





Drying temperatures on the functional properties of purple-fleshed sweet potato

Herbert Gama Vidal²  Leticia Figueiredo de Araujo¹ José Lucena Barbosa Junior^{1*} 

¹Departamento de Tecnologia de alimentos, Instituto de Tecnologia, Universidade Federal Rural do Rio de Janeiro (UFRRJ), 23890-000, Seropédica, RJ, Brasil. E-mail: lucenadta@gmail.com. *Corresponding author.

²Programa de Pós-graduação em Ciência e Tecnologia de Alimentos, Universidade Federal Rural do Rio Janeiro (UFRRJ), Seropédica, RJ, Brasil.

ABSTRACT: Purple-fleshed sweet potatoes are rich in phenolic compounds, such as anthocyanins, and also exhibit hypoglycemic properties. Anthocyanins are natural antioxidants with the capacity to inhibit or delay injuries caused by free radicals. Drying is one of the most commonly used vegetable preservation methods; although, it has parameters that affect the sensory and physicochemical properties of the final product. The present study assessed the impact of drying temperatures (40, 50, and 60 °C) on the purple-fleshed sweet potato. Cut, unpeeled potato slices of 4 cm in diameter and 3 mm in thickness were dried in an oven with hot air circulation. The effect of the different temperatures on the antioxidant capacity, phenolic compound content, and total and monomeric quantities of anthocyanins in purple sweet potato were measured, and a mathematical model describing the drying kinetics was determined. According to the results observed, the process at 40 °C better preserved the phenolic compounds; however, drying at 50 °C was more efficient for conserving the antioxidant capacity measured by the H⁺ capture method performed by DDPH, and for the total and monomeric quantities of anthocyanins. The mathematical models that best described the kinetic curves were those of Henderson and Pabis, and Page.

Key words: anthocyanins, bioactive compounds, Henderson and Pabis, Page model, drying kinetics, Ipomoea potatoes.

Efeito das temperaturas de secagem nas propriedades funcionais da batata doce de polpa roxa

RESUMO: A batata doce roxa de polpa roxa é rica em compostos fenólicos, como as antocianinas além de possuir também propriedades hipoglicêmicas. As antocianinas são antioxidantes naturais capazes de inibir ou retardar lesões causadas por radicais livres. Um dos métodos de conservação de vegetais mais utilizados é a secagem. Mesmo sendo um método de execução simples, possui parâmetros de processo que interferem amplamente em termos sensoriais e nas propriedades físico-químicas do produto final. O presente trabalho teve por objetivo avaliar o impacto de três temperaturas de secagem (40, 50 e 60 °C), em rodelas de batata doce roxa de polpa roxa com casca, com diâmetro de 4cm e espessura de 3mm, em desidratador com circulação de ar quente sobre a capacidade antioxidante, teor de compostos fenólicos, antocianinas totais e monoméricas, além de determinar um modelo matemático que pudesse descrever as cinéticas de secagem. De acordo com os resultados obtidos a secagem a 40 °C se mostrou mais conveniente em termos de compostos fenólicos, porém a secagem a 50 °C se mostrou mais eficiente para o resultado de capacidade antioxidante pelo método de captura de H⁺ realizado por DPPH e para antocianinas totais e monoméricas. Os modelos matemáticos que descreveram melhor as curvas de cinética foram o modelos de Henderson e Pabis e o de Page.

Palavras-chave: antocianinas, compostos bioativos, Henderson e Pabis, Page, cinética de secagem, Ipomoea batatas.

INTRODUCTION

Sweet potato (*Ipomoea batatas* L.) is a plant originating in America that is classified by its format, size, and skin and pulp color, among other factors. It is an edible tuberous root with approximately 50 genera and more than 1000 species (NASCIMENTO, 2017). Its cultivation is widespread throughout Brazil due to its production capacity in poor soils, low incidence of pests and limiting diseases, and reduced management requirements. Given the vast overall

knowledge of this vegetable, it is widely used in domestic cooking or as a raw material for industrial processes (ROESLER et al., 2008).

