical point of view, COD tests do not differentiate between recalcitrant and biologically available organic matter.

^{*} e-mail: jorober@fec.unicamp.br

Other disadvantage of this test is that the kinetics of biological degradation under natural conditions cannot be inferred.⁵

Despite the historical use of both BOD and COD procedures to "measure" organic carbon and recent uses of UV absorbance,⁶ absorbance and fluorescence⁷ or biosensors,8 the results always are expressed in terms of mg O₂/L, thus inferring (and not measuring) the amount of organic material present in the sample. In this scenario, the determination of total organic carbon (TOC) would be a more rational approach to this particular problem, and seriously considered as a potential replacement for BOD and COD analysis. This new trend in routine as well as research laboratories has been strengthened in recent years due the dissemination of methods using catalytic oxidation at high temperature (650-900 °C), or UV photo-oxidation at low temperature, both techniques with non-dispersive infrared detectors for the final CO₂ measurement.⁹ It is important to mention here that due to operational problems, most TOC data are obtained using filtered samples. In this case, they account for the total dissolved organic carbon, and should correctly be quoted as DOC (Dissolved Organic Carbon).

As pointed out by Roscoe,¹⁰ TOC automation has been considered seriously in many agencies devoted to environmental monitoring and protection. For instance, by the NRA, stating "our recommendation (for on-line installation) is TOC. For many categories of effluent there are consistent relationships between BOD and TOC which would permit conversion of BOD to equivalent TOC values", by the Chief Inspectors Guidance (section 5), HMIP: "There is often a reliable though non-linear relationship between (the standard) BOD and TOC", by The Urban Waste Water Treatment (England and Wales): "The parameters (BOD or COD) can be replaced by another parameter: TOC or TOD if a relationship can be established between BOD 5 and the substitute parameter".

Also, in respect to the replacement of BOD, Jones,¹¹ and Aziz and Tebbutt,² agree with the need of a consistent correlation between the alternative and the classical methods. Viraraghavan¹² recommends caution in the use of TOC, since he has not obtained significant correlation between BOD, COD and soluble organic carbon in raw sewage, septic tank effluent and polluted ground water samples.

In this paper, correlation between COD, BOD and TOC obtained in samples from waste stabilization ponds are presented and discussed. The use of TOC in routine laboratory work as the key data on the concentration of organic carbon in waste waters is evaluated under the analytical point of view. Another important aspect related to the routine analysis of DOC and TOC was a tremendous development in this commercial area, and the cost of both equipment and analysis decreased markedly. This development was centred not only in the way carbon is oxidized to CO_2 (now carried out by catalytic combustion or wet oxidation using persulphate), but mainly due to the CO_2 detection using non-dispersive infrared detector.¹³

Fadini¹⁴ developed an alternative and low-cost procedure to determine DOC in natural aqueous samples by coupling Flow Injection Analysis (FIA) with a conductimetric detector. The method is based upon an early work of Pasquini and Faria,15 later modified by Jardim et al.16 The method explores the use of on-line digestion using UV and persulphate. The CO₂ produced in then measured after membrane diffusion by conductimetry. The equipment is able to process 14 samples/h in the determination of DOC and 25 samples/h when determining inorganic carbon. Compared to the vast majority of last generation HTCO (high temperature catalytic oxidation) commercially available equipments, the cost of this "home made" apparatus is 8 times lower (around US \$ 4,000.00), showing an operational cost in the range of US \$ 7.00 per 1,000 samples analyzed.

Experimental

Samples were collected in a sewage treatment plants at Limeira city and Indaiatuba city, both in São Paulo state, Brazil. The first plant, at Limeira city, consists of one anaerobic followed by two facultative ponds. The second plant, located in Indaiatuba city have an aerated pond followed by a sedimentation pond. Values of dissolved BOD, COD and DOC in the anaerobic and in the second facultative pond effluents were determined after filtration through baked (500 °C) Whatman GF/C glass-fiber filter. COD tests were performed as recommended in a open reflux method, and BOD by the 5-day test with azide modification using the Winkler method for DO measurement.¹⁷ DOC measurements were made in a Shimadzu carbon analyzer, model TOC 5000. The values were obtained from six replicates for BOD, three for COD and two or three injections for DOC (third injection was made if the coefficient of variation was above 2%). Collection and analysis were performed in the same day without preservation. Samples were collected in a polyethylene flasks and transported in a thermal box with ice.

