

Obtaining and characterization of bacterial cellulose synthesized by *Komagataeibacter hansenii* from alternative sources of nitrogen and carbon

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ABSTRACT

This work aimed to obtain and characterize bacterial cellulose (BC) membranes obtained by cultivating *Komagataeibacter hansenii* ATCC 23769 using mannitol, glucose, fructose, lactose, glycerol, inulin, and sucrose as carbon sources, and corn steep liquor and Prodex Lac® as alternative sources of nitrogen. The formation of the BC's gelatinous membrane was monitored for 12 days under static conditions and a temperature of 30 °C. After purification, the membranes were dried and characterized by thermogravimetric analysis (TGA), Fourier-transform infrared spectroscopy (FTIR), and scanning electron microscopy (SEM). The highest BC concentrations were found in the culture medium containing Prodex Lac® as the source of nitrogen. Among sugars, fructose and mannitol presented the best results. TGA analyzes indicate that all membranes have similar thermal behavior. The FTIR results show that the chemically synthesized membranes are equivalent to the structures cited in the literature. The micrographs obtained by SEM showed that the medium might influence BC's morphology, but in general, all presented nanofibers, an essential feature in the membrane. Thus, the BC membranes synthesized in this study proved that the BC production using low-cost alternative means is feasible. The material obtained meets the expected thermal, physical, and chemical properties.

Keywords: Bacterial cellulose, corn steep liquor, Prodex Lac®, nitrogen sources, carbon sources.

1. INTRODUCTION

Cellulose is the most abundant biopolymer on earth. A new cellulose material, bacterial cellulose (BC), has gained more attention in recent years. Bacterial cellulose is made up of β -D-glucopyranose monomers linked by $\beta(1-4)$ glycosides linkages. Different from cellulose from plants, BC has a three-dimension structure of an ultrafine nanofiber network. So, BC retains unique properties related to hydroxyl groups' ability to form supramolecular interactions of the type intra- and intermolecular [1]. Compared with cellulose from plants, BC is considered free of impurities, like lignin and hemicellulose molecules, challenging to remove. Consequently, cellulose has some distinguishing features, like high purity, high porosity, biocompatibility, high mechanical strength and stillness, biodegradability, and renewability, which makes this material attractive for industrial applications [2, 3].

In recent years, BC has been a focus for the development of health foods (coconut gel) [4], high-end electrical conductor [5], biomedical wound care products [6], cosmetic facial masks [7], sustainable clothing [8], effluent treatment [9] and other industrial applications, such as biodegradable materials for active packag- ing in food [10].

Several microorganisms can synthesize bacterial cellulose (BC) and, among them, the bacterium *Komagataeibacter hansenii* has been widely cited. The production of bacterial cellulose can be done by means of static cultures, which are the traditional ones, or in dynamic cultivations, that accelerate the production [11, 12]. Microorganisms are conventionally grown in media containing carbon sources, nitrogen sources and basic

nutrients to form of a hydrogel membrane of BC. One of the common and traditional means used for the optimum production of cellulose from bacteria is Hestrin and Schramm's medium. However, low yield and

prolonged fermentation conditions limit their production on a larger scale and enhance their properties. In recent years, studies have focused on various cellulose-producing bacterial strains, inexpensive nutrient sources, and supplementary materials to produce inexpensive BC. In this context, research has been carried out in search of media with high glucose content, such as fruit juices [13], maple syrup [14], various agricultural and industrial residues, such as molasses [15], sisal juice [16], carrot juice [17], hot water extracted wood sugars [18] to enhance cellulose production [19]. Although some authors have been successful in increasing CB production, depending on the nutritional source, they require considerable cultivation time, limiting production on an industrial scale, and some studies have not verified whether other substrates in the culture medium compromised the properties of the obtained polymer.

This work's objective was to evaluate the effect of different culture media, varying carbon, and nitrogen sources, aiming to optimize BC production. The utilization of corn steep liquor, a residue of maize maceration as a source of nitrogen, and a wild yeast extract are known commercially as Prodex Lac®, both of which have economic advantages, were evaluated. The membranes were characterized for their microstructure, chemical, and thermal analysis since the medium conditions can influence the properties and then direct future studies and applications.

2. MATERIALS AND METHODS

2.1 Microorganism

The microorganism used to evaluate the BC production was the bacterium *Komagataeibacter hansenii* (ATCC 23769) obtained from the "Tropical Culture Collection (CCT)" (Andre Tosello Foundation), Campinas/SP. The microorganisms were stored at - 80 °C in a culture medium composed of mannitol, yeast extract, and peptone.

