# ESTIMATION OF THE KINETIC HEAD COEFFICIENT (k) BASED ON THE GEOMETRIC CHARACTERISTICS OF EMITTER PIPES<sup>1</sup>

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**ABSTRACT**: The objective of this study was to determine the variability of the head loss as a function of the emitter geometry as well as to develop a relation between local head loss caused by the emitter insertion and geometric characteristics of the emitter pipe, using index of obstruction for dripper pipes with non-coaxial emitters. For this, an experimental bench was developed to control the system and obtain the variables pertinent to the study. From the value of the total head loss in the emitter pipe and the value obtained with calculation of the distributed head loss in the pipe, the difference of these values was local head loss caused by the insertion of the emitter. Total head loss in the emitter pipe and local head loss on the emitter presented a potential relation with flow rate. The kinetic head coefficient (k), for each emitter studied, was obtained from the local head loss on the emitter and the kinetic head. A model for estimating the k coefficient based on the obstruction index was then generated.

KEYWORDS: non-coaxial emitters, obstruction index, trickle irrigation, head loss.

## **INTRODUCTION**

The Brazilian irrigated area occupies approximately 4.5 million hectares, and is responsible for 16% of agricultural production and 35% of the economic value of the total production of the country (Paulino et al., 2011).

Trickle irrigation is highlighted in relation to the others irrigation methods, since it has the potential to present high indices of water application efficiency (Frizzone et al., 2012; Provenzano et al., 2013). Studies show the efficiency of trickle irrigation systems compared with the other systems, in different crops, without negatively influencing productivity (Andrade et al., 2014; Carvalho et al., 2014; Geisenhoff et al., 2015; Uribe et al., 2013).

The correct estimate of head loss is an important factor in trickle irrigation projects as it influences the total dynamic head, and in turn, in the choice of the pumping system (Cardoso & Frizzone, 2014). According to Al-Amoud (1995) one of the factors that interfere with the lateral line head loss is the obstruction caused by the emitter, which can increase the total head loss in the system by up to 33%.

The emitters are one of the main components of drip irrigation (Frizzone et al., 2012). The local head loss caused by the emitters can be estimated by the general equation of local head loss which presents a portion k of the Bernoulli kinetic head ( $V^2/2g$ ) known as the Reynolds similarity principle, and it is represented by Equation 1 (Azevedo Netto & Fernandes, 2015).

$$hf_{e} = k \cdot \frac{V^{2}}{2 \cdot g}$$
(1)

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#### where,

- hf<sub>e</sub> local head loss on the emitter, m;
- k kinetic head coefficient, dimensionless;
- V mean velocity at uniform pipe section, m s<sup>-1</sup>; and
- g acceleration of gravity,  $9.806 \text{ m s}^{-2}$ .

The kinetic head coefficient (k) is dependent on the viscous forces and the emitter geometry. In studies carried out by Bagarello et al. (1997), Gomes et al. (2010), Provenzano et al. (2005) and Rettore Neto et al. (2009) it was evidenced that for conditions where Reynolds number (Re) is greater than 10,000 the viscous forces become negligible, thus, the obstruction becomes the main cause of the local head loss. In order to evaluate the head loss as a function of the obstruction, Bagarello et al. (1997) developed an exponential equation (Equation 2) based on the Obstruction Index (Equation 3). For this, the authors used the obstruction ratio (Equation 4) obtained through the obstructed area by the emitter and the pipe area.

$$\mathbf{k} = \boldsymbol{\alpha} \cdot \mathbf{O}\mathbf{I}^{\boldsymbol{\beta}} \tag{2}$$

$$OI = \frac{\left(1 - r\right)^2}{r^2}$$
(3)

$$\mathbf{r} = \frac{\mathbf{A}_{\mathrm{r}}}{\mathbf{A}_{\mathrm{0}}} \tag{4}$$

where,

- k kinetic head coefficient, dimensionless;
- OI obstruction index, dimensionless;
- $\alpha$  and  $\beta$  adjustment coefficients, dimensionless;
- r obstruction ratio, dimensionless;
- $A_0$  pipe cross-section area, mm<sup>2</sup>, and
- $A_r$  reduced pipe cross-section area on emitter insertion, mm<sup>2</sup>.

However, due to the large quantity and variety of emitter pipes on the market studies are needed to generate or improve models for estimating the kinetic head coefficient based on the emitter characteristics. In this sense, this study aims to determine the variability of head loss as a function of the emitter geometry as well as to develop relation between the local head loss caused by the emitter insertion and the geometric characteristics of the pipe through the use of obstruction index for emitter pipes with non-coaxial emitters.

