Abridged Acid-Base Wet-Milling Synthesis of High Purity Hydroyapatite

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There is a plethora of routes to produce hydroxyapatite(HA) and in general calcium phosphates(CP) but production usually leads to a mixture of several phases. Besides ionic contamination, most of these methods are cumbersome, restricted to small volumes of product and require a lot of thermal energy. The acid-base route eliminates foreign ions or additives and its only byproduct is water. Heterogeneous reaction drawback is that solid reactants do not easily come in contact with each other and therefore addition and stirring times become very lengthy and still the product is a mixture.

The synthesis started from calcium hydroxide and phosphoric acid (PA). Ball milling was used to favor kinetics and stoichiometry. Six sets of PA addition, paddle stirring and ball milling times were used. Products were evaluated by X ray diffraction (XRD), Fourier Transform Infrared (FTIR), scanning electron microscopy (SEM), X ray fluorescence (XRF) and Ca/P ratio. Chemical analysis for calcium proceeded through oxalate precipitate and phosphorus by the phosphomolibdate technique. A set of conditions yielding high purity HA was established.

Keywords: hydroxyapatite synthesis, high purity hydroxyapatite, mechanosynthesis

1. Introduction and Literature Review

CPs are the most abundant inorganic constituent of living beings hard tissues. This inorganic part provides bone and teeth with hardness, density and mechanical stability. HA $(Ca_{10}(PO_4)_6(OH)_2)$ is the main CP present in these tissues^{1,2}.

Hypomineralization, fractures and many pathologies make necessary the reinforcement or substitution of hard tissues with various CPs among which HA plays a central role. Injuries and disease treatments for improving or restoring body functions require also the use of metallic plates, wires and screws as well as calcium phosphates based cements for adhesion or gap filling²⁻⁸. HA is the main or one of the major starting components for these biomaterials and usually the main final phase after physicochemical and biological processes. Therefore it is important to count on a reliable, expedite method for producing inexpensive abundant pure HA.

There are many synthetic routes and preparation methods for HA. There is also a large variability of products with several CPs contaminants present, fact that demonstrates how difficult it is to obtain pure stoichiometric HA⁷. Several methods belong in the most used techniques, namely wet synthesis, solid state reaction, sol-gel process, sonochemical synthesis and the hydrothermal route⁷⁻¹⁷. A couple of these methods are able to produce pure HA but their yield is low compared to the mass and volume used (5 to 14.8 g of product per 100 mL of initial reaction volume).

Almost all of the commercially available CPs are mixtures of several phases and many contain foreing elements. Some of the common methods rely on CPs compounds for producing HA. This strategy just postpones the problem without solving it, otherwise the starting CP has to be synthesized without contamination in order to calculate precise proportions for a defined reaction. For instance solid monocalcium phosphate monohydrate (MCPM) can be reacted at 1200 °C with solid CaCO₃ to produce HA but MCPM usually contains

phosphoric acid, some dicalcium phosphate dihydrate (DCPD) and probably anhydrous monocalcium phosphate (MCPA). In this way the time to produce HA has to include the synthesis and characterization of pure MCPM.

Synthesis in solution imply foreign ions since most calcium salts are sparingly soluble and only a few like nitrates, chlorides or acetates are suitable for this method. In order to displace foreign anions, phosphorus is supplied as a salt, usually sodium, potassium or ammonium salts and hence non CPs such as NaCl or sodium acetate are formed. Organic anions can be burnt off. Ammonium nitrate seems to leave no residue. Filtering is often an inapropiate practice because once the CP sediment is formed most methods separate the mother liquor from the solid by decantation or filtration. This supernatant contains most of the soluble foreign salts plus an incongruent concentration of calcium and phosphorus that deviate the solid stoichiometry generating extraneous phases. Solid state route relies on CPs and very prolonged heating, milling, pelletizing and reheating cycles in order to achieve homogeneity and complete reaction.

The sol-gel method has advantages for instance final particle size and coating forming capabilities but the high cost and low content of organometallic precursors are noticeable as well as its chemical instability. Hydrothermal conditions are limited because of the internal useful volume of the reactor.