2.2 Synthesis and purification of bacterial cellulose

The inoculum was grown in a 1000 mL Erlenmeyer flask containing 400 mL of culture medium having the following composition: 20 g L⁻¹ mannitol, 5 g L⁻¹ yeast extract and 5 g L⁻¹ peptone. To the sterilized culture medium was added, the microorganism *K. hansenii*. The culture time for activation was 48 h in a static condition at 30 °C.

After cultivation, the cells were transferred at a 20% inoculum ratio to 125 mL Erlenmeyer flasks containing 20 g L⁻¹ of the sugar to be investigated, 5 g L⁻¹ of Prodex Lac® (P) (yeast autolysate, nitrogen source) or 5 g L⁻¹ of Corn Steep Liquor (CSL) (nitrogen source) according to Table 1. The culture was maintained at 30 °C, with sampling done every two days for 12 days.

Prodex Lac® is a wild yeast extract used as a source of low-cost vitamins to replace purified yeast extract [20].

Corn steep liquor, a by-product of the corn wet-milling industry, consists of 50% water and is rich in vitamins, amino acids, minerals, and other growth stimulants. It is a viscous concentrated brown liquid with a pH of 3.7 to 4.1 [21]. Corn steep liquor can be used as the best alternative for yeast extract, as a nitrogen source in biochemical industries [22].

The hydrogel membrane formed culture medium's surface was collected, washed with distilled water and immersed in a 0.1 M NaOH solution at 80 °C for one h to eliminate cell debris and contaminants from the culture medium. Then the membrane was washed with distilled water repeatedly until neutral. The membranes obtained were dried under vacuum at 30 °C for 48 h for the characterizations.

NITROGEN SOURCE (5 g L ⁻¹)	CARBON SOURCE (20 g L ⁻¹)	CULTURE MEDIA		
Yeast extract + Peptone	Mannitol	Control		
Corn Steep Liquor (CSL)	Fructose	CSL-Fru		
	Glucose	CSL-Glu		
	Glycerol	CSL-Gly		
	Inulin	CSL-Inu		
	Lactose	CSL-Lac		
	Mannitol	CSL-Man		
	Sucrose	CSL-Suc		
Prodex Lac® (P)	Fructose	P-Fru		
	Glucose	P-Glu		
	Glycerol	P-Gly		
	Inulin	P-Inu		
	Lactose	P-Lac		
	Mannitol	P-Man		
	Sucrose	P-Suc		

 Table 1: Culture media tested with their different compositions in relation to alternative sources of carbon and nitrogen.

2.3 Characterization

2.3.1 Thermogravimetric analysis - TGA

The TGA analyzes were performed to determine the thermal degradation, mass loss, thermal stability, degradation temperature (T_{onset}) and maximum degradation temperature (T_{max}) of membranes. TG curves were obtained in an equipment TGA-Q50/TA Instruments. The samples were heated at 25 to 600 °C at 10 °C min⁻¹ under a nitrogen atmosphere. The experimental parameters' adjustments were made in TA Universal Analysis software and graphically represented for better interpretation.

2.3.2 Fourier-transform infrared spectroscopy - FTIR

Characterization of functional groups of the membranes was performed by Fourier-transform infrared spectroscopy (FTIR) on Perkin Elmer Spectrum One equipment. Sixteen scans per sample were performed in the range of 4,000 to 650 cm⁻¹, with a resolution of 4 cm⁻¹ using the attenuated total reflectance (ATR) accessory.

2.3.3 Scanning electron microscopy – SEM

Samples of BC membranes were fixed in metal support and covered with a thin layer of gold using a BAL- TEC SCD 050 sample metallizer and observed by a scanning electron microscope (SEM) Zeiss DSM 940A, under a voltage of 10 kV, and magnification of 10,000 X. The software imageJ (public domain) was used to evaluate the images and measure the nanofibers' diameter.

3. RESULTS AND DISCUSSION

3.1 Effect of nitrogen and carbon sources on membrane formation

BC production is traditionally conducted from commercial culture media containing glucose as a source of carbon and other high-cost nutrients for the process. The use of carbon and nitrogen sources from agro-indus- trial wastes is an alternative to lower costs in obtaining biotech products. The use of these wastes contributes to lower production costs and fewer environmental impacts caused by improper disposal of these materials. Several successful by-products such as corn steep liquor [23], sugar cane molasses [24], cheese whey [11], fruit juices [13] has been used for this purpose. As shown in Figure 1, there was BC's formation for both nitrogen sources tested, regardless of the carbon source. However, Prodex Lac® provided higher yields of BC.