Results and Discussion

Table 1 show the experimental results obtained when using filtered samples in this study for the anaerobic and the facultative pond, raw sewage, aerated and sedimentation pond, respectively.

Mathematical relations involving values of COD, BOD, and DOC obtained for these samples are shown in Table 2.

Best significative levels for correlation, between dissolved organic carbon (DOC) and BOD as well as COD were observed for the raw sewage. The worst significative levels was obtained among these parameters for the facultative and sedimentation effluents. Mathematical

Table 1. COD, BOD, and DOC values obtained for different effluents

Source of sample	BOD (mgO ₂ /L)	$COD (mgO_2/L)$	DOC (mgC/L)	
Anaerobic pond effluent				
Mean ± s	57.8 ± 22.2	138.1 ± 25.9	55.1 ± 22.0	
Range	14 - 79	97 - 172	20 - 98	
Number of samples	10	10	10	
Facultative pond effluent				
Mean ± s	31.1 ± 17.2	98.6 ± 13.4	37.4 ± 11.2	
Range	16 – 64	77 – 119	18 - 56	
Number of samples	10	10	10	
Raw sewage effluent				
Mean ± s	130.0 ± 43.3	273.2 ± 90.7	65.8 ± 19.1	
Range	91 - 191	191 - 419	38 - 88	
Number of samples	5	5	5	
Aerated pond effluent				
Mean ± s	29.8 ± 12.0	99.2 ± 35.5	26.0 ± 9.4	
Range	17 – 45	45 - 138	13 - 39	
Number of samples	5	5	5	
Sedimentation pond effluent				
Mean ± s	30.0 ± 6.8	113.4 ± 13.1	18.6 ± 6.3	
Range	21 - 37	99 - 131	12 - 29	
Number of samples	5	5	5	

Table 2. Ratio involving BOD, COD, and DOC values obtained for different effluents

Source of sample	BOD/COD	BOD/DOC	DOC/COD	
Anaerobic pond effluent				
Mean ± s	0.40 ± 0.12	1.05 ± 0.24	0.39 - 0.10	
Range	0.14 - 0.56	0.70 - 1.44	0.21 - 0.57	
Number of samples	10	10	10	
Facultative pond effluent				
Mean ± s	0.29 ± 0.13	0.85 ± 0.47	0.39 ± 0.14	
Range	0.19 - 0.54	0.37 - 1.61	0.18 - 0.56	
Number of samples	10	10	10	
Raw sewage effluent				
Mean ± s	0.48 ± 0.04	1.99 ± 0.32	0.24 ± 0.04	
Range	0.41 - 0.53	1.64 - 2.39	0.20 - 0.30	
Number of samples	5	5	5	
Aerated pond effluent				
Mean ± s	0.31 ± 0.08	1.15 ± 0.21	0.26 ± 0.03	
Range	0.21 - 0.38	0.83 - 1.36	0.22 - 0.29	
Number of samples	5	5	5	
Sedimentation pond effluent				
Mean ± s	0.27 ± 0.07	1.69 ± 0.40	0.17 ± 0.07	
Range	0.19 - 0.36	1.24 - 2.08	0.09 - 0.28	
Number of samples	5	5	5	

equations obtained from the plots of each paired parameter and their respective correlation are presented ins Tables 3 and 4.

Aziz and Tebbutt,² working with activated sludge, obtained a relation for BOD/DOC in filtered samples that ranged from 1.263 down to 0.488, when the aeration time increased from 1.8 up to 15.5 h. This behaviour is expected since recalcitrant carbon will remain in solution as aeration proceeds. Note that the results obtained in our work for the anaerobic (1.04) and the facultative (0.85) also show the same trend and are within the range obtained by the above mentioned authors.