One of the starting points where the almost inherent CPs phase contamination can be avoided is to use non CPs sources of calcium and phosphorus namely $Ca(OH)_2$ and H_3PO_4 so that the only byproduct is water, is a very clean reaction (Equation 1). Calcium hydroxide is only slightly soluble and if the solution approach is to be applied then quite large volumes of very dilute solutions must be used and small amounts of HA will be obtained. Since productivity is a must then high solid to liquid ratio suspensions should be used. The main

drawback of this heterogeneous systems is that the reaction does not proceed easily to the desired and calculated product because of mass transfer restrictions in and around insoluble calcium hydroxide grains (Figure 1). Acidic sparingly soluble CPs (mainly dicalcium phosphate dihydrate or DCPD) are rapidly formed on the surface of calcium hydroxide grains engulfing the unreacted core and hindering further reaction. Composition of solution surrounding grains is ruled by this non HA acidic CPs whose solubility product constant is huge compared to that of HA ($-\log Ksp = 6.59$ for DCPD and 116.8 for HA at 25 °C¹) and also the Ca/P ratio in solution is different from 1.67 (1.0 for DCPD) and therefore filtration should be avoided to maintain precise reactants proportions for a preselected product. While acidic CPs are on the outer layers, unreacted calcium hydroxide and basic CPs lie inside. Careful attention was exerted to dodge any unwanted deviation in stoichiometry caused by processes such as filtering.

The primary purpose of this work was to establish the relative importance of addition, stirring and ball milling times on final product content indicating the capability to break or disperse the grains. Breaking facilitates access for acid-base reaction to proceed. The final purpose was to attain a brief and easy method for obtaining high purity HA.

2. Experimental Procedure

2.1. HA synthesis

United States Pharmacopoeia (USP) grade calcium carbonate (content > 99%) was heated to constant weight at 900 °C (3 hours) to obtain calcium oxide that was kept in a desiccator and finally carefully weighed. Recently boiled cool deionized water was carefully mixed in under mechanical paddle stirring with calcium oxide to give a thick calcium hydroxide suspension. Splatter caused by intense heat evolution was controlled using deionized ice and cool water inside the vessel that was partially submerged in ice water. For methods one through five 295 g of calcium hydroxide were contained in 400 mL deionized water, (S/L ratio 0.74). Without delay 161.0 mL of analytical reagent grade orthophosphoric acid solution (85%, Merck[®]) previously titrated with NaOH was poured or dropwise added on the calcium hydroxide slurry following the six methods described below. The proper stoichiometric weights were calculated based on Equation 1

$$10Ca(OH)_2 + 6H_3PO_4 \rightarrow Ca_{10}(PO_4)_6(OH)_2 + 18H_2O$$
(1)

Methods were numbered 1 through 6 (M1, M2 ...,M6), the product of each method was labeled HA1 for method 1 and so on.



Figure 1. Partially reacted $Ca(OH)_2$ grain structure with concentration gradient layers. H_3PO_4 solution is background. Zone 1 is rich in phosphate, zone 6 is rich in calcium probably calcium hydroxide. Ca / P ratio increases going inward.

M1 with many small variations is perhaps the most widely used wet route method⁷ and here it was included as a starting point and as a comparison. The six methods were:

- M1) PA dropwise addition during 6 hours (0.45 mL per minute) on the stirred aqueous calcium hydroxide suspension mixing with a teflon blades stirrer for 18 hours more. The product was named HA1;
- M2) Rapid PA addition (13 minutes equivalent to 12.38 mL per minute) over the calcium hydroxide slurry with stirring for 24 hours including the addition time;
- M3) One hour PA addition on calcium hydroxide stirred suspension followed by 1 hour wet ball milling;
- M4) PA addition in 1 hour over stirred calcium hydroxide slurry and 6 hours ball milling;
- M5) Rapid PA addition (13 minutes) on stirred calcium hydroxide suspension plus 6 hours ball milling. Solid calcium hydroxide to deionized water weight ratio (S/L) was 0.74; and
- M6) The same as M5 but solid to water ratio was 1.18 (295 g/250 mL).

Milling was conducted with alumina balls in a jar mill fitted with a porcelain ceramic tank rotating at 58 rpm. Transfer from reaction vessel to milling tank was done quantitatively for supernatant and solids without wasting any reactant but keeping rinsing water volume as small as possible. Milled slurries were transferred into platinum crucibles for drying and firing with lid on. Resulting HA was dried at 100-110 °C for 2 hours and sintered for 4 hours at 1000 °C.