The performance of Prodex Lac® can be justified because it is a wild yeast extract, while the conventional medium for BC cultivation uses nitrogen as a source of yeast and peptone extract. Prodex Lac® is considered a source of low-cost vitamins (especially the B-complex) used in industrial biotechnology to replace the purified yeast extract. Prodex Lac® has also been shown to be beneficial in the production of β - galactosidase by yeasts [25], and in the production of glucosyltransferase by *Erwinia sp* to obtain maximum enzymatic activity and reduced costs in the fermentation process [26].

Regardless of the nitrogen source, it is observed that all carbon sources result in the formation of BC, and the best yields $(5.50, 4.20 \text{ and } 4.00 \text{ g L}^{-1})$ were found in lactose, fructose, and mannitol, respectively.

The results obtained for the synthesis of BC containing mannitol and glucose as carbon sources were 4.00 and 1.75 g L⁻¹ (having Prodex Lac® as nitrogen source) and 2.40 and 0.60 g L⁻¹ (taking corn steep liquor as nitrogen source). Hutchens *et al.* compared mannitol and glucose, having better results with mannitol, about 50% by mass [27]. According to the authors, mannitol is a sugar alcohol, which provides electrons for the metabolism of bacteria and stimulates a higher yield of cellulose than glucose.

In the assay containing fructose and glucose as carbon source, BC's formation was 4.20 g L⁻¹ and 1.75 g L⁻¹, respectively, having Prodex Lac® as the nitrogen source. According to SANTOS *et al.* [28], glucose and sucrose provided low BC production in a short period, while glycerol, mannitol, and fructose allowed consistent production throughout the growing time and in larger amounts when compared to glucose and sucrose. According to the carbon source, different production rates were also described by MIKKELSEN *et al.* [29]. The results revealed that cellulose production was stimulated by all carbon sources tested for 96 h of production, except for galactose. In 48 h of culture, mannitol yielded the highest yields in BC (2.04 g L⁻¹). It produced relatively high cellulose concentrations (1.89 and 1.79 g L⁻¹), respectively.

The concentrations resulting from the lactose use were 5.57 g L⁻¹ in the medium containing Prodex Lac® and only 1.31 g L⁻¹ for the medium containing corn steep liquor. TSOUKO *et al.* [30] obtained a low concentration of BC when lactose was used as a carbon source, attributing this result to the fact that the genus *Gluconacetobacter* does not have the gene coding for β -galactosidase, the enzyme responsible for the hydrolysis of lactose. However, in this study, in conjunction with Prodex Lac®, an opposite behavior was observed, resulting in a high BC concentration, indicating that the nitrogen source can influence the synthesis, providing a higher yield.

The low production performance when using glucose as a carbon source, 1.83 g L⁻¹, and 0.67 g L⁻¹, and as a source of nitrogen Prodex Lac® and corn steep liquor, respectively, was also reported by SANTOS *et al.*, [28] which obtained only 1.2 g L⁻¹ with this same carbon source. These authors justify correlating BC production with the carbon source rate, showing that glucose is consumed faster than the other carbon sources. Besides, glucose can be easily transported through the cell membrane and incorporated into the cellulose biosynthetic pathway. However, it has been reported that most glucose is converted into gluconic acid byproducts, which decreases the pH of the crop, causing lower BC production [31].

The use of glycerol did not sho results for BC formation, being 1.42 g L^{-1} when associated with Prodex Lac® and 1.26 g L⁻¹ along with corn steep liquor, diverging from another study that obtained 3.50 g L⁻¹ [30]. These results indicate that the interaction between the nitrogen source and the carbon source influences the BC synthesis. The same occurred when sucrose was used, which resulted in low concentrations, 1.40 g L⁻¹ in the medium containing Prodex Lac® and 0.94 g L⁻¹ in medium with corn steep liquor, while TSOUKO *et al.* [30] reported yielding 4.90 g L⁻¹.

Of all the carbon sources investigated, inulin showed the lowest yields, 0.88 g L^{-1} using Prodex Lac® and 0.66 g L^{-1} for corn steep liquor. This fact can be justified by the complexity of the bonds present in this polymer. TIBONI [32] suggests using fructooligosaccharides (FOS) as an alternative source of carbon since this can be obtained by hydrolyzed inulin with soft catalysts such as phosphoric acid and citric acid. In this way, the bacterium uses this sugar more efficiently, increasing its conversion in BC.

