

## Rheology applied to the environmental management of mineral tailings: focus on safer disposal and water reuse

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**Bruna Camara Trampus<sup>1,2</sup>**

<https://orcid.org/0000-0002-0468-0205>

**Silvia Cristina Alves França<sup>1,3</sup>**

<https://orcid.org/0000-0003-2645-9007>

<sup>1</sup>CETEM – Centro de Tecnologia Mineral (Centre for Mineral Technology), Rio de Janeiro - RJ, Brasil

E-mails: <sup>2</sup>[btrampus@cetem.gov.br](mailto:btrampus@cetem.gov.br),

<sup>3</sup>[sfranca@cetem.gov.br](mailto:sfranca@cetem.gov.br)

### Abstract

Mining activities worldwide are subject to serious geotechnical accidents involving tailings dams. Therefore, many studies have focused on tailings dewatering before their deposition. This article studies the rheological properties of flocculated and thickened nickel tailings in order to determine the effect of the initial solid concentration and type of rheology modifying agents (two anionic polymeric flocculants) on their stability for disposal in dams. The sediment was submitted to rheological tests, with the vane technique, and slump tests, to obtain information about static and dynamic yield stress and slump height, respectively. The results showed a strong influence of the initial solid concentration and the polymeric flocculant on the particle aggregation. Both particle cohesion and yield stress of the sediment increased, reaching static yield stress of around 1,400 Pa. Both flocculants were efficient in thickening by batch sedimentation, allowing water recycling in the range of 70-90% with turbidity less than 100 NTU and the production of sediment with static yield stress much higher than specified for mineral paste.

**keywords:** rheology; yield stress; mineral paste; water recycling; nickel tailings.

### 1. Introduction

The mining industry is one of the main contributors for the production of raw materials used to manufacture goods in a wide range of sectors. As resource consumption continues to increase, mining has become one of the most important economic activities. However, ore processing demands large volumes of water and generates an enormous amount of tailings, which are commonly deposited as slurries with a low percentage of solids in tailings dams (not adequate term) (Sofrá and Boger, 2002; Boger, 2009). Improper tailings management can lead to the release of millions of cubic meters of slurry (mineral pulp), and cause serious disasters, such as the Fundão tailings dam failure at the Samarco mine in Brazil on November 5<sup>th</sup>, 2015 and the partial dam failure at the Tonglvshan mine in China on March 12<sup>th</sup>, 2017 (Wise Uranium Project, 2017). As a result, tailings thickening or dewatering before deposition makes disposal of these tailings in the environment safer, besides allowing partial recovery of process water and reduction of the volume of tailings and

the area required for storage. However, this increases the difficulties and production costs (Sofrá and Boger, 2002, 2011; Boger, 2009, 2013).

Mineral pastes are defined as homogeneous and dense material with low or no free water level, without particle size segregation, and a laminar flow with positive displacement pumps (Sofrá and Boger, 2002; Boger, 2013). The difference between pastes and thickened tailings is determined by yield stress, which measures the ability of the tailings to withstand deformation. Pastes are thickened tailings with a lower limit of the yield stress of 200 Pa (Clayton *et al.*, 2003; Boger, 2013; Fitton and Seddon, 2013). Thus, a good understanding of the rheological properties of paste is important for the mining industry.

The solid waste paste filling technology was introduced at the mining with cemented backfill. Therefore, the addition of different cementitious materials to the mineral tailings, decrease the volume of tailing, but increases the costs (Deng *et al.*, 2017). However, previous studies have

investigated the use of rheology modifying agents, such as water-soluble polymers with high molecular weight, for the production of thickened tailings and pastes (Dias *et al.*, 2004; Gadelha and França, 2015). The existence of polymer-slurry interaction enables the formation of flocs, which are irregularly shaped aggregates with liquid in their structures. Their characteristics are highly dependent on the type of polymer-slurry interaction and the floc formation process (Dias *et al.*, 2004; Jarvisa *et al.*, 2005). Therefore, the yield stress is strongly dependent on the dosage and polymer structure as well as tailings characteristics, such as particle size and shape, solids concentration, surface charge density, solid density, bulk density and pH (Sofrá and Boger, 2011; Parsapour *et al.*, 2014; Wu *et al.*, 2015).