The presence of polyphenols, anthocyanins, β -carotene, vitamins, and fibers promoted sweet potato functionality and nutritional value (TOYAMA et al., 2006). Among the numerous varieties of skin and pulp colors of sweet potatoes, the purple pulp is highlighted for its bioactive properties due to phenolic compounds such as anthocyanins, and also for its hypoglycemic capacity (JIANTENG XU et al., 2015).

Phenolic substances are known for their antioxidant capacity, providing functionality to various foods and inhibiting or delaying injuries caused by free radicals. These are molecules with one or more unpaired electrons that quickly react with different cellular targets, causing damage associated with degenerative disease and aging processes. Anthocyanins are phenolic compounds that are abundant in purple-fleshed sweet potato (PSP) (VIZZOTTO et al., 2017).

Anthocyanins are water-soluble pigments that belong to the group of flavonoids responsible for a wide variety of colors in fruits, ranging from red-orange to purple. Their primary function is to protect the plant against ultraviolet (UV) rays and prevent the formation of free radicals, and the main anthocyanins reported in purple sweet potatoes are the acylated forms of cyanidin and peonidin. The acylation pattern of different phenolic acids makes PSP anthocyanins unique and offers stabilization advantages over pH, heat, and light resistance (OLIVEIRA et al., 2019).

Temperature is an important factor in the stability of anthocyanins since degradation starts at temperatures above 25 °C, and it advances as the pH of the medium increases. However, some studies have shown, such as those conducted by SAPERS et al. (1981) and CHIGURUPATI et al. (2002), that the stability of anthocyanins regarding temperature is positively correlated to the degree of acylation (LOPES et al., 2007). Additionally, purple sweet potato anthocyanins are reported primarily in acylated form with phenolic acids, keeping them stabilized under pH changes, high temperatures, and light variations (JIANTENG XU et al., 2015).

Due to their perishability, the primary use of roots and tubers is in cooking or as a raw material for obtaining sweets, flour, flakes, and starch (ROESLER et al., 2008). Drying is a widely used conservation method for obtaining flours, and despite being straight forward it has process parameters that interfere with the sensory attributes and physicochemical properties of the final product (ALONSO & PARK, 2005).

The analysis of drying kinetics provides information about the mass transfer behavior between purple pulp sweet potato slices and the drying agent (hot air). It is fundamental to determine the drying time and the final relative humidity of the flour to be produced for dryer design and simulations.

Although, studies exist on the evaluation of different drying methods on purple sweet potato in relation to bioactive activity, research on the effect of convective drying conditions on the quality and quantity of bioactive compounds present in purple-fleshed sweet potato has not been identified. Thus, this study

evaluated the impact of different drying temperatures in a dehydrator with hot air circulation on the antioxidant capacity, phenolic compound content, and total and monomeric anthocyanins in purple-fleshed sweet potato, as well as to propose a mathematical model that could describe the drying kinetics involved.

MATERIALS AND METHODS

The sweet potato (*Ipomoea batatas*L.) used in this study had purple skin and purple pulp (PSP) and was obtained through the Integrated Agroecological Production System –SIPA (Fazendinha Agroecológica) located in Seropédica, Rio de Janeiro -RJ (22°48'00" S and 43°41'00" W).

The PSP samples used in the drying process followed the preparation flowchart shown in figure 1.

Physicochemical analysis

The moisture content of the raw material was determined by dry weight at 105 °C in an oven following the method 012/IV of the Adolfo Lutz