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All these results show that cellulose synthesis by bacteria is complex and is affected by many factors. A better yield in BC production may depend on the effective use of the carbon and nitrogen sources. Considering the diversity of enzymes and metabolic pathways present in BC-producing bacteria, several carbon sources can be used to develop and produce BC, yielding different yields [31].

3.2 Thermogravimetric analysis – TGA

The thermogravimetric curves (TG and DTG) obtained from TGA for BC membranes synthesized from dif- ferent carbon sources, containing Corn Steep Liquor and Prodex Lac® as a nitrogen source, are presented in Figure 2a and 2b, respectively. The extrapolated onset temperature (T_{onset}), which denotes the temperature at which the mass loss begins, was taken as the temperature at which the mass loss started, as is shown in Figure 2a and 2c. The temperature of the maximum mass loss rate (T_{max}) was calculated from the first derivative of the TG curve (DTG), and it indicates the point of the most significant rate of change on the mass loss curve (Figure 2b and 2d). The extrapolated onset temperature (T_{onset}), the temperature of maximum mass loss rate (T_{max}), percentage of mass loss, and residual mass percentage at 600 °C are shown in Table 2.



Figure 2: BC curves synthesized from different carbon sources: TG (a) and DTG curves (b) for Corn Steep Liquor (CSL) as nitrogen source; TG (c) and DTG curves (d) for Prodex Lac® as nitrogen source.

The degradation profile of the control BC membranes shows three mass-loss events. The first thermal event that presented mass loss between 9.1% is associated with water loss between 30 and 150 °C [33]. The second event was more pronounced and occurred in $T_{onset2} = 309$ °C with 64.9% mass loss and $T_{max2} = 335$ °C, according to Gea *et al.* [34] is attributed to cellulose degradation, including depolymerization and decomposi- tion of glucose units. The third event represents the degradation of carbonaceous residues that extends from 400 to 1000 °C with a percentage of residual at 600 °C determined was 19% [34].

For the other samples, the mass loss percentage of the first stage varied between 3.4 and 10.5 °C, evidencing BC's high hygroscopicity. The maximum decomposition temperature is a criterion of thermal stability. The determined T_{max2} varied between 316 and 339 °C, so that CSL-Man (339 °C), CSL-Frut (337 °C) and Prodex Lac®-Man (336 °C) presented slightly higher thermal stability than the control sample. It is also veri- fied that the means that provided the higher concentration of BC were the same ones that also presented better results in the thermal analyzes. Similarly, the means that provided lower BC membrane formation were, pre- cisely, the ones that showed lower values for T_{max} , such as P-Inu (318 °C) and CSL-Inu (316 °C), showing lower thermal stability. The T_{max2} data obtained in this work were much lower than the T_{max2} values of BC membranes produced by *Gluconacetobacter xylinus* using low-cost non-conventional carbon sources investi- gated by Vazquez *et al.* [35], which obtained values between 353 and 379 °C. The lower thermal stability of this work's BC membranes of can be explained by the different strains used by Vazquez *et al.* [35]. The third event represents the degradation of carbonaceous residues that extends from 400 to 600 °C, with a percentage of residues found ranging from 2.3 to 23.1%. It was observed that CLS-Inu and P-Inu membranes were the ones with the lowest residue content.

NITROGEN SOURCE: CORN STEEP LIQUOR (CSL)	MASS LOSS 1 (%)	T _{onset2} (°C)	MASS LOSS 2 (%)	T _{max2} (°C)	MASS LOSS 3 (%)	RESIDUAL AT 600 °C (%)
Control	9.1	309	64.9	335	6.9	19.0
CSL-Gly	10.5	281	58.7	319	7.9	23.1
CSL-Man	6.6	313	69.3	339	6.0	17.8
CSL-Glu	4.8	299	70.8	333	5.9	18.3
CSL-Fru	6.7	306	67.0	337	8.7	17.5
CSL-Inu	8.2	273	66.7	316	16.5	8.6
CSL-Suc	9.0	292	66.2	326	7.2	17.5
CSL-Lac	7.9	301	65.0	333	7.8	19.2
NITROGEN SOURCE: PRODEX LAC® (P)	MASS LOSS 1 (%)	T _{onset2} (°C)	MASS LOSS 2 (%)	T _{max2} (°C)	MASS LOSS 3 (%)	RESIDUAL AT 600 °C (%)
Control	9.1	309	64.9	335	6.9	19.0
P-Gly	3.4	302	75.7	333	5.7	15.2
P-Man	7.3	309	67.3	336	6.7	18.6
P-Glu	8.8	301	65.5	334	7.7	18.0
P-Fru	7.1	302	66.0	325	7.2	19.5
P-Inu	8.8	280	67.1	318	21.7	2.3
P-Suc	9.9	298	63.9	332	7.6	18.3
P-Lac	5.0	301	69.4	330	6.5	19.1