This paper reports the development of a flocculant system for the mining industry that can simultaneously target several properties, such as the solid-liquid separation process, water recovery (qualitative and quantitative) and paste formation

## 2. Materials and methods

The materials and experimental procedure were based on the data obtained by Andrade (2016) for flocculation and

### 2.1. Materials

The material used in the experimental study was a tailings sample produced by the flotation of nickel sulphide ore, obtained from a tailings dam in the state of Minas Gerais.

The flocculants studied were two

### 2.2 Tailings characterization

The nickel tailings were characterized according to the particle size distribution by laser diffraction, with a Malvern Mastersizer 2000.

The average particle electrophoretic mobility was used to calculate the zeta potential (Lima and Luz, 2007;

thickening of nickel tailings. Pulps were studied with solid concentration (C0) from 10 to 23% (w/w) and were submitted to

anionic polymers manufactured by Basf, referred to as R-10 and R-90. In both cases the flocculants were hydrated with distilled water and diluted to 0.5 g/L. In order to keep the polymer dose as low as possible, based on the

Bárány *et al.*, 2011), since the nickel tailings are composed of a mixture of particles of different mineralogical species. 10% (w/w) solid slurries were prepared with KCl indifferent electrolytes (0.01 and 0.001 M). The measurements were conducted at room

flocculation and batch sedimentation tests in order to obtain information about sediment cohesion.

literature data obtained by Andrade (2016), they were used at the dosage of 80 g/t of dry solids. This is the minimum dosage to obtain appropriate turbidity of the supernatant and sedimentation rate.

temperature and pH range of 2 to 12, adjusted with KOH and HCl dilute solutions, using a Malvern ZetaSizer Nano ZS (Malvern Instruments Inc.). The zeta potential was calculated using the experimentally-determined data and the Henry's model.

### 2.3 Preparation of thickened flocculated tailings

The pulps were prepared with nickel tailings and tap water, flocculated in a Jar Test equipment and transferred to a 2 L graduated cylinder for batch sedimentation. The flocculant solution was then added to the slurry and stirred at 300 rpm for 1 min, followed by slow stirring at 150

rpm for 2 min. Considering the importance of shear rate and solids concentration in the flocculation rate, the operational conditions can be expressed in terms of Camp number (time [s] x shear gradient [s<sup>-1</sup>]), given respectively by  $C_{fast} = 33,000$  and  $C_{slow} = 21,600$ .

The flocculated pulp was transferred to the graduated cylinder, and was set aside undisturbed for 24 h. After that, the supernatant liquid was removed and the sediment (underflow) was studied to determine its properties, with the equipment and techniques presented in the items that follow.

### 2.4 Thickened tailings characterization

#### 2.4.1 Slump test

The slump test is a technique standardized and is conventionally used to determine the consistency of fresh concrete. This technique is applied with conical geometry. However, according to the results of various studies, adaptation to cylindrical geometry can be used to evaluate the consistency of mineral suspensions

(Pashias *et al.*, 1996; Clayton *et al.*, 2003; Osorio *et al.*, 2008; Boger, 2009; Mizani and Simms, 2016).

The experimental procedure of this study can be observed in Figure 1, in which a small PVC cylinder (radius = height = 53 mm) is filled with bottom sediment from the graduated

cylinder and then removed vertically to allow the material to slump under its own weight. Therefore, it is possible to calculate the height difference between the cylinder and the sediment (Equation 1), and the slump height (SH) (Equation 2). This provides an empirical measurement of tailings consistency.