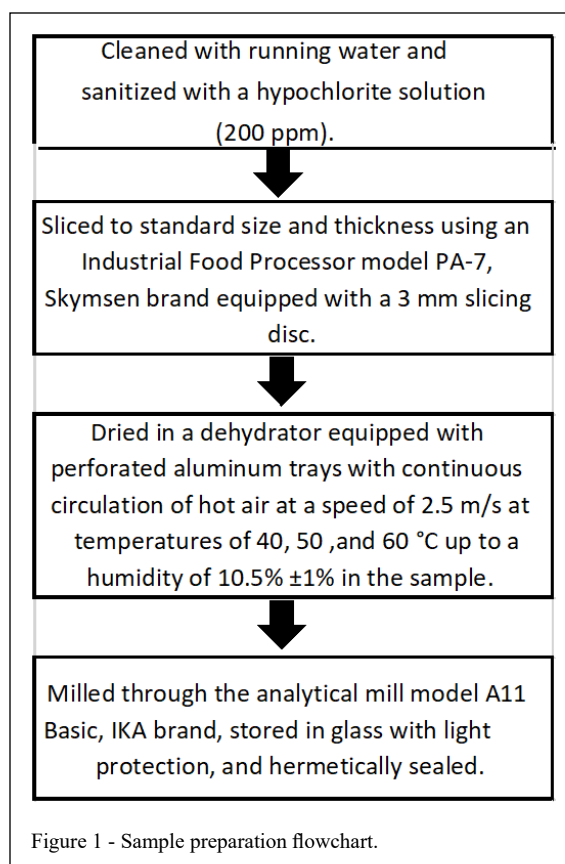


Figure 1 - Sample preparation flowchart.

Institute (IAL, 2005), performed in triplicate using an initial mass of approximately 10 g for each sample.

The extract preparation procedure for the analyses of antioxidant capacity, phenolic compounds content, and total and monomeric anthocyanins, was performed according to RUFINO et al. (2010), with minor modifications. One gram of sample was weighed and transferred into an Erlenmeyer flask along with 25 mL of solvent (acetone: alcohol: water, 40:40:20 v/v/v), and stirred at 3500 rpm, at room temperature for 1 h, in the dark. After extraction, the extract was filtered through a no.3 sintered funnel with the aid of a vacuum pump (SOLAB, Model SL-60). The residue retained on the filter was then re-extracted and washed with 5 mL of solvent under the same conditions. The filtrates were placed in a volumetric flask (100 mL) in the dark and used for physicochemical analyses.

The total phenolic compounds in the studied flour fractions were obtained according to SWAIN & HILLIS (1959), with modifications. One milliliter of extract, 10 mL of distilled water, 1 mL of Folin Ciocalteu 0.25 N reagent, and 1.5 mL of 10% Na_2CO_3 were added, followed by homogenization. The solution was stored at room temperature in the dark for 2 h, and the absorbance was measured at 725 nm using a spectrophotometer. Results were expressed as the mg equivalent of gallic acid per gram of dry sample (mg GAE. g^{-1} of the dry sample).

Antioxidant capacity was determined using the DPPH method according to the procedure described by RUFINO et al. (2010), with minor modifications. Extracts (150 μL) were reacted with 2.85 mL of a methanolic solution of DPPH (0.06 mM) for 1 h in the dark. The absorbance was then read using a spectrophotometer (Spectrophotometer Model NOVA 2000 UV) at a wavelength of 517 nm. Trolox was used as a reference for the construction of the calibration curve, and the results were expressed in μg of Trolox equivalent per gram of sample.

Phosphomolybdenum analysis was performed using spectrophotometry, whereby 0.3 mL of extract was added to a reagent mixture (3 mL) containing 0.6 M sulfuric acid, 28 mM sodium phosphate, and 4 mM ammonium molybdate. After 90 min of incubation at 95 °C, the absorbance of the mixture was read at 695 nm; the blank consisted of 0.3 mL ethanol with 3 mL of the reagent mixture. Results are expressed in millimoles of Trolox per gram of sample.

The quantification of total and monomeric anthocyanins was performed using the differential pH method proposed by GIUSTI & WROLSTAD (2001), with absorbances measured at $\lambda 510$ and $\lambda 700$ nm for pH 1.0 and 4.5, respectively in an SP 22 visible UV spectrophotometer. Results were expressed in cyanidin

equivalent milligrams – three glycosides per kilogram of purple sweet potato dry mass ($\text{mg}_{\text{eq}} \cdot \text{C}_3\text{G/kg}$).