Table 2: T_{onset} , T_{max} , percentage of mass loss and percentage of residual mass at 600 °C determined from the TG and DTG curves of the BC samples synthesized from different sources of carbon and having Corn Steep Liquor and Prodex Lac® as sources of nitrogen.

 T_{onset} = extrapolated onset temperature; T_{max} = temperature of maximum mass loss rate.

3.3 Fourier-transform infrared spectroscopy – FTIR

The FTIR spectra of the membranes obtained from the different culture media were carried out to prove the polymer's synthesis is shown in Figure 3.

The main bands of BC control are: a broad band at 3341 cm⁻¹ attributed to the U(OH) of type I cellulose and to intramolecular bonds (3-OH ... O-5); a 2897 cm⁻¹ band attributed to U(CH) and Ua(CH₂); a 1641 cm⁻¹ band characteristic of δ (OH); a band at 1400 cm⁻¹ relative to δ (CH₂); a band at 1369 cm⁻¹ related to δ (CH); a 1335 cm⁻¹ band assigned δ (OH); an intense band at 1159 cm⁻¹ referring to the glycosidic linking ring (C-O-C) derived from the cellulose backbone; a band at 1100 cm⁻¹ referring to U(C 2...O 2); a 1052 cm⁻¹ band corre- sponding to U(CO)/(CC) and another band at 1029 cm⁻¹ attributed to Us(CO)/(CC) and another 1003 cm⁻¹ intense band related to U(C3...O3), referring to the main bond-forming the crosslinking. There are also two tiny bands related to cellulose I_a (750 cm⁻¹) and I_β (710 cm⁻¹). These bands are also present in the other samples, proving BC's production in all sources tested [2, 34 -36]. The bands attributed to BC are also presented in Table 3.



Figure 3: FTIR spectra of membranes synthesized from different carbon sources, having as nitrogen source: a) corn steep liquor (CSL), b) Prodex Lac®.

Table 3: Assignment of bacterial cellulose FTIR absorption bands as they were observed in the membranes synthesized from different carbon sources, having as nitrogen source corn steep liquor (CSL), and Prodex Lac® (P).