2.2. Characterization

Dry unsintered HA (indicated by nsHA1 through nsHA6) and sintered HA samples (sHA1 through sHA6) were subjected to XRD (Philips type PW 1820 Based diffractometer, copper anode, 40 KV, 30 mA, $\lambda = 1.54181$ nm.), FTIR (Perkin Elmer Paragom 500) and their Ca / P molar ratios were assessed by chemical wet analysis.

Calcium was measured by precipitating calcium as oxalate, dissolving it with sulfuric acid and titrating with standardized KMnO₄ solution. Phosphorus content was also volumetrically measured by precipitating phosphorus as ammonium phosphomolibdate, dissolving the yellow precipitate with NaOH and finally titrating excess sodium hydroxide with standardized hydrochloric acid solution^{18,19}. Results are the media of three determinations for Ca and three for P in each of the samples.

Particle size was measured by laser dispersion (Cilas 1064) for green dry HA suspended in 96% ethanol with 60 seconds ultrasonication prior to reading. Particle size of sHA depends on temperature and sintering time, contact area, pressure and many other factors as well as manually breaking HA lumps, so it was not measured but estimated from scannig electron microscopy (SEM). Basic crystallite size was calculated by means of Equation 2:

$$L = \frac{k\lambda}{\beta\cos\theta}$$
(2)

k = 0.9; β = peak width at half height of main XR signal. $\lambda_{_{Cu}}$ = 1.54181 nm.

The effect of milling contamination on elemental composition was assessed by XRF semiquantitative analysis (Philips[®] Magic X PRO PW 2440/00) on 40 mm diameter disks pressed with calcium hydroxide or sHA6 powder and spectroscopic wax tabletting aid (Merck-Hoechst[®]).

3. Results and Discussion

XRD peaks were assigned after careful comparison with XRD data^{7,8,20} for possible CP compounds as follows : $Ca_{10}(PO_4)_6(OH)_2$, or

HA, α-Ca₃(PO₄)₂ or alfa tricalcium phophate (α-TCP), β-TCP (here simplified to TCP on XRD patterns), Ca(OH)₂, CaO, Ca(H₂PO₄)₂·H₂O monocalcium phosphate monohydrate or MCPM, Ca₈H₂(PO₄)₆·5H₂O octacalcium phosphate (OCP), CaHPO₄·2H₂O dicalcium phosphate dihydrate or DCPD, Ca(H₂PO₄)₂ monocalcium phosphate anhydrous or MCPA, Ca₄(PO₄)₂O tetracalcium phosphate or TetCP, carboa-patite Ca₁₀(PO₄)₃(CO₃)₃(OH)₂ and CaHPO₄ dicalcium phosphate anhydrous or DCPA. Five phases (HA, β-TCP, Ca(OH)₂, CaO and monocalcium phosphate anhydrous) were identified by comparison with JCPDS files 09-0432, 09-0169, 04-733, 037-1497 and 09-080 respectively²⁰.

Figures 2 and 3 show the diffractograms for nsHA1 to 6. As seen, before firing there are always four detected phases. Equations 3 through 6 may proceed simultaneously. TCP and DCPA are incomplete reaction products. Calcium hydroxide is remaining reactant.

$$2\text{CaHPO}_{4} + \text{Ca(OH)}_{2} \rightarrow \text{Ca}_{2}(\text{PO}_{4})_{2} + 2\text{H}_{2}\text{O}$$
(3)

$$6CaHPO_4 + 4Ca(OH)_2 \rightarrow Ca_{10}(PO_4)_6(OH)_2 + 6H_2O$$
(4)

$$2Ca_{3}(PO_{4})_{2} + 2CaHPO_{4} + 2Ca(OH)_{2} \rightarrow$$

$$Ca_{10}(PO_{4})_{2}(OH)_{3} + 2H_{2}O$$
(5)



Figure 2. XRD patterns of non sintered HA 1, 2 and 3.



Figure 3. XRD patterns of non sintered HA 4, 5 and 6.

$$6Ca_{3}(PO_{4})_{2} + 2Ca(OH)_{2} \rightarrow 2Ca_{10}(PO_{4})_{6}(OH)_{2}$$
(6)

$$Ca(OH)_2 \rightarrow CaO + H_2O$$
 (7)

$$Ca_{10}(PO_4)_6(OH)_2 + 2CaHPO_4 \rightarrow 4Ca_3(PO_4)_2 + 2H_2O$$
 (8)

3.1. Unsintered products

By comparison of peaks between 30 and 35 degrees for nsHA1 and 2 (Figure 2) it can be seen that slower acid addition (M1) favors the formation of HA and shorter times (M2) favor CaHPO₄ and TCP. The fact that M1 and M2 used the same total stirring scheme (24 hours) but different addition times implies the latter exerts a stronger effect.