Obtaining data for the kinetic curve

The drying process was performed in a dehydrator with hot air circulation at a speed of 2.5 m/s, equipped with a digital temperature controller and perforated aluminum trays. Continuous repetitive weighing of the samples was conducted until they reached a constant weight, as shown in table 1.

The drying curves were obtained by converting the data relating to water loss into the dimensionless water content ratio (Y) parameter, using the following formula (Equation 1):

$$Y = \frac{X_{bus} - X_e}{X_{bus\text{initial}} - X_e} \quad (1),$$

where:

X_{bus} = water content (dry basis);

$X_{bus\text{initial}}$ = initial water content (dry basis); and

X_e = water content in the equilibrium (dry basis).

The experimental data for the drying of the purple pulp of sweet potato (Table 1) were fitted to four mathematical models (Equations 2–5) that are frequently used to represent the kinetics of agricultural products, and are presented in table 2 to predict the drying time required to achieve a specific moisture content in the purple sweet potato flour.

The effective diffusivity (D_{ef}) of the water inside the product was determined by assuming the approximation of the purple pulp sweet potato slices to the shape of a flat plate using the following information (CRANK, 1975):

- uniform initial moisture $X(z, t) = X(z, 0) = X_0$;

- maximum humidity in center $\partial X / \partial z|_{z=0} = 0$, and

- constant humidity on surface $X(z, t)|_{z=L} = X(L, t) = X_{eq}$.

Thus

$$Y = \frac{8}{\pi^2} \sum_{i=0}^{\infty} \frac{1}{(2i+1)^2} \exp\left(- (2i+1)^2 \pi^2 D_{ef} \frac{t}{4L^2}\right) \quad (6),$$

with t = drying time, i = number of components, D_{ef} = effective diffusivity,

$2L$ = thickness of the flat sample, and Y = the dimensionless parameter.

A nonlinear regression analysis was performed to adjust the mathematical models to the experimental data using the quasi-Newton method, using the computer program STATISTICA 7.0®. The parameter values were estimated as a function of the sample's independent variable, air drying temperature, and equilibrium water content.

Statistical analysis

The statistical values of the coefficient of determination (R^2) and root mean square error (RMSE)

Table 1 - Drying data in a dehydrator with forced hot air circulation.

-----Data used in the construction of the Drying Kinetic Curve-----									
Time (min)	-----Drying at 40 °C-----			-----Drying at 50 °C-----			-----Drying at 60 °C-----		
	Xbs	Xbus	Dimensionless	Xbs	Xbus	Dimensionless	Xbs	Xbus	Dimensionless
0	1.923	0.658	1.000	1.752	0.637	1.000	1.923	0.658	1.000
20	1.455	0.593	0.896	1.252	0.556	0.867	1.122	0.529	0.794
40	1.145	0.534	0.803	0.922	0.480	0.742	0.785	0.440	0.651
60	0.906	0.475	0.710	0.674	0.403	0.616	0.472	0.321	0.461
100	0.613	0.380	0.558	0.374	0.272	0.401	0.248	0.199	0.266
140	0.407	0.289	0.414	0.208	0.172	0.237	0.156	0.135	0.164
180	0.255	0.203	0.277	0.123	0.110	0.135	0.097	0.088	0.089
240	0.148	0.129	0.159	0.068	0.064	0.059	0.068	0.064	0.050
300	0.099	0.090	0.098	0.050	0.048	0.033	0.055	0.052	0.031
360	0.073	0.068	0.062	0.043	0.041	0.022	0.047	0.045	0.020
420	0.056	0.053	0.038	0.039	0.037	0.015	0.043	0.041	0.014
480	0.045	0.043	0.022	0.036	0.035	0.012	0.040	0.039	0.010
1440	0.030	0.029	0.000	0.029	0.028	0.000	0.034	0.033	0.001
1500	0.030	0.029	0.000	0.029	0.028	0.000	0.034	0.033	0.000

were used as the first criteria for evaluating the best mathematical model. However, to better assess the non-linear mathematical models, the mean relative error (E) was employed, according to Equation 7:

$$E(\%) = \frac{100}{N} \sum_{i=1}^N \left| \frac{Y - \bar{Y}}{Y} \right| \quad (7)$$

where:

Y= experimental value, \bar{Y} = predicted model values, and N= experimental data points.