	H	CONTROL	CSL-GLY	CSL-MAN	CSL-FRU	CSL-SUC	CSL-INU	CSL-GLU	CSL-LAC
	(cm⁻¹)*								
υ(O-H)									
Celullose I	3340	3341	3340	3347	3347	3341	3341	3341	3327
(3-OHO- 5)	2210	0011	00.0	0017	0017	0011	0011	0011	0021
υ(CH); va	2000	2807	2806	2806	2002	2002	2806	2806	2000
(CH2)	2900	2897	2890	2890	2905	2905	2890	2890	2909
δ(OH)	1641	1642	1645	1645	1645	1640	1645	1645	1645
δ(CH2)	1428	1426	1426	1428	1428	1427	1427	1427	1428
δ(CH)	1369	1364	1364	1367	1369	1364	1367	1367	1369
δ(OH)	1335	1335	1336	1337	1339	1337	1337	1337	1337
va(C-O-C)	1159	1160	1160	1160	1162	1160	1162	1162	1160
υ(C2O2)	1110	1107	1107	1107	1110	1110	1110	1110	1110
υ(C-O)/(C-	1050	1050	1050	1057	1055	1055	1057	1054	1055
C)	1052	1052	1052	1057	1057	1057	1057	1054	1055
vs(C-O)/(C- C)	1020	1020	1020	1020	1020	1020	1020	1020	1020
	1029	1050	1050	1030	1050	1030	1030	1030	1050
v(C3O3)	1003	1002	1002	1002	1000	1000	1001	1001	1001
Cellulose Ia	750	749	749	749	749	750	749	750	750
Celluose Iß	710	709	710	710	709	710	710	710	710
ASSIGNMENT	WAVELENGT H	CONTROL	P-GLY	P-MAN	P-FRU	P-SUC	P-INU	P-GLU	P-LAC
	(cm⁻¹)*								
υ(O-H)	(cm⁻¹)*								
v(O-H) Celullose I	(cm ⁻¹)*	3340	3333	3340	3340	3340	3340	3348	3348
v(O-H) Celullose I (3-OHO- 5)	(cm ⁻¹)* 3340	3340	3333	3340	3340	3340	3340	3348	3348
v(O-H) Celullose I (3-OHO- 5)	(cm ⁻¹)*	3340	3333	3340	3340	3340	3340	3348	3348
v(O-H) Celullose I (3-OHO- 5) v(CH); va	(cm ⁻¹)*	3340	3333	3340	3340	3340	3340	3348	3348
v(O-H) Celullose I (3-OHO- 5) v(CH); va (CH2)	(cm ⁻¹)* 3340 2900	3340 2898	3333 2898	3340 2898	3340 2898	3340 2898	3340 2898	3348 2898	3348 2898
υ(O-H) Celullose I (3-OHO- 5) ν(CH); να (CH2) δ(OH)	(cm ⁻¹)* 3340 2900 1641	3340 2898 1648	3333 2898 1648	3340 2898 1647	3340 2898 1642	3340 2898 1648	3340 2898 1642	3348 2898 1642	3348 2898 1642
υ(O-H) Celullose I (3-OHO- 5) υ(CH); υα (CH2) δ(OH) δ(CH2)	(cm ⁻¹)* 3340 2900 1641 1428	3340 2898 1648 1429	3333 2898 1648 1428	3340 2898 1647 1430	3340 2898 1642 1430	3340 2898 1648 1428	3340 2898 1642 1426	3348 2898 1642 1430	3348 2898 1642 1430
ν(O-H) Celullose I (3-OHO- 5) ν(CH); να (CH2) δ(OH) δ(CH2) δ(CH)	(cm ⁻¹)* 3340 2900 1641 1428 1369	3340 2898 1648 1429 1368	3333 2898 1648 1428 1368	3340 2898 1647 1430 1368	3340 2898 1642 1430 1368	3340 2898 1648 1428 1368	3340 2898 1642 1426 1368	3348 2898 1642 1430 1368	3348 2898 1642 1430 1368
υ(O-H) Celullose I (3-OHO- 5) υ(CH); υa (CH2) δ(OH) δ(CH2) δ(CH) δ(OH)	(cm ⁻¹)* 3340 2900 1641 1428 1369 1335	3340 2898 1648 1429 1368 1336	3333 2898 1648 1428 1368 1337	3340 2898 1647 1430 1368 1337	3340 2898 1642 1430 1368 1337	3340 2898 1648 1428 1368 1337	3340 2898 1642 1426 1368 1337	3348 2898 1642 1430 1368 1337	3348 2898 1642 1430 1368 1337
υ(O-H) Celullose I (3-OHO- 5) ν(CH); va (CH2) δ(OH) δ(CH2) δ(OH) ν(C-O-C)	(cm ⁻¹)* 3340 2900 1641 1428 1369 1335 1159	3340 2898 1648 1429 1368 1336 1161	3333 2898 1648 1428 1368 1337 1161	3340 2898 1647 1430 1368 1337 1163	3340 2898 1642 1430 1368 1337 1161	3340 2898 1648 1428 1368 1337 1159	3340 2898 1642 1426 1368 1337 1161	3348 2898 1642 1430 1368 1337 1161	3348 2898 1642 1430 1368 1337 1164