Viraraghavan,¹² also studied the correlation among BOD, COD, and DOC in 3 different types of water samples. The results, showing a very poor correlation, are presented in Table 5.

Mathematical equations relating these 3 parameters were also investigated by other authors. Maier and McConnel¹ present the following relations: COD = 3.504TOC - 20.3 and BOD = 1.87TOC - 11.6 for typical wastewater samples. Values obtained in a paper plant effluent showed a correlation with between BOD and TOC expressed as TOC = 1.045BOD + 112.7.

Conclusion

It is clear from the preliminary results presented in this paper as well all the information so far published that there isn't an expected theoretical correlation between COD and DOC or BOD and DOC. However, it is also clear that, as long as some key physico-chemical and biological characteristics of a given effluent remains fairly constant over time, then values of DOC can be used instead of BOD and/or COD. Nevertheless, before this replacement occurs, a solid data bank on these 3 values would be necessary.

The determination of COD and BOD can make it difficult to establish relationships between the tests. The organic matter is inferred by measuring oxidant

Table 3. Mathematical relations obtained for COD, BOD, and DOC in both anaerobic and facultative effluents

SAMPLE	EQUATION	r
Anaerobic effluent	BOD = 0.7394COD - 44.3091	0.8609
	COD = 1.0793DOC + 78.6295	0.9156
	BOD = 0.8191DOC + 12.6696	0.8090
Facultative effluent	BOD = 0.8753COD - 55.2086	0.6824
	COD = -0.2890DOC + 109.4080	-0.2426
	BOD = 0.1378DOC + 25.9461	0.0902

Table 4. Mathematical relations obtained for COD, BOD, and DOC in the raw sewage, aerated effluent and sedimentation effluent

SAMPLE	EQUATION	r
Raw Sewage	BOD = 0.4589COD + 4.6417	0.9612
-	COD = 4.1794DOC - 1.8015	0.8808
	BOD = 2.0626DOC - 5.7170	0.9105
Aerated effluent	BOD = 0,2749COD + 2.5253	0.8106
	COD = 3.5739DOC + 6.2795	0.9453
	BOD = 1.1733DOC - 0.7057	0.9150
Sedimentation effluent	BOD = -0.007COD + 30.8275	-0.0114
	COD = -1.3412DOC + 138.3462	-0.6505
	BOD = 0.7259DOC + 16.5000	0.6794

Table 5. Relation between BOD, COD and DOC from data obtained by Viraraghavan¹²

SAMPLE	EQUATION	r
Raw sewage	BOD = 0.031DOC + 554 COD = 1.17DOC + 879	0.016 0.344
Septic tank effluent	BOD = 1.27DOC + 187 COD = 3.56DOC + 368	0.395 0.341
Polluted ground-water	BOD = 1.20DOC + 48 COD = 3.32DOC + 47	0.340 0.559

consumption. The oxygen is measured by the BOD test and the dichromate ions are measured by the COD test.

The organic matter is oxidized in the DOC determination and the CO_2 formed is quantified, which allows an effective measure of the organic matter level.

There is a negative correlation between COD and DOC as shown in Tables 3 and 4.

In both cases the effluent had contact with anaerobic sites where a removal of organic matter could occur through the generation of CH_4 and CO_2 , as well as the reduction of different chemical species that act as electron receptors in the anaerobic respiration process, such as Fe(III), Mn(IV), NO_3^- and SO_4^{-2-} , that are respectively reduced to Fe(II), Mn(II), Mn(II), N₂ or NH₃ and S²⁻.

An effluent with anaerobic characteristics can be poor in organic matter and enriched with reduced inorganic species that can be oxidized by the dissolved oxygen through the BOD process and by the dichromate ions through the COD process. This explains any eventual negative relationships, which commonly occur between DOC and COD, since the oxidant used in the COD process is very strong.

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