### **MATERIAL AND METHODS**

The experiment was carried out in the Irrigation Laboratory of the Center of Technological Development of the Federal University of Pelotas (CDTec / UFPel). The three models of studied emitters are integrated into the pipe, non-coaxial type. The models and characteristics reported by the manufacturer are described in Table 1.

Brand	AZUD	NaanDanJain	Rain Bird
Model	Premier Line PC	Amnon Drip AS	XF-SDI
Self-compensating	Yes	Yes	Yes
Antidrenant	No	Yes	No
Nominal flow rate (1 h <sup>-1</sup> )	2.30	1.60	2.27
Nominal diameter (mm)	16	16	16
Internal diameter informed (mm)	13.70	13.90	13.61
Wall thickness (mm)	0.90	1.00	1.24
Spacing between emitters (m)	0.50	0.33	0.30
Minimum working pressure (bar/mH <sub>2</sub> O)	0.5 / 5.10	0.5 / 5.10	0.59 / 6.02
Maximum working pressure (bar/mH2O)	4.0 / 40.79	4.0 / 40.79	4.14 / 42.22

TABLE 1. Models of emitter pipes studied and technical characteristics according to the manufacturer.

To conduct the study an experimental bench was used which had the necessary equipment to control the system and data acquisition as shown in Figure 1.

The experimental bench is connected to a 372-liter reservoir and a pump motor system, brand KSB model Hidrobloc P1000T, of 1 hp. A thermometer was used to verify the temperature with a scale of 0 to 50°C and precision of 1°C trapped inside the reservoir. The water for the study is from the public water supply system. To avoid impurities they used  $1\frac{1}{2}$ " and 120 mesh Y-disc filter manufactured by Plasnova Tubos.

The flow values were obtained using a Krone-Conaut electromagnetic flowmeter with certified operating range from 0 to 3.5 m<sup>3</sup> h<sup>-1</sup>, and an accuracy of 0.5% mv (measured value) transformed by means of the continuity equation into flow velocities. To verify the pressure at the beginning of the drip line it was used a Lámon digital manometer with a service range of 0 to 200 mH<sub>2</sub>O and precision of 0.1% FS. The pressure difference between the beginning and the end of the drip line was performed using a differential manometer in "U" with mercury which has specific gravity ( $\gamma_{Hg}$ ) 13,600 kgf m<sup>-3</sup>.

The pressure was maintained constant during all the tests at 20 mH<sub>2</sub>O varying only the flow velocity inside the piping to avoid changes in the pipe diameter which would cause errors in the correct estimation of the head loss values (Rettore Neto et al., 2013; Rettore Neto et al., 2014; Rettore Neto et al., 2016).

For each value of mean velocity the respective value of the head loss was obtained in the emitter pipe. Four replicates were performed for each emitter pipe model. In order to standardize the tests the values of the data pairs were collected in descending order of flow, that is, the test was started with higher values of velocity. In order not to change the flow rate along the emitter pipe, all emitters were sealed, and the Reynolds number was used to classify the flow regime.



- 2 Centrifugal pump
- 3 Electromagnetic flowmeter
- 4 Disc filter
- 5 Gate valve

- 7 Digital manometer
- 8 Connection of differential manometer
- 9 Emitter pipe
- 10 Mercury differential manometer

FIGURE 1. Experimental bench plot for head loss determination.

The geometric characteristics of the pipes and the emitters (wet areas and perimeters of the cross sections) were obtained through an optical profile projector, Starret HB 400, and drawing software (AutoCAD) with the assistance of the Irrigation Laboratory at the School of Agriculture Luiz de Queiroz (ESALQ / USP), and are presented in Table 2. For the length pipe determination and spacing between emitters was used measuring tape. The number of emitters in the pipe tested varies according to the spacing between them, but it was chosen to keep the length near the maximum length of the bench (10 meters).

For the pressure outlet connections of the differential manometer the described methodology by Rettore Neto et al. (2009), where the holes in the pipes were made with a stainless steel rod with diameter of 2.4 mm with a pointed end. First, a marker hole was made and after, inserted the heated driller. At the time of removal of the driller swivel rotating movements were made avoiding possible accumulation of material from the hole inside the pipe.

To connect the manometer to the pressure outlet we used PVC clamps with internal diameter equal to the outside diameter of the pipe. So that there was no strangulation of the section, the clamp was divided into two parts of equal size, and was arranged on the pipe. To fix them in the emitter pipe we used two wrapping metal clamps without pressing it.

The first pressure outlet was installed after the first emitter at a distance of half the emitter spacing, and the second pressure outlet was installed at half the spacing before the last emitter maintaining the pressure outlet between two emitters.