ν(O-H) Celullose I (3-OHO- 5) ν(CH); νa (CH2) δ(OH) δ(CH2) δ(CH) ν(C-O-C) ν(C-2O2)	(cm ⁻¹)* 3340 2900 1641 1428 1369 1335 1159 1110	3340 2898 1648 1429 1368 1336 1161 1110	3333 2898 1648 1428 1368 1337 1161 1110	3340 2898 1647 1430 1368 1337 1163 1110	3340 2898 1642 1430 1368 1337 1161 1110	3340 2898 1648 1428 1368 1337 1159 1110	3340 2898 1642 1426 1368 1337 1161 1110	3348 2898 1642 1430 1368 1337 1161 1110	3348 2898 1642 1430 1368 1337 1164 1110
υ(O-H) Celullose I (3-OHO- 5) υ(CH); va (CH2) δ(OH) δ(CH2) δ(OH) να(C-O-C) ν(C2O2) ν(C-O)/(C-	(cm ⁻¹)* 3340 2900 1641 1428 1369 1335 1159 1110 1052	3340 2898 1648 1429 1368 1336 1161 1110 1053	3333 2898 1648 1428 1368 1337 1161 1110 1054	3340 2898 1647 1430 1368 1337 1163 1110 1056	3340 2898 1642 1430 1368 1337 1161 1110 1054	3340 2898 1648 1428 1368 1337 1159 1110 1054	3340 2898 1642 1426 1368 1337 1161 1110 1054	3348 2898 1642 1430 1368 1337 1161 1110 1054	3348 2898 1642 1430 1368 1337 1164 1110 1056
υ(O-H) Celullose I (3-OHO- 5) υ(CH); υa (CH2) δ(OH) δ(CH2) δ(OH) υ(C-O-C) υ(C-O)/(C-C) C)	(cm ⁻¹)* 3340 2900 1641 1428 1369 1335 1159 1110 1052	3340 2898 1648 1429 1368 1336 1161 1110 1053	3333 2898 1648 1428 1368 1337 1161 1110 1054	3340 2898 1647 1430 1368 1337 1163 1110 1056	3340 2898 1642 1430 1368 1337 1161 1110 1054	3340 2898 1648 1428 1368 1337 1159 1110 1054	3340 2898 1642 1426 1368 1337 1161 1110 1054	3348 2898 1642 1430 1368 1337 1161 1110 1054	3348 2898 1642 1430 1368 1337 1164 1110 1056
υ(O-H) Celullose I (3-OHO- 5) υ(CH); va (CH2) δ(OH) δ(CH2) δ(OH) va(C-O-C) ν(C2O2) ν(C-O)/(C-C) νs(C-O)/(C-C)	(cm ⁻¹)* 3340 2900 1641 1428 1369 1335 1159 1110 1052 1029	3340 2898 1648 1429 1368 1336 1161 1110 1053 1030	3333 2898 1648 1428 1368 1337 1161 1110 1054 1030	3340 2898 1647 1430 1368 1337 1163 1110 1056 1030	3340 2898 1642 1430 1368 1337 1161 1110 1054 1030	3340 2898 1648 1428 1368 1337 1159 1110 1054 1030	3340 2898 1642 1426 1368 1337 1161 1110 1054 1030	3348 2898 1642 1430 1368 1337 1161 1110 1054 1030	3348 2898 1642 1430 1368 1337 1164 1110 1056 1030
ν(O-H) Celullose I (3-OHO- 5) ν(CH); νa (CH2) δ(OH) δ(CH2) δ(OH) ν(C-O-C) ν(C-O)/(C-C) ν(C-O)/(C-C) ν(C3O3)	(cm ⁻¹)* 3340 2900 1641 1428 1369 1335 1159 1110 1052 1029 1003	3340 2898 1648 1429 1368 1336 1161 1110 1053 1030 1002	3333 2898 1648 1428 1368 1337 1161 1110 1054 1030 1000	3340 2898 1647 1430 1368 1337 1163 1110 1056 1030 1000	3340 2898 1642 1430 1368 1337 1161 1110 1054 1030 1004	3340 2898 1648 1428 1368 1337 1159 1110 1054 1030 1000	3340 2898 1642 1426 1368 1337 1161 1110 1054 1030 1000	3348 2898 1642 1430 1368 1337 1161 1110 1054 1030 1003	3348 2898 1642 1430 1368 1337 1164 1110 1056 1030 1000
υ(O-H) Celullose I (3-OHO- 5) υ(CH); va (CH2) δ(OH) δ(CH2) δ(OH) v(C-O-C) ν(C-O)/(C-C) ν(C-3O3) Cellulose I _α	(cm ⁻¹)* 3340 2900 1641 1428 1369 1335 1159 1110 1052 1029 1003 750	3340 2898 1648 1429 1368 1336 1161 1110 1053 1030 1002 749	3333 2898 1648 1428 1368 1337 1161 1110 1054 1030 1000 748	3340 2898 1647 1430 1368 1337 1163 1110 1056 1030 1000 750	3340 2898 1642 1430 1368 1337 1161 1110 1054 1030 1004 -	3340 2898 1648 1428 1368 1337 1159 1110 1054 1030 1000 750	3340 2898 1642 1426 1368 1337 1161 1110 1054 1030 1000 748	3348 2898 1642 1430 1368 1337 1161 1110 1054 1030 1003 749	3348 2898 1642 1430 1368 1337 1164 1110 1056 1030 1000 749