The development of the model allows the predictability of drying time \times the relative humidity

of the sample that is expected for dehydrators with continuous hot air circulation.

The statistical analysis of the drying points was performed using the chi-square test to verify the existence of a significant difference ($P < 0.05$) between the point values, using Minitab 19 Software (Pennsylvania, USA, 2019). Means were compared using Tukey's test ($P \leq 0.05$).

RESULTS AND DISCUSSION

The samples after drying at 40, 50, and 60 °C are presented in table 1, which shows that

Table 2 - Mathematical models applied to the drying of purple-fleshed sweet potato.

Models	-----Model Designation-----	
Fick - with 6 terms	$Y = \frac{8}{\pi^2} \sum_{i=0}^{\infty} \frac{1}{(2i+1)^2} \exp\left(-\frac{(2i+1)^2 \pi^2 D_{ef} t}{4L^2}\right)$	(BROOKER et al., 1992) (6)
Henderson; Pabis	$Y = a \cdot \exp(-k \cdot t)$	(HENDERSON & PABIS, 1961) (7)
Page	$Y = \exp(-k \cdot t^n)$	(PAGE, 1949) (8)
Peleg	$Y = 1 - \frac{t}{(a + b \cdot t)}$	(PELEG, 1988) (9)

Y- water content ratio (dimensionless); t- drying time (min); L-thickness of the flat sample; k- drying constants; a,b,n- model coefficients; Def – effective diffusivity (m^2/s).

the dehydration stability, that is, the non-significant difference between the measured points, is reached earlier at 50 and 60 °C when compared to the results at 40 °C. According to PARK et al. (2001), the evaporation of water contained in a solid is governed by two phenomena: heat transfer and mass transfer. Mass transfer is a function of the physical nature of the solid in terms of its temperature and moisture content, and heat is governed by parameters such as temperature, air humidity, airflow, air direction, and the exposed area of the solid. In this study, the only parameter that changed between the analyses was the drying air temperature; that is, higher temperatures tended to lead to earlier stabilization when compared to lower temperatures.

However, when analyzing the endpoints of the analysis (1440 and 1500 min), a lower humidity was observed in the samples at 50 °C and 40 °C compared to the dry sample at a temperature of 60 °C. This result relates to the dried crust formation on the surface of samples that had a high sugar content and were dried at high temperatures, which creates challenges in the removal of non-free water and; consequently, dehydration of the sample (PARK et al., 2007).

Table 3 shows the coefficient values of the four mathematical models analyzed and the statistical values of the determination coefficients (R^2), adjusted determination coefficients (R^2_{adj}) of the root mean square error (RMSE), and mean relative error (E).

Based on the findings of GONELI et al. (2009) and SILVA et al. (2015), the magnitude of the drying constant (k) in our study has a direct correlation with the drying air temperature.

In all treatments, the mathematical models adjusted to the experimental data presented coefficients of determination (R^2) above 97.81% and RMSE values below 0.039. Other drying studies obtained similar results, showing high values for R^2 . SILVA et al. (2015) obtained R^2 values above 97% for dried achachairu pulp, and COSTA et al. (2018) acquired an R^2 greater than 99% for the kinetics of ripe banana using the Henderson and Pabis, and Page models. For the drying of pão/sapo green banana, TAVONE et al. (2020) obtained R^2 values greater than 99% using the Page model.

Although, the four studied models demonstrated an adequate representation in the description of the drying kinetics of purple-fleshed sweet potatoes, according to MADAMBA et al. (1996), R^2 greater than 95% is the minimum value required to obtain a good reproduction of the models. Therefore, the Henderson and Pabis, and Page models were the best fit because they presented greater R^2 values and the lowest RMSE (Table 2).