	AZUD Premier Line PC		NaanDanJain Amnon Drip AS		Rain Bird XF-SDI	
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	μ	σ	μ	σ	μ	σ
$A_0 (mm^2)$	142.73	2.2829	143.06	6.5619	146.33	1.8399
WP (mm)	42.35	0.3388	42.39	0.9768	42.88	0.2699
$A_r (mm^2)$	88.65	3.4316	97.74	4.6966	95.72	4.194
$WP_r$ (mm)	52.99	0.6548	60.05	1.1943	64.39	0.9143
D (mm)	13.48	-	13.5	-	13.65	-
D <sub>r</sub> (mm)	6.69	-	6.51	-	5.95	-
OI	0.37	-	0.22	-	0.28	-
L (m)	10	-	10.23	-	10.2	-
n <sub>e</sub>	20	-	31	-	34	-
n	197	-	178	-	197	-

TABLE 2. Mean values ( $\mu$ ) and standard deviation ( $\sigma$ ) of the geometric characteristics of the studied emitters pipes.

 $A_0$  - pipe cross-section area, mm<sup>2</sup>; WP - pipe wet perimeter, mm;  $A_r$  - reduced pipe cross-section area on emitter insertion, mm<sup>2</sup>; WP<sub>r</sub> - wet perimeter of pipe reduced cross-section, mm; D - inner pipe diameter, mm; D<sub>r</sub> - hydraulic diameter of pipe reduced cross-section, mm; OI - obstruction index, dimensionless; L - pipe length, m; n<sub>e</sub> - number of emitters in the pipe, dimensionless; n - number of data pairs "Head Loss x Flow", dimensionless.

Considering the piping level and with sealed emitters using silicon, that is, with no change in position head and kinetic head, the total head loss in the emitter pipe can be considered as the difference in pressure between the start and the end of the pipe. To measure the pressure difference we used the differential manometer in "U".

The total head loss in the emitter pipe was quantified as a function of the flow rate using a potential type model (Equation 5) as proposed by Gomes et al. (2010).

$$hf_{t} = A \cdot Q^{B}$$
(5)

where,

 $hf_t$  - total head loss in the emitter pipe, m;

Q - flow rate, m<sup>3</sup> s<sup>-1</sup>, and

A and B - adjustment coefficients, dimensionless.

In order to obtain the local head loss on the emitter it is necessary to estimate the distributed head loss in the pipe, and for this we used the universal equation with the coefficient f determined by the Blasius equation (Equation 6), with coefficients proposed by Rettore Neto et al. (2009), for polyethylene pipes.

$$\mathbf{f} = \mathbf{c} \cdot \mathbf{R} \mathbf{e}^{-\mathbf{m}} \tag{6}$$

where,

f - Darcy friction factor, dimensionless;

Re - Reynolds number, dimensionless, and

c and m - adjustment coefficients, c = 0.296 and m = 0.25.

From the total head loss in the emitter pipe, distributed head loss in the pipe, and the number of emitters was obtained the local head loss on the emitter (Equation 7).

$$hf_{e} = \frac{hf_{t} - hf_{d}}{n_{e}}$$
(7)

where,

hf<sub>e</sub> - local head loss on the emitter, m;

 $hf_t$  - total head loss in the emitter pipe, m;

hf<sub>d</sub> - distributed head loss in the pipe, m, and

n<sub>e</sub> - number of emitters in the emitter pipe, dimensionless.

In possession of flow rate and local head loss on the emitter data, was adjusted an exponential model as shown in [eq. (8)], according to preliminary studies by Gomes et al., (2010).

 $hf_a = a \cdot Q^b$ 

where,

hfe - local head loss on the emitter, m;

Q - flow rate,  $m^3 s^{-1}$ , and

a and b - adjustment coefficients, dimensionless.

Table 3 shows the maximum and minimum values for each emitter pipe model studied on variables observed in the study, flow rate, temperature, total head loss in the emitter pipe, and variables calculated, mean velocity at uniform pipe section, viscosity, Reynolds number, Darcy friction factor, distributed head loss in the pipe and local head loss on the emitter .

To determine the k coefficient on the head loss general equation (Equation 1) a linear regression was performed from the pairs of local head loss and kinetic head data ( $V^2/2g$ ). In the adjustment of the proposed model by Bagarello et al. (1997) (Equation 2) we used a data group by Provenzano & Pumo (2004); Provenzano et al. (2005); Rettore Neto et al. (2009) which had data of non-coaxial emitter, in addition to the obtained data of this study. After that a potential equation was adjusted determining the coefficients  $\alpha$  and  $\beta$ .