v = stretching; $\delta =$ angular bending; s = symmetric; a = asymmetric.

* Wavenumber obtained from the literature [2, 34 -36]

3.4 Scanning electron microscopy – SEM

The micrographs of the surfaces of the BC membranes obtained from the different carbon sources are presented in Figure 4 and 5, using as a nitrogen source, corn steep liquor, and Prodex Lac®, respectively.



Figure 4: Micrographies of BC obtained from CSL and different sources of carbon: a) control; b) CSL-Gly; c) CSL-Man; d) CSL-Fru; e) CSL-Suc; f) CSL-Inu; g) CSL-Glu e h) CSL-Lac.



Figure 5: Micrographies of BC obtained from Prodex Lac® and different carbon sources: a) control; b) P-Gly; c) P-Man; d) P-Fru; e) P-Suc; f) P-Inu; g) P-Glu e h) P-Lac.

The membrane produced in yeast extract, peptone, and mannitol (control) medium (Figure 4a and 5a), as well as the other synthesized membranes, presented a network of randomly distributed nanofibers with high aspect ratio and diameter varying between 18 and 90 nm, measured with the ImageJ software, strong morphological characteristics of BC [37, 38].

The membranes of BC produced in a medium using Corn Steep Liquor with fructose (CSL-Fru) (Figure 4d) and Prodex Lac® with fructose (P-Fru), inulin (P-Inu) and mannitol (P-Man) presented in (Figure 5c, 5d and 5f), respectively showed good dispersion of the nanofibers within the matrix, with no visible aggregates, like other micrographs typical of BC found in the literature [31, 35].

The membranes of BC produced in medium containing corn steep liquor with glycerol (CSL-Gly) (Figure 4b), fructose (CSL-Fru) (Figure 4d), inulin (CSL-Inu) (Figure 4f), glucose (CSL-Glu) (Figure 4g) and lactose (CSL-Lac) (Figure 4h) also showed good dispersion of the nanofibers in the matrix, but in a more dense form, which was also observed in samples cultured in Prodex Lac® medium with glucose (P-Glu) (Figure 5g) e lactose (P-lac) (Figure 5h). They also appeared smooth and dense.

The membranes of BC produced in medium containing corn steep liquor and sucrose (CSL-Suc) (Figure 4e) and corn steep liquor and lactose (CSL-Lac) (Figure 4h) were also dense. However, although nanofibers have been observed, they are heterogeneously arranged in the matrix, as highlighted in the figures (circle). The same observation can be observed for the membranes obtained in culture medium containing Prodex Lac® with glycerol (P-Gly) (Figure 5b) and Prodex Lac® with sucrose (P-Suc) (Figure 5e).

Finally, in the micrograph of the BC membrane produced in a medium containing corn steep liquor and mannitol (Figure 5f) it is impossible to observe the nanofibers in the matrix. This membrane was smooth, dense and with presence of whitish aggregates.

The formation of BC pellicle may be impacted by the overall medium composition, carbon source, and factors related to the operational conditions (e.g. pH, temperature, agitation or not of the medium, size and shape of the container, etc.). MOHAMMADKAZEMI *et al.* [33] and KLEMM *et al.* [39] evaluated BC production in different carbon sources and culture media and found that the medium may result in different morphologies.

According to Vieira *et al.* [40] all the BC membranes tend to have a similar structure. However, the pore size and quantity are different due media components and cellulose fibers' interaction.

These differences may influence cellulose's final application, where more porous or compact structures are required to create a device or product [41]. The high aspect ratio of nanofibrils affects the membrane's mechanical properties such as tensile strength elasticity [37].

4. CONCLUSIONS

The results obtained show that it is possible to obtain BC from different culture media compositions, varying nitrogen and carbon sources, using the bacterium *K. hansenii* in static culture.

Among the nitrogen sources analyzed, Prodex Lac® was more efficient, resulting in higher yields of BC. The sources of carbon, fructose, mannitol, and lactose presented higher yields than the others. The results of TGA indicate that all the samples of BC have similar thermal behavior, and the most thermally stable were CSL-Man (339 °C), CSL-Fru (337 °C) and P-Man (335 °C). The FTIR results show that the different samples are chemically equivalent to the structures cited in the literature. The micrographs showed that the medium might influence BC's morphology, but in general, the microstructure consists of an interwoven network of randomly distributed cellulose nanofibers, an essential feature for several applications.

Following the structure presented, it is concluded that BC's production using alternative means and low cost is feasible and that the material obtained presents the characteristic thermal, physical and chemical prop- erties of the cellulose.

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