In this regard, patterns for nsHA1 and nsHA3 show that method 1 (6 hours acid addition + 18 hours stirring) seems to be slightly better

than M3 (1 hour addition + 1 hour milling). Observing nsHA2 and 3 it can be seen that 1h addition (M3) works out better than quick addition (13 minutes in M2). The influence of milling time can be inferred from nsHA4's diffractogram which displays lower HA peaks than expected when keeping in mind nsHA3. This can be interpreted in terms of a small milling effect. Nevertheless as discussed below, the content of pure HA after burning is not directly related to HA content in unsintered samples. When intending to increase the HA content in non sintered material it would seem important to proceed with a slow addition of PA and very lengthy stirring times.

3.2. Sintered products

Inspection of diffractograms for sintered products (Figures 4 and 5) makes clear that thermal treatment has reduced the phases to three. CaHPO₄ has disappeared probably through reactions 3 to 5



Figure 4. XRD patterns of sintered products from methods 1, 2 and 3.



Figure 5. XRD patterns of sintered products from methods 4, 5 and 6.

rendering either TCP (M1, M2, M3, M5) or HA (M4, M6) as the main DRX signals. Calcium hydroxide has dehydrated into calcium oxide (reaction 7). Whenever TCP displays the strongest peaks, there is also non reacted calcium oxide (~37.39 degrees and far right peak in sHA1, 2, 3 and 5). In the patterns where HA's peaks are the strongest there is either very little calcium oxide (sHA4) or no calcium oxide (sHA6). TCP and calcium oxide should react following reaction 6 to yield HA but when those two chemical are not evenly distributed reaction is hindered.

It is interesting to note that non sintered patterns with HA strongest peaks can lead to a sintered product with TCP displaying the main peaks, see for instance nsHA1 and sHA1. Also, nsHA4 and nsHA6 do not outstand for HA intense peaks but once heated sHA4 and sHA6 exhibit an almost pure or pure HA diffractogram. An intense HA peak can become a TCP peak through reactions 3 and 8. As stated above, TCP is present whenever calcium oxide is present, these two would react following reaction 6 but this does not happen because inhomogeneity does not allow it. Resulting homogeneity and probably particle size is the difference among methods and it is not noticeable until sintering makes it apparent.

M3 results indicate that 1 hour addition and 1 hour milling do not end in a suitable homogeneity. M4 shows that increasing milling to 6 hours achieves an almost pure sHA. Trials with longer milling did not show any improvement. Milling efficiency is probably restricted by the liquid fraction that dampers and absorbs balls collision energy

M5 (sHA5, Figure 5) makes clear that the effect of 6 hours milling is outweighed by the disadvantage of quick PA addition.

Since milling longer than 6 hour with M4 did not work then an increase in milling efficiency through solid to liquid ratio control was included in M6. Figure 5 sets forth a sHA6 without any XRD detectable contamination. The result of a pure monophasic sHA6 reveals that an increased solid to liquid ratio largely overcomes the deleterious effect of quick acid addition of M6 and results are even better than those of 1 hour PA addition of M4.

In an interesting approach some researchers¹⁷ used the same acidbase reaction for HA starting from an aqueous calcium hydroxide suspension stabilized with an ionic polymeric defflocculant (Darvan) to have up to 148 g calcium hydroxide per liter then following lengthy method 1 here described. That article has to rely on an assumed total elimination of the organic moiety as well as the ammonim counterion. In the present article about 1,180 g calcium hydroxide can be contained in a liter of water so productivity is in a proportion of nearly 8 to 1 (1180/148), the studied method requires no filtration, less time and energy for drying and includes no extraneous ions or molecules, characteristic that might be of paramount importance in an endogenous implanted biomaterial. Contaminated product of M1 requires 24 hours while pure HA number 6 needs only 6 hours and 13 minutes. Whatever the method is calcium hydroxide preparation is advisable because even though it consumes time and energy it assures calcium hydroxide purity since its obtention starts from a stable compound of known composition (calcium carbonate). Commercial calcium hydroxide might contain foreign elements and depending on shelf life it can be wet and carbonated, so any way there is need to dry it and fire it.