Fick's second law describes the dynamic behavior of the drying process during the period of decreasing moisture over time, since effective diffusion (Def) is the primary mass transfer mechanism (HENRÍQUEZ et al., 2014). The increase in temperature directly affected the effective diffusion of the sample; as shown in table 2, there was an increase in this constant compared to the temperatures of 40 and 60 °C.

Figure 2 shows the drying kinetics estimated by Fick(6-term diffusive models), Henderson and Pabis, Page, and Peleg. The best

Table 3 - Statistical parameters and drying constant of the applied mathematical models.

Model	T(°C)	Parameters					R^2	R^2_{adj}	RMSE	E (%)
		Def	k	n	a	b				
Fick	40 °C	3.1675E-10	-	-	-	-	0.9781	0.6781	0.0388	25.0980
	50 °C	4.5273E-10	-	-	-	-	0.9792	0.6792	0.0300	27.4081
	60 °C	5.5245E-10	-	-	-	-	0.9792	0.6792	0.0231	15.5659
Henderson & Pabis	40 °C	-	0.0070	-	1.0376	-	0.9976	0.9143	0.0131	9.1773
	50 °C	-	0.0100	-	1.0463	-	0.9972	0.9138	0.0130	10.5615
	60 °C	-	0.0128	-	1.0167	-	0.9990	0.9157	0.0280	19.2568
Page	40 °C	-	0.0026	1.1859	-	-	0.9996	0.9163	0.0048	2.7007
	50 °C	-	0.0031	1.2389	-	-	0.9997	0.9164	0.0087	6.7135
	60 °C	-	0.0090	1.0752	-	-	0.9993	0.9159	0.0059	6.9479
Peleg	40 °C	-	-	-	110.7582	0.8437	0.9824	0.8991	0.0383	39.2784
	50 °C	-	-	-	75.1932	0.8635	0.9793	0.8960	0.0371	44.9725
	60 °C	-	-	-	53.1257	0.8963	0.9861	0.9027	0.0280	32.7852

The means of each variable were compared by tukey's test ($P < 0.05$).

fits were determined by the Henderson and Pabis and Page models because of their correspondence between experimental and estimated values.

The most significant amount of phenolic compounds was obtained from the dry flour at 40 °C. The drying process facilitated their extraction; however, in general, a higher drying temperature corresponds to a greater degradation of the phenolic compounds, which did not differ from the values obtained for the purple sweet potato with purple pulp. TANG et al. (2015) obtained similar results when they studied the behavior of phenolic compounds in purple sweet potato under different thermal processes (traditional cooking for 30 min, steam cooking for 30 min, and drying in a traditional oven at 230 °C for 30 min). They obtained the highest content with traditional cooking, which is the least severe method in terms of temperature. YANG et al. (2010) demonstrated that the total phenolic compounds of purple sweet potato increased in all drying processes applied (drying with hot air, microwave, and lyophilization) when compared to the content of the fresh samples. This is due to cell disruption during thermal processing, which allows for a greater extraction of compounds.

The results of the phenolic compounds obtained in the present study (18.24 – 32.02 mg EAG/100 g dry sample), corroborated those reported by other authors in studies with purple sweet potatoes. TANG et al. (2015) reported results ranging from 11.43 to 24.90 mg GAE/100g dry sample, and AHMED et al. (2010) showed a range of 4.29 to 8.33 mg GAE/100 g dry sample in purple sweet potato flour samples.

The drying process increased the antioxidant capacity of the studied samples, as shown in table 4, and the highest index was obtained for the flour dried at 50 °C using the free radical capture method by DDPH. For the flour dried at 60 °C, increased values were found in the total antioxidant capacity method performed by phosphomolybdenum analysis. This difference in the analysis is due to the anthocyanin content in the samples at 50 and 60 °C, where the degradation of anthocyanins during drying at higher temperatures results in a decrease in the capacity to capture free radicals (LOPES et al., 2007).