$$h = H - H_s \quad (1)$$

$$\% SH = (h / H) \times 100 \quad (2)$$

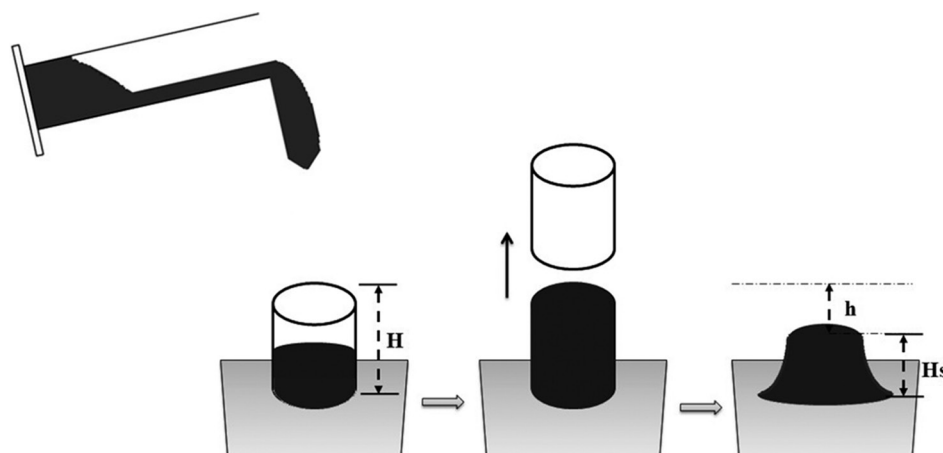


Figure 1  
Schematic of slump test with cylinder.

### 2.4.2 Shear rheology

Yield stress ( $\tau_0$ ) can be estimated from different rheometry techniques. All  $\tau_0$  data presented in this study were obtained using the vane technique, to eliminate slip (Boger, 2009, 2013; Sofrá and Boger, 2011). Two measurement techniques were used to obtain the  $\tau_0$ : direct method and regression method based on

$$\tau = \tau_0 + K_h \dot{\gamma}^{n_h} \quad (3)$$

Where,  $\tau_0$  is the H-B YS, K is the fluid consistency index, and n is the flow behavior index.

Thus, in this study, the  $\tau_0$  was obtained for the bottom and top sediments of the graduated cylinder with a Haake RheoStress 1 rotational rheometer, and the experimental procedure was performed in three stages at room tempera-

ture. First, the sediment's (bottom and top samples) yield stress was obtained by the direct method applying a constant shear rate of  $0.1 \text{ s}^{-1}$  for a maximum time of 300 s. These data are referred to as static  $\tau_0$ . After this, the sediment was subjected to a constant high shear, 400 rpm, in order to destroy the floc structure and release the contained water. This new sediment had

finer than  $1.3 \text{ }\mu\text{m}$  represented 10% of the total amount of tailings. This particle fineness associated with strong electrostatic repulsion in natural pH ( $7 \leq \text{pH} \leq 8$ ) (Figure 2b), impairs the

and it is equivalent to the  $\tau_0$ . In this work, the Herschel-Bulkley model (H-B) (Equation 3), which is more appropriate to describe the flow curve of thickened tailings, was used to fit the experimental results and obtain the  $\tau_0$  by regression (Nguyen and Boger, 1983, 1998; Sofrá and Boger, 2002, 2011; Boger, 2009, 2013).

its yield point analyzed by both methods and is referred to as dynamic  $\tau_0$ . The direct method was the same as the previous one, and for plotting the flow curve, the shear rate and shear time were defined as  $0.01$  to  $100 \text{ s}^{-1}$  and 5 min per point. The analysis of sediment  $\tau_0$  after high shearing intends to evaluate the maximum floc destruction due to pipeline transport.

### 2.4.3 Sediment concentration analysis

The sediment concentration ( $C_{\text{sed}}$ ) was obtained indirectly by a moisture analyzer, OHAUS, model

MB23. Therefore, after the rheological analysis, the sample was transferred to the moisture analyzer and

subjected to heating, allowing percent solid determination.

## 3. Results and discussion

### 3.1 Nickel tailings characterization

From Figure 2(a), it can be observed that the nickel tailings presented a very fine particle size. Particles smaller than  $28.3 \text{ }\mu\text{m}$  accounted for 90%,  $5.9 \text{ }\mu\text{m}$  accounted for 50% and

natural sedimentation process (Sofrá and Boger, 2011). However, the presence of fine material is indispensable for paste formation. Thus, the need exists to use flocculants.