	AZUD		NaanDanJain		Rain Bird	
	Premier Line PC		Amnon Drip AS		XF-SDI	
	Maximum	Minimum	Maximum	Minimum	Maximum	Minimum
$Q(m^3 s^{-1})$	28.8 x 10 <sup>-5</sup>	4.5 x 10 <sup>-5</sup>	30.8 x 10 <sup>-5</sup>	4.0 x 10 <sup>-5</sup>	30.2 x 10 <sup>-5</sup>	4.5 x 10 <sup>-5</sup>
hf <sub>t</sub> (m)	8.9838	0.2016	10.6470	0.3402	9.9288	0.3024
T (°C)	23.7	17.5	23.0	17.0	22.0	18.0
V (m s <sup>-1</sup> )	2.15	0.28	2.01	0.32	2.06	0.31
V <sup>2</sup> /2g (m)	23.65 x 10 <sup>-2</sup>	0.41 x 10 <sup>-2</sup>	20.62 x 10 <sup>-2</sup>	0.51 x 10 <sup>-2</sup>	21.70 x 10 <sup>-2</sup>	0.48 x 10 <sup>-2</sup>
$v (m^2 s^{-1})$	1.07 x 10 <sup>-6</sup>	9.27 x 10 <sup>-7</sup>	1.09 x 10 <sup>-6</sup>	9.41 x 10 <sup>-7</sup>	1.06 x 10 <sup>-6</sup>	9.63 x 10 <sup>-7</sup>
Re	28757	4105	27518	4113	27836	4283
f	0.0370	0.0227	0.0370	0.0230	0.0366	0.0229
hf <sub>d</sub> (m)	3.9800	0.1113	3.6427	0.1410	3.7370	0.1312
hf <sub>e</sub> (m)	0.2498	0.0045	0.2331	0.0063	0.1831	0.005

TABLE 3. Maximum and minimum values of the variables observed and calculated in the tests.

Q - flow rate, m<sup>3</sup> s<sup>-1</sup>; hf<sub>t</sub> - total head loss in the emitter pipe, m; T - temperature inside reservoir, °C; V - mean velocity at uniform pipe section, m s<sup>-1</sup>;  $V^2/2g$  - kinetic head, m; v - kinematic viscosity, m<sup>2</sup> s<sup>-1</sup>; Re - Reynolds number, dimensionless; f - Darcy friction factor, dimensionless; hf<sub>d</sub> - distributed head loss in the pipe, m; hf<sub>e</sub> - local head loss on the emitter, m.

### **RESULTS AND DISCUSSION**

Figures 2.A, 2.C and 2.E show data of total head loss in the emitter pipe as function of the flow rate, as well as the obtained regression equation according to Equation 5. Yet in figures 2.B, 2.D and 2.F, we can observe the local head loss on the emitter according to the flow rate, and its respective regression equation (Equation 8).

(8)



FIGURE 2. Total head loss in the emitter pipe  $(hf_t)$  and local head loss on the emitter  $(hf_e)$  as a function of flow rate (Q).

It can be seen in Figures 2.A, 2.C and 2.E that the total head loss in the emitter pipe has a potential relation with the flow rate, presenting Pearson correlation coefficients with values above 0.99 which represents that more than 99% of data can be explained by the equation presented in the graphs.

The regression coefficient A was  $21.8 \times 10^6$ ,  $34.6 \times 10^6$  and  $63.5 \times 10^6$  for the Rain Bird XF-SDI, AZUD Premier Line PC and Naan Dan Jain Amnon Drip AC emitter pipes, respectively. In relation to coefficient B it can be observed that the values were 1.80 for the Rain Bird SF-SDI, 1.88 for AZUD Premier Line PC and 1.92 for Naan Dan Jain Amnon Drip AC. These values are close to those observed by Gomes et al. (2010) which obtained coefficients between 1.76 and 1.84 in studies with coaxial emitters.

The local head loss on the emitter presented Pearson correlation coefficients higher than 0.99 in relation to the flow rate, for the three emitter models present in the study (Figures 2.B, 2.D and 2.F), that is, the local head loss can be explained by the flow rate. Zitterell et al. (2014) found similar behavior for this relationship in studies with connectors for trickle irrigation systems. The Naan Dan Jain Amnon Drip AS emitter pipe presented the highest dispersion in the data which according to Rettore Neto et al (2009) can be explained due to the lack of uniformity on the emitter insertion inside the pipe.