We observed that the drying temperature of the flour obtained in this study directly influenced the total anthocyanin content. The flour dried at 50 °C had

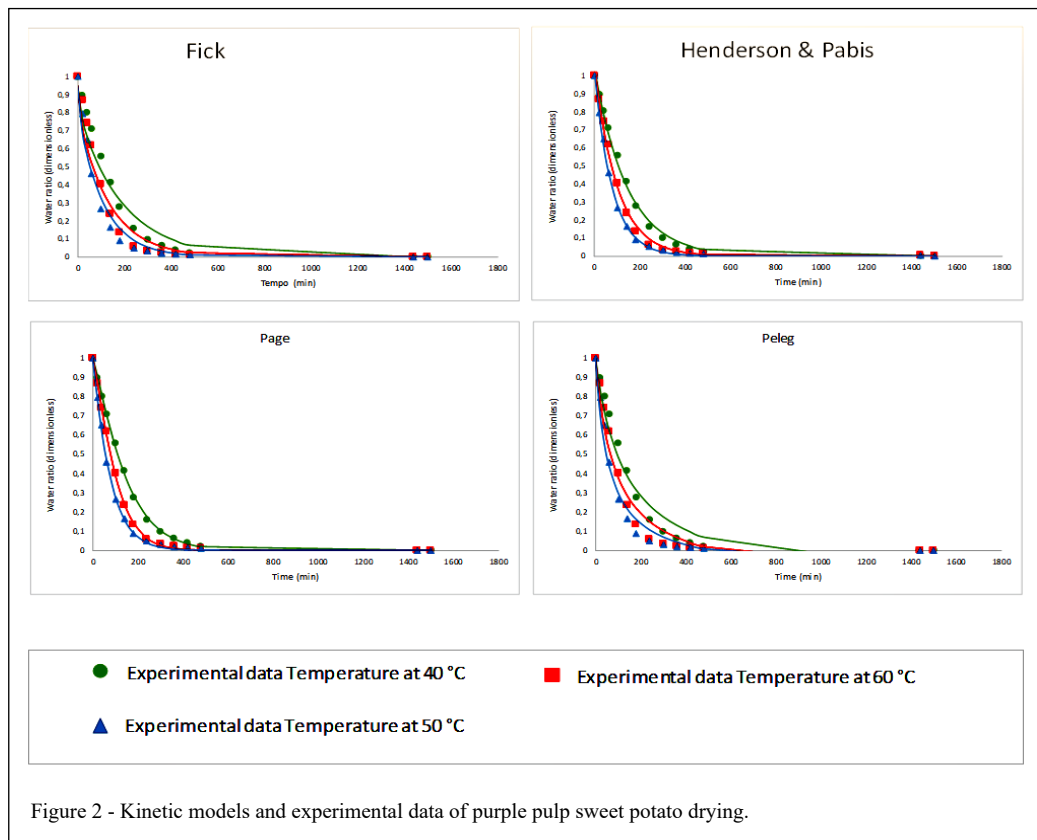


Table 4 - Results of analyses of purple pulp sweet potato flour.

Extract	Phenolic Compounds ^a	DPPH ^b	Phosphomolybdenum ^c	Total Anthocyanins ^d	Monomeric Anthocyanins ^d
<i>In Natura</i>	11.86 ± 0.33 ^f	29.81 ± 3.75 ^f	-	24.86 ± 0.78 ^f	5.07 ± 0.43 ^f
Flour 40 °C	32.02 ± 0.52 ^e	40.97 ± 2.66 ^e	240.39 ± 50.44 ^e	38.19 ± 1.02 ^e	7.67 ± 1.05 ^e
Flour 50 °C	25.94 ± 0.35 ^h	56.47 ± 3.08 ^h	629.52 ± 25.82 ^h	72.07 ± 2.69 ^h	14.96 ± 2.46 ^h
Flour 60 °C	18.24 ± 0.21 ⁱ	32.03 ± 3.57 ^f	929.31 ± 49.15 ⁱ	37.09 ± 0.76 ^e	7.36 ± 0.99 ^e

^a Expressed in mg gallic acid/100g sample.

^b Expressed in mg of Trolox equivalent/g of sample.

^c Expressed in mmol Trolox/g sample.

^d Expressed in mg cyanidin-3-glucoside equivalent/100g dry weight sample.