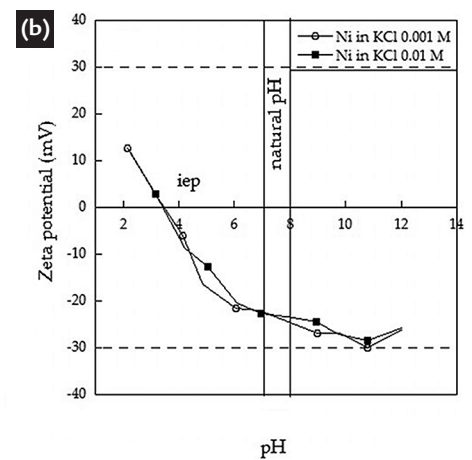
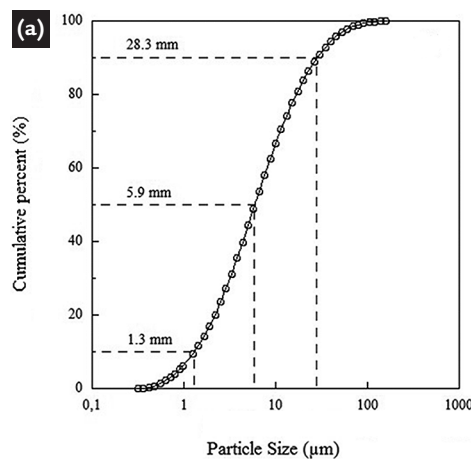


Figure 2  
Nickel tailings

characterization: (a) particle size distribution; (b) net surface charge of the particles.

### 3.2 Thickened tailings characterization

The laboratory-scale batch sedimentation tests (graduated cylinder) were carried out to determine the performance of paste thickeners under the established conditions, by obtaining data on the thickener underflow characteristics.  $\tau_0$  and  $C_{\text{sed}}$  obtained from the various techniques, polymeric flocculants (R-10 and R-90), and  $C_0$  (in the range of 10 to

23% w/w), can be observed in Figures 3 and 4. As reported in literature, there was a variation of the  $C_{\text{sed}}$  in the sediment compaction zone, and the flow properties of concentrated mineral suspensions varied significantly with  $C_{\text{sed}}$  (França *et al.*, 1999; Sofrá and Boger, 2002; Boger, 2013). In this study, the flocculated and thickened sediment presented a concen-

tration variation of up to 28% w/w between top and bottom. Figure 3 (a) shows the increase of the static and dynamic  $\tau_0$  for the bottom sediment relationship to the top. This behavior is due to the existing concentration gradient, thus allowing the acquisition of data on  $\tau_0$  in the limit conditions of each case analyzed. Figure 3 (a) also shows that the measurement

techniques used (direct method and by regression) produced very similar values, even with the difficulties in reaching such low shear rates. Figure 3 (b) illustrates the strong dependence of the  $\tau_0$  on the  $C_0$  and the flocculating polymer type. The increase in  $C_0$  led to growth of the sediment  $\tau_0$ . This occurred because the difference in the  $C_0$  influences the shape

and structure of the flocs formed, and consequently the settling velocity and sediment cohesion (Jarvisa *et al.*, 2005; Sofrá and Boger, 2011; Parsapour *et al.*, 2014). Between the two polymers, R-10 reached higher values of static and dynamic  $\tau_0$ , reaching 1400 Pa and 83 Pa, respectively, for pulps with 23% (w/w) of  $C_0$ . The different efficiencies between

the studied polymers can be explained by the existing polymer-slurry interaction difference, i.e., interaction type (bridging particle flocs or neutralized charge particle flocs), floc size and other aspects (Jarvisa *et al.*, 2005; Sofrá and Boger, 2011). However, for better understanding, it is necessary to elucidate the polymers' structures and characteristics.