The coefficient a (Equation 8) was  $4.9 \times 10^5$ ,  $20.9 \times 10^5$  and  $27.7 \times 10^5$  for the Rain Bird XF-SDI, AZUD Premier Line PC and Naan Dan Jain Amnon Drip AS, emitters respectively. Gomes et al. (2010) found values between  $2.2 \times 10^5$  and  $28.3 \times 10^5$ . This variation may be due to the type of studied emitter and the obstruction index caused by its insertion.

In Figures 3.A, 3.C and 3.E is the relationship between the local head loss on the emitter, and the kinetic head and in Figures 3.B, 3.D and 3.F are the values of kinetic head coefficient for the studied emitters in relation to the Reynolds number.

It can be observed in Figure 3 that the k values are 0.8625, 1.0337 and 1.0658 for the Rain Bird XF-SDI, AZUD Premier Line PC and Naan Dan Jain Amnon Drip AS emitters, respectively. For all studied emitters the Pearson's correlation coefficient showed values above 0.99 showing that the local head loss on the emitter is related to the kinetic head.

In similar studies Rettore Neto et al. (2009) found k values of 0.3378, 0.5295, 0.8445 and 1.2719 with obstruction index of 0.0799, 0.1765, 0.1882 and 0.5649, respectively. Gomes et al. (2010), in studies with coaxial emitter pipes, found k values of 0.1497, 0.3577, 1.1478 and 1.2193 with obstruction indices of 0.0541, 0.1316, 1.1702 and 1.2336. It is clear that the results of the literature demonstrate that k coefficient presents variability according to studied emitter, presenting relation with the obstruction caused by the insertion inside the pipe. This shows the importance of this kind of studies since from the values of k it is inferred the local head loss caused by the emitter in the pipe.

The k coefficient presents dependence on Reynolds number and the geometric characteristics of the obstructing element however in cases where the Reynolds number is high the head loss tends to be dependent only on the emitter obstruction. Thus, in Figures 3.B, 3.D and 3.F present the values of k for the studied emitter pipes in relation to the Reynolds number.

It can be observed in Figures 3.B, 3.D and 3.F that for high Reynolds number values the head loss depends on the emitter geometry, and not on the viscous forces, a fact that can be proven by the stabilization of k values with number of Re>10,000. All the studied emitters presented similar behavior which is in accordance with the literature, such as the studies by Bagarello et al. (1997), Gomes et al. (2010), Provenzano & Pumo (2004), Provenzano et al. (2005) and Rettore Neto et al. (2009).



FIGURE 3. Local head loss on the emitter (hf<sub>e</sub>) as a function of kinetic head ( $V^2/2g$ ) and kinetic head coefficient (k) as a function of Reynolds number (Re).

Figure 4 show the values of k as function of the obstruction index, obtained with the experimental data and the k values observed in the literature by Provenzano & Pumo (2004); Provenzano et al. (2005); Rettore Neto et al. (2009).



FIGURE 4. Kinetic head coefficient (k) as a function of obstruction index (OI).

In Figure 4 the dashed line corresponds to Equation 2 applied with coefficient  $\alpha$  equal to 1.66 and coefficient  $\beta$  equal to 0.413.

Bagarello et al. (1997) compiling data from Al-Amoud (1995) found for online emitters coefficients  $\alpha$  and  $\beta$  of 1.68 and 0.645, and Cardoso & Klar (2014) observed  $\alpha$  of 1.228 and  $\beta$  of 0.507. Gomes et al. (2010) in similar studies, but with coaxial emitters obtained 1.387 for  $\alpha$  and 0.577 for  $\beta$ .

However, by performing an analysis with integrated wafer type emitters Rettore Neto et al. (2009) found values of 1.94 for  $\alpha$ , and 0.595 for  $\beta$ , for domain 1.08 <A/A<sub>r</sub> <1.75. The proposed model by the present study added six new pairs of data, all within the same domain.

All the studies carried out in this sense found similar behavior of the data however, further studies are still necessary in order to allow the best adjustment of the model due to the great variability of the emitters form. It can be stated that physically the regression equation is coherent because when there is a zero obstruction index, that is, no obstruction in the pipe, k coefficient is also zero, with no local head loss.

#### CONCLUSIONS

The total head loss in the pipe and local head loss on the emitter presented potential relation in function to the flow rate in each studied model of the emitter pipe.

The Rain Bird XF-SDI emitter presented kinetic head coefficient (k) of 0.8625 while the emitters AZUD Premier Line PC and Naan Dan Jain Amnon Drip AS presented values of 1.0337 and 1.0658 respectively.

The kinetic head coefficient can be estimated by the equation ( $k = 1.66 \text{ IO}^{0.413}$ ) with  $r^2 = 0.75$  for the OI range from 0.008032 to 0.5649.

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