Means followed by the same letter do not differ statistically from each other, according to Tukey's test ($P < 0.05$).

the highest content (72.07 mg/100 g of dry sample), followed by that at 40 °C (38.19 mg/100 g of dry sample) and 60 °C (37.09 mg/100 g of the dry sample). This parabolic behavior in anthocyanin content at different temperatures has two explanations. First, because drying at 40 °C has a longer duration (at least 60% longer than other temperatures), degradation of anthocyanins occurs during the drying process. Second, as OLIVEIRA et al. (2015) stated, there is a deleterious effect on anthocyanins at higher temperatures, as shown in the results of the present study.

When comparing the total anthocyanins of the samples in this study with the data obtained in the literature from different purple sweet potato varieties, it can be observed that the three flours with content between 37.09 – 72.07 mg/100 g of dry sample were similar to those found by other researchers. TEOW et al. (2007) reported total anthocyanin content in 19 sweet potato genotypes, ranging from 1.7 to 53.1 mg/100 g of fresh sample. Table 5 shows that the purple-fleshed sweet potato used here presents levels of total anthocyanins similar to other studies

Table 5 - Comparison of total anthocyanin content in purple sweet potato studies.

Variety name	Anthocyanins ^a	Method	References
Stokes Purple	328 ^b		
NC 415	178 ^b	pH differential	TRUONG et al. (2010)
Okinawa	65 ^b		
Shinzami	1342	HPLC	KIM et al. (2012)
12 Variedades da China Central	78 - 695	HPLC	ZHU et al. (2010)
NDOP5847-1	175	pH differential	RODRIGUEZ-SAONA et al. (1998)
P40	1390	HPLC	JIAN TENG XU et al. (2015)
ILS 16	1112 ^b	pH differential	VIZZOTTO et al. (2017)
ILS 56	1072 ^b		
ILS 71	361 ^b		
CNPH 0005	88,6	pH differential	PILON et al. (2020)
CNPH 0080	60,6		
CNPH 1261	57		
CNPH 1399	193,8		
CNPH 1402	56,2		
CNPH 1405	200		

^a in mg/100g dry sample. ^b values converted to dry basis using 77% moisture as indicated in the USDA Food and Nutrient Database for Dietary Studies.

but in relatively smaller amounts when compared to some species, particularly Asian varieties. According to ISHIGURO et al. (2017), factors such as relative humidity and temperature influence the concentration of anthocyanins during the production of purple sweet potato.

Regarding monomeric anthocyanins, the results follow the same pattern as total anthocyanins, with the highest content found in the 50 °C sample (14.95 mg/100 g of dry sample), followed by 40 °C (7.67 mg/100 g of dry sample) and 60 °C (7.36 mg/100 g dry sample).

CONCLUSION

The present study demonstrated that it is possible to obtain purple sweet potato flour with purple pulp that meets the moisture specifications (less than 13%, according to Resolution No. 344, of December 13, 2002) with shorter drying times (140 to 300 min) when using a dehydrator with a continuous circulation of hot air.

The best mathematical model that described the drying kinetics at all temperatures was the Page model, followed by the Henderson and Pabis model.

The physicochemical properties varied according to the temperature of the air used for drying in an oven with forced ventilation. The total phenolic compounds decreased as the drying temperature increased, but with higher content than the fresh sample. However, the antioxidant potential increased up to a drying temperature of 50 °C and decreased at a temperature of 60 °C. The same behavior was observed in the analysis of total and monomeric anthocyanins; the values increased until the drying temperature reached 50 °C and then decreased at 60 °C. The most suitable temperature for drying this purple sweet potato with purple pulp was 50 °C, with forced ventilation.

DECLARATION OF CONFLICT OF INTEREST

The authors declare no conflict of interest. Funding sponsors had no role in the design of the study; the collection, analyses, or interpretation of data; the writing of the manuscript; or the decision to publish the results.

AUTHORS' CONTRIBUTION

All authors contributed equally to the conception and writing of this manuscript. All authors critically revised the manuscript and approved the final version.

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