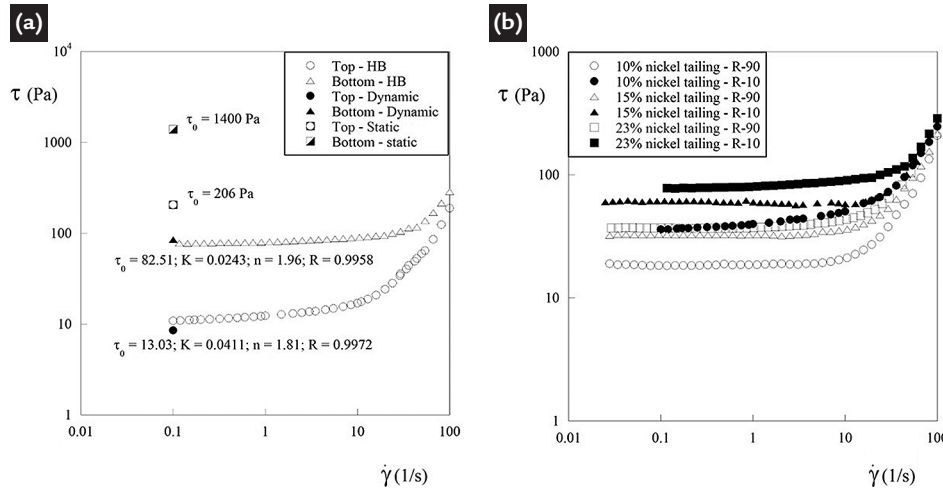


Figure 3 Flow behavior for the thickened nickel tailings. (a) for the top and bottom sediment of the pulp with  $C_0$  of 23% (w/w) and flocculated with the polymer R-10; (b) only dynamic  $\tau_0$  for the sample from the bottom sediment.

The curves presented in Figure 4 show the same trends as those presented in several other studies (Nguyen and Boger, 1998; Sofrá and Boger, 2002, 2011; Boger, 2013), i.e., the exponential growth of  $\tau_0$  with  $C_{sed}$ . The static  $\tau_0$  (Figure 4-a) has values higher than 200 Pa for  $C_{sed}$  greater than 47 and 50% (w/w), flocculated with R-10 and R-90 respec-

tively. These data are of great importance because they are used for rake design in thickeners and for pump restart and design (Boger, 2009).

It can be observed that for all cases studied the underflow had static  $\tau_0$  above that specified for pastes. However, it can be seen in Figure 4 (b) that the dynamic  $\tau_0$  reached maximum values of 82.5 and

37 Pa, with R-10 and R-90 respectively, indicating that in the case of complete destruction of the flocs, the thickened tailings do not achieve paste consistency. However, for paste transportation, a positive displacement pump is used instead of a centrifugal pump. Thus, it is certain that the floc destruction will be much less intense.

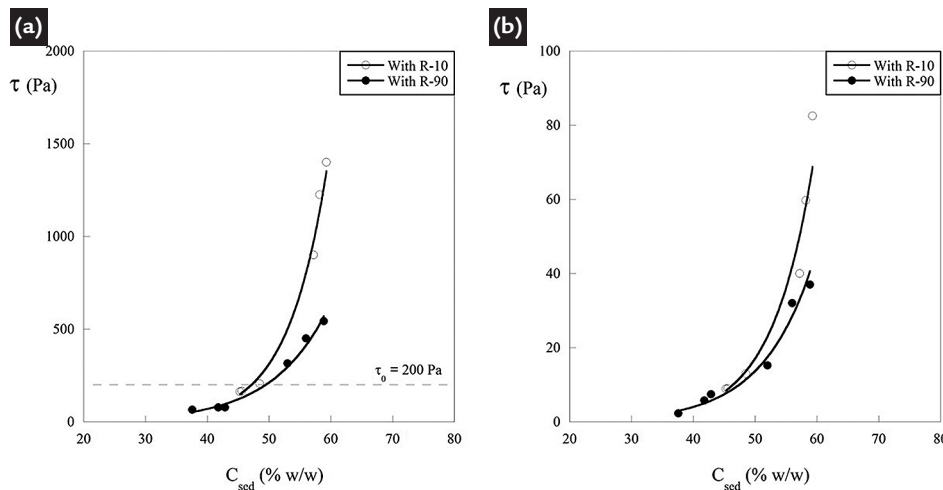


Figure 4  $\tau_0$  as a function of  $C_{sed}$ . (a) static  $\tau_0$ ; (b) dynamic  $\tau_0$ .

An example of the slump test is shown in Figure 5, and Figure 6 illustrates the strong relationship of the static and dynamic  $\tau_0$ ,  $C_{sed}$  and slump height. The data in Figure 5 indicate the same trends as those presented in other studies (Pashias *et al.*, 1996; Clayton *et al.*, 2003; Osorio *et al.*, 2008; Boger,

2009; Deng *et al.*, 2017; Mizani and Simms, 2016), i.e., an inverse relationship of %SH with  $\tau_0$  and  $C_{sed}$ . Figure 6 (a) evidences that the use of polymer R-10 as a flocculant allowed the formation of more cohesive sediments, that is, with higher values of static  $\tau_0$  and lower values of %SH, reaching SH=12%.