Crystallite size calculated from main DRX peak for sHA6 was 6.64 nm and that estimated from SEM observations that obviously corresponds to aggregates was approximately 8 µm (Figure 6).

Experimental Ca/P molar ratios appear in Table 1.

These are all close to the theoretical value (1.666) even those corresponding to mixtures of various phases like sHA1, sHA3 or sHA5. The ratio is only an indication of global composition and does not imply presence of a certain phase or even phase purity because

for instance, before reaction a solid mixture of 7 moles of calcium carbonate and 3 moles of MCPM calculated for producing stoichiometric HA yields a perfect Ca/P =1.67 if it is very uniform but there is no HA at all. Lower or higher ratios can be obtained the greater the heterogeneity is. This ratio here indicates that reactants were added in the right proportions and that there was little or no loss.

FTIR spectra of samples prepared in KBr pellets display (Figure 7) adsorption bands related to OH ion stretching (3571 cm⁻¹)

Table 1. Experimental molar Ca/P ratios of sintered products.

Sample	Molar Ca/P.
sHA1	1.65
sHA2	1.64
sHA3	1.66
sHA4	1.64
sHA5	1.66
sHA6	1.67



Figure 6. 10,000 magnification SEM of sintered HA6.



Figure 7. FTIR spectra of nsHA6 and sHA6.

and water in the sample (3400-3200 cm⁻¹), which is very noticeable for nsHA6 but almost inexistent for sHA6 because the latter had been recently sintered while the former had not. For upper curve spectroscopic grade KBr pellet background was substracted in order to better observe inherent final product features.

Lower curve band at 1636 is originated in a KBr absorption. The nsHA6 bands at 1419 and 896 cm⁻¹ are caused mainly by the asymmetric in plane stretching and out of the plane bending modes of $CO_3 = respectively^7$. These two bands disappeared in sinter indicating that carbonate was eliminated by heat treatment.

Absorptions at 1091, 1044 (v3) and shoulder at 960 (v1) are characteristic for phosphates as well as those at 601 and 570 cm⁻¹ (v4). The band at 631 cm⁻¹ is attributed to an OH ion libration²². HPO4 = can be identified by a band at 870 cm⁻¹ in calcium deficient apatites^{7,21} and that band is absent in sHA6. In short, sHA6 generates an FTIR spectrum that is characteristic of hydroxyapatite and contains no indication of carbonate or HPO₄ = content.

XRF elemental analysis of calcium hydroxide detected five minor elements (Al, Si, S, Zn and Sr). PA specifications state traces of several elements, most of them below a few parts per million (ppm) or even less. Out of the five above mentioned traces only S and Zn (0.0007% and 0.0002%) arise from PA. In sHA6 the same five elements were found. Two of these elements might come from alumina balls or porcelain milling tank: Al and Si. Silicon remained virtually constant in both samples (0.099%) that is before and after milling. Aluminum increased from 0.052% in calcium hydroxide to 0.224% in sHA6 implying that milling device does slightly impair product's composition. Sulphur, zinc and strontium percent concentrations in sHA6 were 0.010, 0.003 and 0.010 respectively and do not significantly differ from those in calcium hydroxide.

4. Conclusions

Four phases constitute all the six methods' raw products namely calcium hydroxide, TCP, HA and CaHPO4 regardless of the range of applied conditions. Calcium hydroxide and CaHPO4 disappear during sintering because they react following various reactions that increase HA or TCP content. Calcium hydroxide also disappears by dehydration forming calcium oxide. In method number 6 TCP, calcium hydroxide and CaHPO4 react without residue to form only HA.

Slow PA addition favors cold HA formation in raw mixtures. Quick PA addition works in the opposite direction, it cuts down HA formation. Mechanical paddle stirring time slightly improves reaction, it exerts a less important effect than addition time and is insufficient for reaching a thorough homogeneity. One hour milling promotes HA final content but 6 hours are necessary for making a nearly uniform dispersion of raw product suitable for a complete thermally activated reaction. Heating is necessary for a complete the reaction. Solid to liquid proportion is a determining factor in directing reaction towards high purity HA. Solid to liquid ratio influence is much larger than that of quick PA addition. There is no complete reaction without a thorough homogeneity and a thermal activation. An abridged method for producing highly pure monophasic HA in substantial amounts has been established.

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