Figure 6 (b) allows comparison of the  $\tau_0$  and %SH of the sediment before and after shearing, that is, before and after the breaking of the flocs. It can be observed that the breaking of the flocs released the contained water, abruptly reducing the sediment consistency, increasing %SH and reducing  $\tau_0$ .



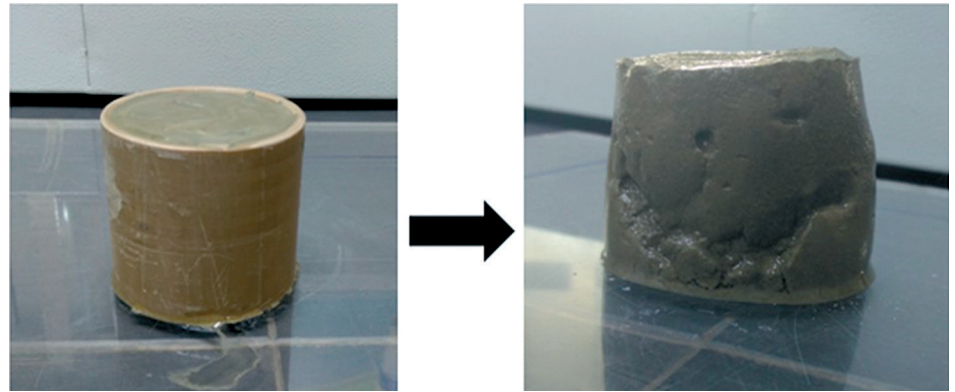


Figure 5  
Slump test for the sediment formed with C0 of the 23% and 80 g/t R-10.

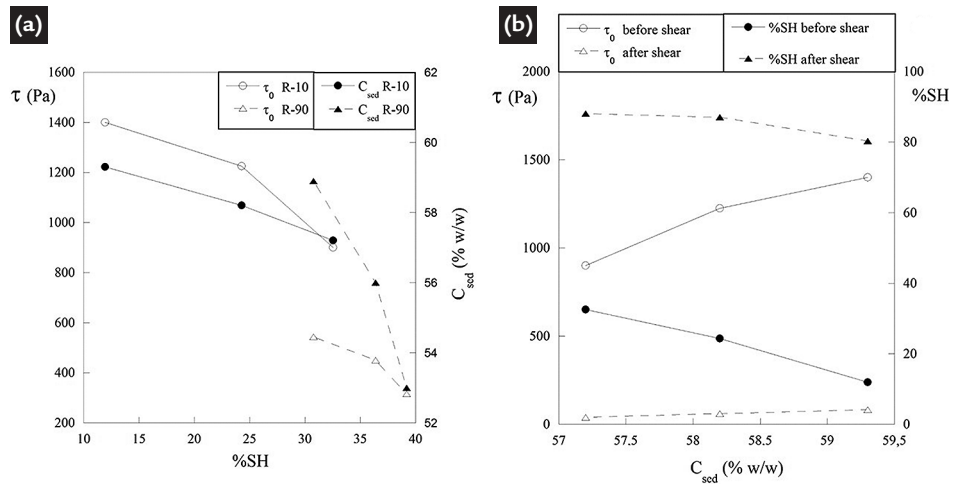


Figure 6  
Relationship between the  $\tau_0$ ,  $C_{sed}$  and %SH. (a) static  $\tau_0$ ; (b) dynamic and static  $\tau_0$  for polymer R-10.

The flocculation and sedimentation of the nickel tailing allowed a water recovery up

to 90% w/w. In all cases studied, recovered water presented turbidity less than 100 NTU

that according to the Brazilian standards, allows its reuse or disposal in the environment.

#### 4. Conclusion

This article presented and discussed the effect of initial solid concentration and polymeric flocculant type on the cohesion of nickel tailings. Both flocculants were efficient in thickening by batch sedimenta-

tion, causing an increase in  $C_{sed}$  with increase in  $C_0$ , and consequently, increase of  $\tau_0$  and reduction of %SH. In other words, they allowed the production of more cohesive and stable sediments. Therefore,

the results provide the mining company a new alternative for the management of their tailings, allowing its disposition in the form of paste and a process water recovery with turbidity less than 100 NTU.

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